

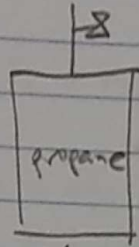
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①



$$V = 200 \text{ L}$$

①

$$T_1 = 400 \text{ K}$$

$$P_1 = 3.5 \text{ MPa}$$

②

$$m_2 = 0.5 \text{ m}$$

$$PV^{1.4} = c$$

Calculate heat transfer during process.

Transient flow

 Ideal gas.  $R = 0.18855 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$ 

$$m_1 = \frac{PV}{RT} = \frac{3500 (200 \times 10^{-3}) \text{ m}^3}{0.18855 (400)} = 9.281 \text{ kg}$$

$$m_2 = 4.641 \text{ kg}$$

$$v_1 = \frac{V_1}{m_1} = 0.0215 \frac{\text{m}^3}{\text{kg}}$$

$$v_2 = \frac{V_2}{m_2} = \frac{200 \times 10^{-3}}{4.641} = 0.0430 \frac{\text{m}^3}{\text{kg}}$$

$$\therefore P_2 v_2^{1.4} = P_1 v_1^{1.4}$$

$$\therefore P_2 = 1321.9 \text{ kPa}$$

Apply 1st Law

$$\Delta U = Q - W + \sum_{in} \dot{m}_i (h_i + \frac{V_i^2}{2} + z_i) - \sum_{out} \dot{m}_j (h_j + \frac{V_j^2}{2} + z_j)$$

$$U_2 - U_1 = Q - m_{out} h_{out}$$

$$m_2 u_2 - m_1 u_1 = Q - m_{out} h_{out}$$

$$m_2 c_v T_2 - m_1 c_v T_1 = Q - m_{out} h_{out}$$

Major issue:  $h_{out}$  is not constant since the temperature inside the tank is changing.

- we need a way to model this behavior

we can either:

- ① solve it in small increments of temperature. This requires a relationship how the temperature varies during the process.

From ideal gas eqn &  $p v^{1/4} = c$ , we can find this

we can also properly integrate the whole process

- ② Knowing  $T_2$  from ideal gas &  $p v^{1/4} = c$ , we can approximate  $T_{out}$  to be the average  $T$  between  $T_1$  &  $T_2$ .

From ideal gas &  $p v^{1/4} = c$ :

$$T_2 = \frac{p_2 V}{m_2 R} = \frac{(1321.9 \text{ kPa}) (200 \times 10^{-3} \text{ m}^3)}{4.641 \text{ kg} \cdot 0.18055}$$

$$= 302.13 \text{ K}$$



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$$T_{avg} = 351.06 \text{ K}$$

$$\therefore m_2 c_v T_2 - m_1 c_v T_1 = Q - (m_1 - m_2) c_p T_{avg}$$

$$\rightarrow Q = 4.641 (1.4909) (302.13)$$

$$- 2.281 (1.4909) (400)$$

$$+ 4.641 (1.6794) (351.06)$$

$$= -708.1 \text{ kJ}$$

$$Q_{loss} = 708.1 \text{ kJ}$$

or using method ①

$$\int_{T_1}^{T_2} du = \int \delta Q - \int_{T_1}^{T_2} m c_v dT$$

 assuming  $c_v, c_p$  constant

$$c_v \int m dT = Q - c_p \int m dT \quad \text{we need } m = f(T)$$

$$m = \frac{pV}{RT}, \quad pV^{1.4} = C$$

$$p = \frac{C}{V^{1.4}} = \frac{C}{\left(\frac{V}{m}\right)^{1.4}}$$

$$= \frac{C m^{1.4}}{V^{1.4}}$$

$$\rightarrow m = \frac{C m^{1.4}}{V^{1.4}} \frac{V}{RT}$$

$$m^{-0.4} = \frac{C V^{-0.4}}{RT}$$

$$m = \left(\frac{C}{R}\right)^{\frac{1}{0.4}} V^{\frac{1}{0.4}} T^{\frac{1}{0.4}}$$

put this into integral &amp; solve analytically or numerically.

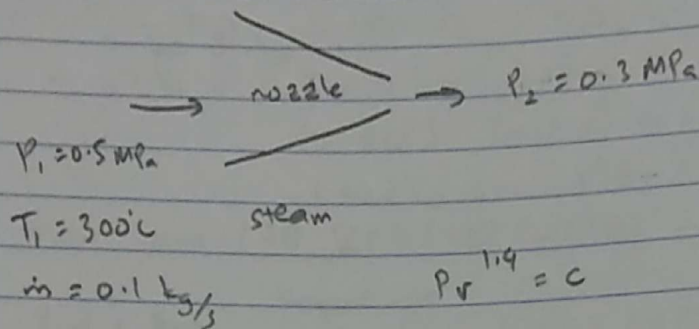
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②


 Find  $\Delta ke$  &  $Q$ 

1st. law:

$$\begin{aligned}
 \sum \dot{Q} - \sum \dot{W} &= \sum \dot{m} (h + ke + pe) - \sum \dot{m} (h + ke + pe) \\
 &= \dot{m} \left[ (h_2 - h_1) + \left( \frac{V_2^2 - V_1^2}{2} \right) \right] \\
 &= \dot{m} [(h_2 - h_1) + \Delta ke]
 \end{aligned}$$

2nd law:

$$\frac{ds}{\dot{m}} = \sum \frac{\dot{Q}}{T} + m(s_1 - s_2) + \frac{\dot{\sigma}}{\dot{m}}$$

$\overset{0}{(steady)}$   $\overset{0}{(reversible)}$

$$\rightarrow Q = T ds$$

 Given  $P_r^{1.4} = c$ 

$$\left. \begin{array}{l} P_1 \\ T_1 \end{array} \right\} \begin{array}{l} s_1 = \checkmark \\ h_1 = \checkmark \\ s_1 = \checkmark \end{array}$$

$$\left. \begin{array}{l} P_2 \\ V_2 \text{ from } P_r^{1.4} = c \end{array} \right\} \begin{array}{l} h_2 = \checkmark \\ s_2 = \checkmark \end{array}$$



To find  $q$ , we can use  $q = T ds$

but the major issue is we do not know  $T$  or the relationship between  $T$  &  $s$  to perform integration

It is suggested that:

- ① we can take the average temperature between  $T_1$  &  $T_2$  for use in  $q = T ds$

$T_2$  can be found from known  $p_2, v_2$

- ② we can perform the above step in small increments of  $p$  until we reach  $p_2$ . The results of the incremental steps can be added to give a more accurate solution.

$$\left. \begin{array}{l} p_1 = 0.5 \text{ MPa} \\ T_1 = 300^\circ\text{C} \end{array} \right\} \begin{array}{l} h_1 = 3064.2 \text{ kJ/kg} \\ v_1 = 0.5226 \text{ m}^3/\text{kg} \\ s_1 = 7.4599 \text{ kJ/kg}\cdot\text{K} \end{array}$$

$$p_2 = 0.3 \text{ MPa}$$

$$v_2 = \left( \frac{p_1}{p_2} \right)^{1/1.4} v_1 = \left( \frac{0.5}{0.3} \right)^{1/1.4} (0.5226)$$

$$= 0.7527 \text{ m}^3/\text{kg}$$

$\left. \begin{array}{l} p_2 \\ v_2 \end{array} \right\}$  Superheated, interpolation;

$$\frac{\Delta h}{\Delta v} = \frac{h_2 - 2865.6}{0.7527 - 0.7163} = \frac{2967.6 - 2865.6}{0.7964 - 0.7163}$$

$$\rightarrow h_2 = 2911.95 \text{ kJ/kg}$$

$$\frac{\Delta s}{\Delta v} = \frac{s_2 - 7.3115}{0.7527 - 0.7163} = \frac{7.5166 - 7.3115}{0.7964 - 0.7163}$$

$$\rightarrow s_2 = 7.4047 \text{ kJ/kg}\cdot\text{K}$$

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$$\frac{\Delta T}{\Delta V} = \frac{T_2 - 200}{0.7527 - 0.7163} = \frac{250 - 200}{0.7964 - 0.7163}$$

$$\rightarrow T_2 = 222.72 \text{ }^\circ\text{C}$$

$$\therefore T_{\text{avg}} = 261.36 \text{ }^\circ\text{C} = 534.36 \text{ K}$$

$$\begin{aligned} \rightarrow Q &= T_{\text{avg}} \Delta S \\ &= 534.36 (7.4047 - 7.4599) \\ &= -29.50 \frac{\text{kJ}}{\text{kg}} \end{aligned}$$

$$\begin{aligned} \dot{Q} &= \dot{Q} \dot{m} \\ &= -2.950 \text{ kW} \end{aligned}$$

$$\begin{aligned} \therefore \Delta Ke &= \dot{Q} + \dot{m} (h_1 - h_2) \\ &= -2.950 + 0.1 (3064.2 - 2911.95) \\ &= ~~-2.950 + 0.1 (3064.2 - 2911.95)~~ \\ &= -2.950 \text{ kW} \end{aligned}$$