

10. S. W. Churchill and H. H. S. Chu. "Correlating Equations for Laminar and Turbulent Free Convection from a Horizontal Cylinder." *International Journal of Heat Mass Transfer* 18 (1975), p. 1049.
11. S. W. Churchill and H. H. S. Chu. "Correlating Equations for Laminar and Turbulent Free Convection from a Vertical Plate." *International Journal of Heat Mass Transfer* 18 (1975), p. 1323.
12. E. R. G. Eckert and E. Soehngen. "Studies on Heat Transfer in Laminar Free Convection with Zehnder-Mach Interferometer." USAF Technical Report 5747, December 1948.
13. E. R. G. Eckert and E. Soehngen. "Interferometric Studies on the Stability and Transition to Turbulence of a Free Convection Boundary Layer." *Proceedings of General Discussion, Heat Transfer ASME-IME*, London, 1951.
14. S. M. ElSherbiny, G. D. Raithby, and K. G. T. Hollands. "Heat Transfer by Natural Convection Across Vertical and Inclined Air Layers." *Journal of Heat Transfer* 104 (1982), pp. 96–102.
15. T. Fujii and H. Imura. "Natural Convection Heat Transfer from a Plate with Arbitrary Inclination." *International Journal of Heat Mass Transfer* 15 (1972), p. 755.
16. A. J. Ghajar and A. Asadi. "Improved Forced Convective Heat Transfer Correlations for Liquids in the Near-Critical Region." *AIAA Journal*, Vol. 24, No. 12 (1986), pp. 2030–2037.
17. S. Ghorbani-Tari and A. J. Ghajar. "Improved Free Convective Heat Transfer Correlations in the Near-Critical Region." *AIAA Journal*, Vol. 23, No. 10 (1985), pp. 1647–1649.
18. K. G. T. Hollands, T. E. Unny, G. D. Raithby, and L. Konicek. "Free Convective Heat Transfer Across Inclined Air Layers." *Journal of Heat Transfer* 98 (1976), pp. 182–193.
19. M. Jakob. *Heat Transfer*. New York: Wiley, 1949.
20. W. M. Kays, M. E. Crawford, and B. Weigand. *Convective Heat and Mass Transfer*. 4th ed. New York: McGraw-Hill, 2005.
21. R. K. MacGregor and A. P. Emery. "Free Convection Through Vertical Plane Layers: Moderate and High Prandtl Number Fluids." *Journal of Heat Transfer* 91 (1969), p. 391.
22. T. S. Najjar and A. J. Ghajar. "Prediction of Density and Constant Pressure Specific Heat for Several Fluids in the Near-Critical Region." AIAA paper No. 83-1476, *AIAA 18th Thermophysics Conference*, Montreal, Canada, June 1–3 (1983).
23. G. D. Raithby and K. G. T. Hollands. "A General Method of Obtaining Approximate Solutions to Laminar and Turbulent Free Convection Problems." In *Advances in Heat Transfer*, eds. F. Irvine and J. P. Hartnett, Vol. II, pp. 265–315. New York: Academic Press, 1975.
24. E. M. Sparrow and J. L. Gregg. "Laminar Free Convection from a Vertical Flat Plate." *Transactions of the ASME* 78 (1956), p. 438.
25. E. M. Sparrow and J. L. Gregg. "Laminar Free Convection Heat Transfer from the Outer Surface of a Vertical Circular Cylinder." *ASME* 78 (1956), p. 1823.
26. L. M. Tam and A. J. Ghajar. "Transitional Heat Transfer in Plain Horizontal Tubes." *Heat Transfer Engineering*, Vol. 27, No. 5 (2006), pp. 23–38.

PROBLEMS*

Physical Mechanism of Natural Convection

20-1C In which mode of heat transfer is the convection heat transfer coefficient usually higher, natural convection or forced convection? Why?

20-2C What is buoyancy force? Compare the relative magnitudes of the buoyancy force acting on a body immersed in these mediums: (a) air, (b) water, (c) mercury, and (d) an evacuated chamber.

20-3C Consider a hot boiled egg in a spacecraft that is filled with air at atmospheric pressure and temperature at all times. Will the egg cool faster or slower when the spacecraft is in space instead of on the ground? Explain.



20-4C When will the hull of a ship sink in water deeper: when the ship is sailing in fresh water or in seawater? Why?

20-5C Consider two fluids, one with a large coefficient of volume expansion and the other with a small one. In what fluid will a hot surface initiate stronger natural convection currents? Why? Assume the viscosity of the fluids to be the same.

20-6C Physically, what does the Grashof number represent? How does the Grashof number differ from the Reynolds number?

20-7 Show that the volume expansion coefficient of an ideal gas is $\beta = 1/T$, where T is the absolute temperature.

20-8 Using its definition and the values listed in Table A-15, determine the volume expansion coefficient of saturated liquid

*Problems designated by a "C" are concept questions, and students are encouraged to answer them all. Problems with the icon  are solved using EES, and complete solutions together with parametric studies are included on the enclosed DVD. Problems with the icon  are comprehensive in nature, and are intended to be solved with a computer, preferably using the EES software that accompanies this text.

20-22 A 450-W cylindrical resistance heater is 0.75 m long and 0.5 cm in diameter. The resistance wire is placed horizontally in a fluid at 20°C. Determine the outer surface temperature of the resistance wire in steady operation if the fluid is (a) air and (b) water. Ignore any heat transfer by radiation. Use properties at 500°C for air and 40°C for water.

20-23 In a plant that manufactures canned aerosol paints, the cans are temperature-tested in water baths at 60°C before they are shipped to ensure that they withstand temperatures up to 55°C during transportation and shelving. The cans, moving on a conveyor, enter the open hot-water bath, which is 0.5 m deep, 1 m wide, and 3.5 m long, and move slowly in the hot water toward the other end. Some of the cans fail the test and explode in the water bath. The water container is made of sheet metal, and the entire container is at about the same temperature as the hot water. The emissivity of the outer surface of the container is 0.7. If the temperature of the surrounding air and surfaces is 20°C, determine the rate of heat loss from the four side surfaces of the container (disregard the top surface, which is open).

The water is heated electrically by resistance heaters, and the cost of electricity is \$0.085/kWh. If the plant operates 24 hours a day 365 days a year and thus 8760 hours a year, determine the annual cost of the heat losses from the container for this facility.

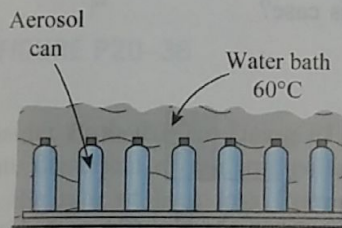


FIGURE P20-23

20-24 Reconsider Prob. 20-23. In order to reduce the heating cost of the hot water, it is proposed to insulate the side and bottom surfaces of the container with 5-cm-thick fiberglass insulation ($k = 0.035$ W/m·K) and to wrap the insulation with aluminum foil ($\epsilon = 0.1$) in order to minimize the heat loss by radiation. An estimate is obtained from a local insulation contractor, who proposes to do the insulation job for \$350, including materials and labor. Would you support this proposal? How long will it take for the insulation to pay for itself from the energy it saves?

20-25 Consider a 15-cm \times 20-cm printed circuit board (PCB) that has electronic components on one side. The board is placed in a room at 20°C. The heat loss from the back surface of the board is negligible. If the circuit board is dissipating 8 W of power in steady operation, determine the average temperature of the hot surface of the board, assuming the board is (a) vertical; (b) horizontal with hot surface facing up; and (c) horizontal with hot surface facing down. Take the

emissivity of the surface of the board to be 0.8 and assume the surrounding surfaces to be at the same temperature as the air in the room. *Answers: (a) 46.6°C, (b) 42.6°C, (c) 50.3°C*

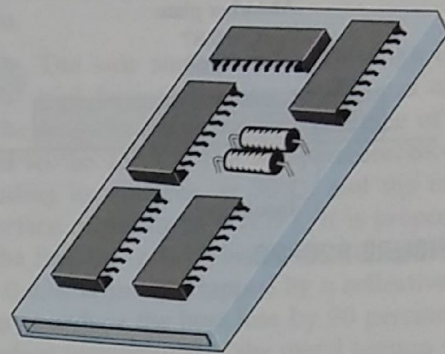



FIGURE P20-25


20-26  Reconsider Prob. 20-25. Using EES (or other) software, investigate the effects of the room temperature and the emissivity of the board on the temperature of the hot surface of the board for different orientations of the board. Let the room temperature vary from 5°C to 35°C and the emissivity from 0.1 to 1.0. Plot the hot surface temperature for different orientations of the board as the functions of the room temperature and the emissivity, and discuss the results.

20-27 Consider a vertical plate with length L , placed in quiescent air. If the film temperature is 20°C and the average Nusselt number in natural convection is of the form $Nu = CRa_L^n$, show that the average heat transfer coefficient can be expressed as

$$h = 1.51(\Delta T/L)^{1/4} \quad 10^4 < Ra_L < 10^9$$

$$h = 1.19\Delta T^{1/3} \quad 10^{10} < Ra_L < 10^{13}$$

20-28 A circular grill of diameter 0.25 m has an emissivity of 0.8. If the surface temperature is maintained at 150°C, determine the required electrical power when the room air and surroundings are at 30°C.

20-29  A manufacturer makes absorber plates that are 1.2 m \times 0.8 m in size for use in solar collectors. The back side of the plate is heavily insulated, while its front surface is coated with black chrome, which has an absorptivity of 0.87 for solar radiation and an emissivity of 0.09. Consider such a plate placed horizontally outdoors in calm air at 25°C. Solar radiation is incident on the plate at a rate of 600 W/m². Taking the effective sky temperature to be 10°C, determine the equilibrium temperature of the absorber plate. What would your answer be if the absorber plate is made of ordinary aluminum plate that has a solar absorptivity of 0.28 and an emissivity of 0.07?

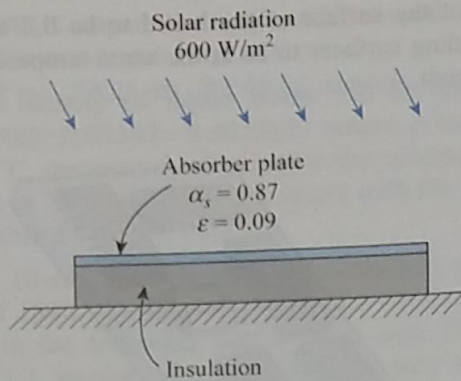


FIGURE P20-29

20-30 Repeat Prob. 20-29 for an aluminum plate painted black (solar absorptivity 0.98 and emissivity 0.98) and also for a plate painted white (solar absorptivity 0.26 and emissivity 0.90).

20-31 A room is to be heated by a coal-burning stove, which is a cylindrical cavity with an outer diameter of 50 cm and a height of 120 cm. The rate of heat loss from the room is estimated to be 1.5 kW when the air temperature in the room is maintained constant at 24°C. The emissivity of the stove surface is 0.85, and the average temperature of the surrounding wall surfaces is 14°C. Determine the surface temperature of the stove. Neglect the heat transfer from the bottom surface and take the heat transfer coefficient at the top surface to be the same as that on the side surface.

The heating value of the coal is 30,000 kJ/kg, and the combustion efficiency is 65 percent. Determine the amount of coal burned a day if the stove operates 14 hours a day.

20-32 Thick fluids such as asphalt and waxes and the pipes in which they flow are often heated in order to reduce the viscosity of the fluids and thus to reduce the pumping costs. Consider the flow of such a fluid through a 100-m-long pipe of outer diameter 30 cm in calm ambient air at 0°C. The pipe is heated electrically, and a thermostat keeps the outer surface

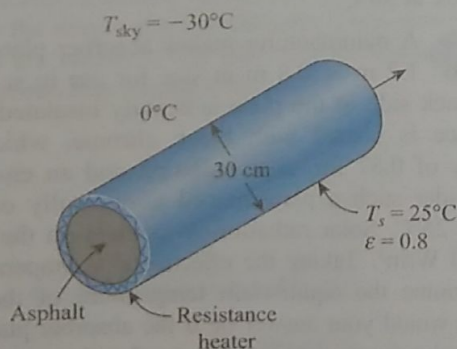


FIGURE P20-32

temperature of the pipe constant at 25°C. The emissivity of the outer surface of the pipe is 0.8, and the effective sky temperature is -30°C. Determine the power rating of the electric resistance heater, in kW, that needs to be used. Also, determine the cost of electricity associated with heating the pipe during a 15-hour period under the above conditions if the price of electricity is \$0.09/kWh. *Answers: 29.1 kW, \$39.3*

20-33 Reconsider Prob. 20-32. To reduce the heating cost of the pipe, it is proposed to insulate it with sufficiently thick fiberglass insulation ($k = 0.035$ W/m·K) wrapped with aluminum foil ($\epsilon = 0.1$) to cut down the heat losses by 85 percent. Assuming the pipe temperature to remain constant at 25°C, determine the thickness of the insulation that needs to be used. How much money will the insulation save during this 15-hour period? *Answers: 1.3 cm, \$33.4*

20-34 Consider a 1.2-m-high and 2-m-wide glass window with a thickness of 6 mm, thermal conductivity $k = 0.78$ W/m·K, and emissivity $\epsilon = 0.9$. The room and the walls that face the window are maintained at 25°C, and the average temperature of the inner surface of the window is measured to be 5°C. If the temperature of the outdoors is -5°C, determine (a) the convection heat transfer coefficient on the inner surface of the window, (b) the rate of total heat transfer through the window, and (c) the combined natural convection and radiation heat transfer coefficient on the outer surface of the window. Is it reasonable to neglect the thermal resistance of the glass in this case?

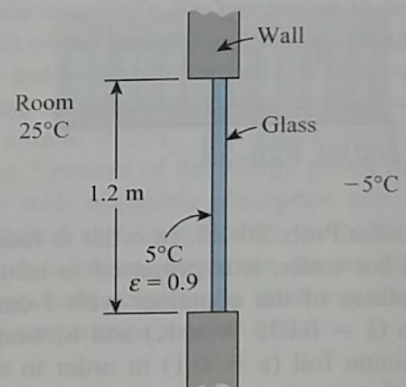


FIGURE P20-34

20-35 A 3-mm-diameter and 12-m-long electric wire is tightly wrapped with a 1.5-mm-thick plastic cover whose thermal conductivity and emissivity are $k = 0.20$ W/m·K and $\epsilon = 0.9$. Electrical measurements indicate that a current of 10 A passes through the wire and there is a voltage drop of 7 V along the wire. If the insulated wire is exposed to calm atmospheric air at $T_\infty = 30^\circ\text{C}$, determine the temperature at the interface of the wire and the plastic cover in steady operation. Take the surrounding surfaces to be at about the same temperature as the air.

20-36 During a visit to a plastic sheeting plant, it was observed that a 45-m-long section of a 2-in nominal (6.03-cm-outer-diameter) steam pipe extended from one end of the plant to the other with no insulation on it. The temperature measurements at several locations revealed that the average temperature of the exposed surfaces of the steam pipe was 170°C , while the temperature of the surrounding air was 20°C . The outer surface of the pipe appeared to be oxidized, and its emissivity can be taken to be 0.7. Taking the temperature of the surrounding surfaces to be 20°C also, determine the rate of heat loss from the steam pipe.

Steam is generated in a gas furnace that has an efficiency of 84 percent, and the plant pays \$1.10 per therm (1 therm = 105,500 kJ) of natural gas. The plant operates 24 hours a day 365 days a year, and thus 8760 hours a year. Determine the annual cost of the heat losses from the steam pipe for this facility.

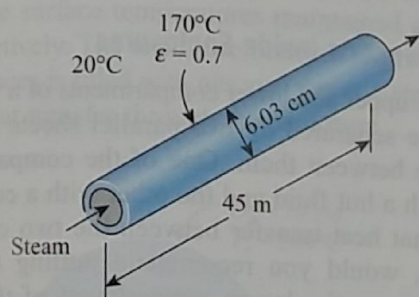


FIGURE P20-36


20-37 Reconsider Prob. 20-36. Using EES (or other) software, investigate the effect of the surface temperature of the steam pipe on the rate of heat loss from the pipe and the annual cost of this heat loss. Let the surface temperature vary from 100°C to 200°C . Plot the rate of heat loss and the annual cost as a function of the surface temperature, and discuss the results.

20-38 Reconsider Prob. 20-36. In order to reduce heat losses, it is proposed to insulate the steam pipe with 5-cm-thick fiberglass insulation ($k = 0.038 \text{ W/m}\cdot\text{K}$) and to wrap it with aluminum foil ($\epsilon = 0.1$) in order to minimize the radiation losses. Also, an estimate is obtained from a local insulation contractor, who proposed to do the insulation job for \$750, including materials and labor. Would you support this proposal? How long will it take for the insulation to pay for itself from the energy it saves? Assume the temperature of the steam pipe to remain constant at 170°C .

20-39 A 50-cm \times 50-cm circuit board that contains 121 square chips on one side is to be cooled by combined natural convection and radiation by mounting it on a vertical surface in a room at 25°C . Each chip dissipates 0.18 W of power, and the emissivity of the chip surfaces is 0.7. Assuming the heat transfer from the back side of the circuit board to be negligible, and the temperature of the surrounding surfaces to be the same as

the air temperature of the room, determine the surface temperature of the chips. *Answer:* 36.2°C

20-40 Repeat Prob. 20-39 assuming the circuit board to be positioned horizontally with (a) chips facing up and (b) chips facing down.

20-41  The side surfaces of a 3-m-high cubic industrial furnace burning natural gas are not insulated, and the temperature at the outer surface of this section is measured to be 110°C . The temperature of the furnace room, including its surfaces, is 30°C , and the emissivity of the outer surface of the furnace is 0.7. It is proposed that this section of the furnace wall be insulated with glass wool insulation ($k = 0.038 \text{ W/m}\cdot\text{K}$) wrapped by a reflective sheet ($\epsilon = 0.2$) in order to reduce the heat loss by 90 percent. Assuming the outer surface temperature of the metal section still remains at about 110°C , determine the thickness of the insulation that needs to be used.

The furnace operates continuously throughout the year and has an efficiency of 78 percent. The price of the natural gas is \$1.10/therm (1 therm = 105,500 kJ of energy content). If the installation of the insulation will cost \$550 for materials and labor, determine how long it will take for the insulation to pay for itself from the energy it saves.

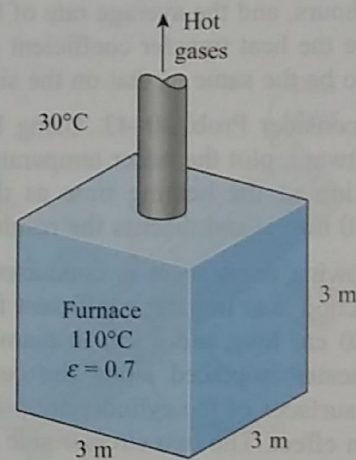


FIGURE P20-41

20-42 A 1.5-m-diameter, 4-m-long cylindrical propane tank is initially filled with liquid propane, whose density is 581 kg/m^3 . The tank is exposed to the ambient air at 25°C in calm weather. The outer surface of the tank is polished so that the radiation heat transfer is negligible. Now a crack develops at the top of the tank, and the pressure inside drops to 1 atm while the temperature drops to -42°C , which is the boiling temperature of propane at 1 atm. The heat of vaporization of propane at 1 atm is 425 kJ/kg. The propane is slowly vaporized as a result of the heat transfer from the ambient air into the tank, and the propane vapor escapes the tank at -42°C through the crack. Assuming the propane tank to be at about

the average surface temperature of the cylinder is measured to be 120°C in the 20°C room air when steady operation is reached, determine the natural convection heat transfer coefficient. If the emissivity of the outer surface of the cylinder is 0.1 and a 5 percent error is acceptable, do you think we used to do any correction for the radiation effect? Assume the surrounding surfaces to be at 20°C also.

20-46 The water in a 40-L tank is to be heated from 15°C to 45°C by a 6-cm-diameter spherical heater whose surface temperature is maintained at 85°C . Determine how long the heater should be kept on.

20-47 Consider a cylinder with a length of 15 cm and a diameter of 10 cm. The cylinder has a surface temperature of 43°C , while the room air temperature is 17°C . Determine whether placing the cylinder horizontally or vertically would achieve higher heat transfer rate.

Natural Convection inside Enclosures

20-48 The upper and lower compartments of a well-insulated container are separated by two parallel sheets of glass with an air space between them. One of the compartments is to be filled with a hot fluid and the other with a cold fluid. If it is desired that heat transfer between the two compartments be minimal, would you recommend putting the hot fluid into the upper or the lower compartment of the container? Why?

20-49C Someone claims that the air space in a double-pane window enhances the heat transfer from a house because of the natural convection currents that occur in the air space and recommends that the double-pane window be replaced by a single sheet of glass whose thickness is equal to the sum of the thicknesses of the two glasses of the double-pane window to save energy. Do you agree with this claim?

20-50C Consider a double-pane window consisting of two glass sheets separated by a 1-cm-wide air space. Someone suggests inserting a thin vinyl sheet in the middle of the two glasses to form two 0.5-cm-wide compartments in the window in order to reduce natural convection heat transfer through the window. From a heat transfer point of view, would you be in favor of this idea to reduce heat losses through the window?

20-51C What does the effective conductivity of an enclosure represent? How is the ratio of the effective conductivity to thermal conductivity related to the Nusselt number?

20-52 Consider a 3-m-high rectangular enclosure consisting of two surfaces separated by a 0.1-m air gap at 1 atm. If the surface temperatures across the air gap are 30°C and -10°C , determine the ratio of the heat transfer rate for the horizontal orientation (with hotter surface at the bottom) to that for vertical orientation. *Answer: 1.66*

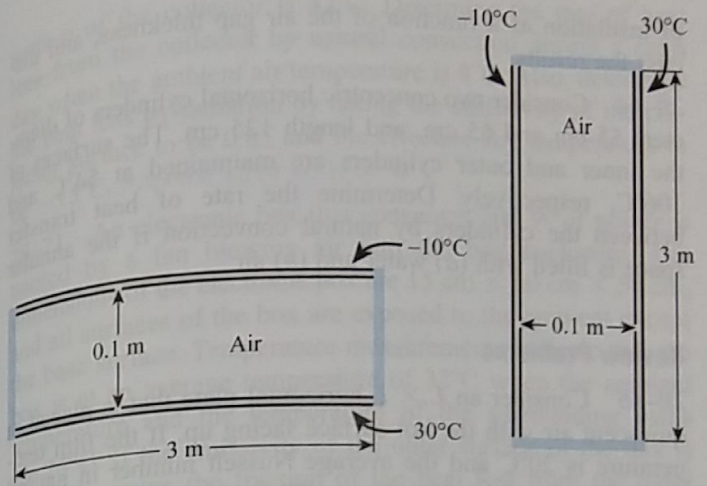


FIGURE P20-52

20-53 Two concentric spheres with radii of 5 cm and 10 cm are having the surface temperatures maintained at 100°C and 200°C , respectively. The enclosure between the two concentric spherical surfaces is filled with nitrogen gas at 1 atm. Determine the rate of heat transfer through the enclosure.

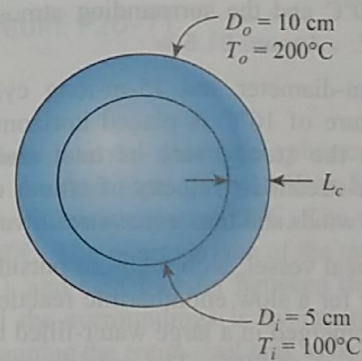


FIGURE P20-53

20-54 Show that the thermal resistance of a rectangular enclosure can be expressed as $R = L_c / (Ak Nu)$, where k is the thermal conductivity of the fluid in the enclosure.

20-55 A vertical 1.5-m-high and 3.0-m-wide enclosure consists of two surfaces separated by a 0.4-m air gap at atmospheric pressure. If the surface temperatures across the air gap are measured to be 280 K and 336 K and the surface emissivities to be 0.15 and 0.90, determine the fraction of heat transferred through the enclosure by radiation. *Answer: 0.30*

20-56 A vertical 1.5-m-high, 2.8-m-wide double-pane window consists of two layers of glass separated by a 2.0-cm air gap at atmospheric pressure. The room temperature is 26°C while the inner glass temperature is 18°C . Disregarding radiation heat transfer, determine the temperature of the outer glass layer and the rate of heat loss through the window by natural convection.

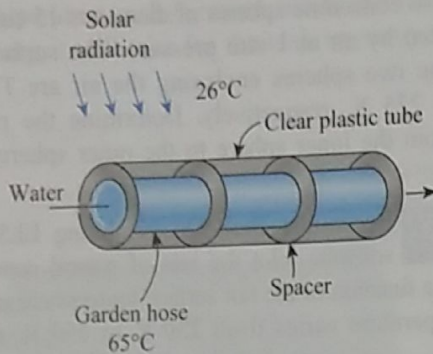



FIGURE P20-60

20-61  Reconsider Prob. 20-60. Using EES (or other) software, plot the rate of heat loss from the water by natural convection as a function of the ambient air temperature as the temperature varies from 4°C to 40°C, and discuss the results.

20-62 A vertical 1.5-m-high and 1.8-m-wide double-pane window consists of two sheets of glass separated by a 2-cm air gap at atmospheric pressure. If the glass surface temperatures across the air gap are measured to be 18°C and 4°C, determine the rate of heat transfer through the window by (a) natural convection and (b) radiation. Also, determine the R -value of insulation of this window such that multiplying the inverse of the R -value by the surface area and the temperature difference gives the total rate of heat transfer through the window. The effective emissivity for use in radiation calculations between two large parallel glass plates can be taken to be 0.82.

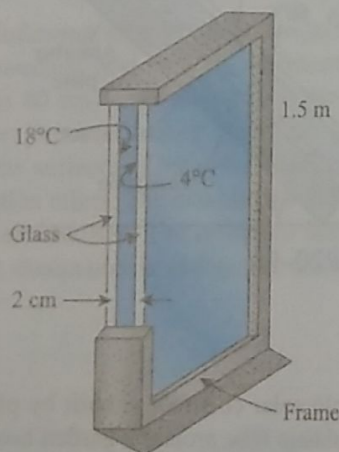



FIGURE P20-62

20-63  Reconsider Prob. 20-62. Using EES (or other) software, investigate the effect of the air gap thickness on the rates of heat transfer by natural convection and radiation, and the R -value of insulation. Let the air gap thickness vary from 0.5 cm to 5 cm. Plot the rates of heat transfer by natural convection and radiation, and the R -value

of insulation as a function of the air gap thickness, and discuss the results.

20-64 Consider two concentric horizontal cylinders of diameters 55 cm and 65 cm, and length 125 cm. The surfaces of the inner and outer cylinders are maintained at 54°C and 106°C, respectively. Determine the rate of heat transfer between the cylinders by natural convection if the annular space is filled with (a) water and (b) air.

Review Problems

20-65 Consider an $L \times L$ horizontal plate that is placed in quiescent air with the hot surface facing up. If the film temperature is 20°C and the average Nusselt number in natural convection is of the form $Nu = C Ra_L^n$, show that the average heat transfer coefficient can be expressed as

$$h = 1.95(\Delta T/L)^{1/4} \quad 10^4 < Ra_L < 10^7$$

$$h = 1.79\Delta T^{1/3} \quad 10^7 < Ra_L < 10^{11}$$

20-66 A plate (0.5 m \times 0.5 m) is inclined at an angle of 30°. The top surface of the plate is well insulated. Estimate the rate of heat loss from the plate when the bottom surface is maintained at 60°C and the surrounding atmospheric quiescent air is at 0°C. *Answer: 81.5 W*

20-67 A 12-cm-diameter and 15-m-long cylinder with a surface temperature of 10°C is placed horizontally in air at 40°C. Calculate the steady rate of heat transfer for the cases of (a) free-stream air velocity of 10 m/s due to normal winds and (b) no winds and thus a free-stream velocity of zero.

20-68 A spherical vessel, with 30.0-cm outside diameter, is used as a reactor for a slow endothermic reaction. The vessel is completely submerged in a large water-filled tank, held at a constant temperature of 30°C. The outside surface temperature of the vessel is 20°C. Calculate the rate of heat transfer in steady operation for the following cases: (a) the water in the tank is still, (b) the water in the tank is still (as in part a), however, the buoyancy force caused by the difference in water density is assumed to be negligible, and (c) the water in the tank is circulated at an average velocity of 20 cm/s.

20-69 Hot water is flowing at an average velocity of 1.2 m/s through a cast iron pipe ($k = 52 \text{ W/m}\cdot\text{°C}$) whose inner and outer diameters are 2.5 cm and 3 cm, respectively. The pipe passes through a 15-m-long section of a basement whose temperature is 15°C. The emissivity of the outer surface of the pipe is 0.5, and the walls of the basement are also at about 15°C. If the inlet temperature of the water is 65°C and the heat transfer coefficient on the inner surface of the pipe is 170 $\text{W/m}^2\cdot\text{°C}$, determine the temperature drop of water as it passes through the basement.

20-70 Consider a flat-plate solar collector placed horizontally on the flat roof of a house. The collector is 1.5 m wide and 4.5 m long, and the average temperature of the exposed