

# PROPERTY TABLES AND CHARTS (SI UNITS)

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TABLE A-1

Molar mass, gas constant, and ideal-gas specific heats of some substances

Substance	Molar Mass $M$ , kg/kmol	Gas Constant $R$ , kJ/kg·K*	Specific Heat Data at 25°C		
			$c_p$ , kJ/kg·K	$c_v$ , kJ/kg·K	$k = c_p/c_v$
Air	28.97	0.2870	1.005	0.7180	1.400
Ammonia, NH <sub>3</sub>	17.03	0.4882	2.093	1.605	1.304
Argon, Ar	39.95	0.2081	0.5203	0.3122	1.667
Bromine, Br <sub>2</sub>	159.81	0.05202	0.2253	0.1732	1.300
Isobutane, C <sub>4</sub> H <sub>10</sub>	58.12	0.1430	1.663	1.520	1.094
<i>n</i> -Butane, C <sub>4</sub> H <sub>10</sub>	58.12	0.1430	1.694	1.551	1.092
Carbon dioxide, CO <sub>2</sub>	44.01	0.1889	0.8439	0.6550	1.288
Carbon monoxide, CO	28.01	0.2968	1.039	0.7417	1.400
Chlorine, Cl <sub>2</sub>	70.905	0.1173	0.4781	0.3608	1.325
Chlorodifluoromethane (R-22), CHClF <sub>2</sub>	86.47	0.09615	0.6496	0.5535	1.174
Ethane, C <sub>2</sub> H <sub>6</sub>	30.070	0.2765	1.744	1.468	1.188
Ethylene, C <sub>2</sub> H <sub>4</sub>	28.054	0.2964	1.527	1.231	1.241
Fluorine, F <sub>2</sub>	38.00	0.2187	0.8237	0.6050	1.362
Helium, He	4.003	2.077	5.193	3.116	1.667
<i>n</i> -Heptane, C <sub>7</sub> H <sub>16</sub>	100.20	0.08297	1.649	1.566	1.053
<i>n</i> -Hexane, C <sub>6</sub> H <sub>14</sub>	86.18	0.09647	1.654	1.558	1.062
Hydrogen, H <sub>2</sub>	2.016	4.124	14.30	10.18	1.405
Krypton, Kr	83.80	0.09921	0.2480	0.1488	1.667
Methane, CH <sub>4</sub>	16.04	0.5182	2.226	1.708	1.303
Neon, Ne	20.183	0.4119	1.030	0.6180	1.667
Nitrogen, N <sub>2</sub>	28.01	0.2968	1.040	0.7429	1.400
Nitric oxide, NO	30.006	0.2771	0.9992	0.7221	1.384
Nitrogen dioxide, NO <sub>2</sub>	46.006	0.1889	0.8060	0.6171	1.306
Oxygen, O <sub>2</sub>	32.00	0.2598	0.9180	0.6582	1.395
<i>n</i> -Pentane, C <sub>5</sub> H <sub>12</sub>	72.15	0.1152	1.664	1.549	1.074
Propane, C <sub>3</sub> H <sub>8</sub>	44.097	0.1885	1.669	1.480	1.127
Propylene, C <sub>3</sub> H <sub>6</sub>	42.08	0.1976	1.531	1.333	1.148
Steam, H <sub>2</sub> O	18.015	0.4615	1.865	1.403	1.329
Sulfur dioxide, SO <sub>2</sub>	64.06	0.1298	0.6228	0.4930	1.263
Tetrachloromethane, CCl <sub>4</sub>	153.82	0.05405	0.5415	0.4875	1.111
Tetrafluoroethane (R-134a), C <sub>2</sub> H <sub>2</sub> F <sub>4</sub>	102.03	0.08149	0.8334	0.7519	1.108
Trifluoroethane (R-143a), C <sub>2</sub> H <sub>3</sub> F <sub>3</sub>	84.04	0.09893	0.9291	0.8302	1.119
Xenon, Xe	131.30	0.06332	0.1583	0.09499	1.667

\*The unit kJ/kg·K is equivalent to kPa·m<sup>3</sup>/kg·K. The gas constant is calculated from  $R = R_u/M$ , where  $R_u = 8.31447$  kJ/kmol·K is the universal gas constant and  $M$  is the molar mass.

Source: Specific heat values are obtained primarily from the property routines prepared by The National Institute of Standards and Technology (NIST), Gaithersburg, MD.

TABLE A-2

## Boiling and freezing point properties

Substance	Boiling Data at 1 atm		Freezing Data		Liquid Properties		
	Normal Boiling Point, °C	Latent Heat of Vaporization $h_{fg}$ , kJ/kg	Freezing Point, °C	Latent Heat of Fusion $h_{if}$ , kJ/kg	Temperature, °C	Density $\rho$ , kg/m <sup>3</sup>	Specific Heat $c_p$ , kJ/kg·K
Ammonia	-33.3	1357	-77.7	322.4	-33.3 -20 0 25	682 665 639 602	4.43 4.52 4.60 4.80
Argon	-185.9	161.6	-189.3	28	-185.6	1394	1.14
Benzene	80.2	394	5.5	126	20	879	1.72
Brine (20% sodium chloride by mass)	103.9	—	-17.4	—	20	1150	3.11
<i>n</i> -Butane	-0.5	385.2	-138.5	80.3	-0.5	601	2.31
Carbon dioxide	-78.4*	230.5 (at 0°C)	-56.6	—	0	298	0.59
Ethanol	78.2	838.3	-114.2	109	25	783	2.46
Ethyl alcohol	78.6	855	-156	108	20	789	2.84
Ethylene glycol	198.1	800.1	-10.8	181.1	20	1109	2.84
Glycerin	179.9	974	18.9	200.6	20	1261	2.32
Helium	-268.9	22.8	—	—	-268.9	146.2	22.8
Hydrogen	-252.8	445.7	-259.2	59.5	-252.8	70.7	10.0
Isobutane	-11.7	367.1	-160	105.7	-11.7	593.8	2.28
Kerosene	204–293	251	-24.9	—	20	820	2.00
Mercury	356.7	294.7	-38.9	11.4	25	13,560	0.139
Methane	-161.5	510.4	-182.2	58.4	-161.5 -100 25	423 301 787	3.49 5.79 2.55
Methanol	64.5	1100	-97.7	99.2	25	787	2.55
Nitrogen	-195.8	198.6	-210	25.3	-195.8 -160 20 25	809 596 703 910	2.06 2.97 2.10 1.80
Octane	124.8	306.3	-57.5	180.7	20	703	2.10
Oil (light)	—	—	—	—	25	910	1.80
Oxygen	-183	212.7	-218.8	13.7	-183	1141	1.71
Petroleum	—	230–384	—	—	20	640	2.0
Propane	-42.1	427.8	-187.7	80.0	-42.1 0 50 50	581 529 449 1443	2.25 2.53 3.13 1.23
Refrigerant-134a	-26.1	216.8	-96.6	—	-50 -26.1 0 25	1443 1374 1295 1207	1.23 1.27 1.34 1.43
Water	100	2257	0.0	333.7	0 25 50 75 100	1000 997 988 975 958	4.22 4.18 4.18 4.19 4.22

\*Sublimation temperature. (At pressures below the triple-point pressure of 518 kPa, carbon dioxide exists as a solid or gas. Also, the freezing-point temperature of carbon dioxide is the triple-point temperature of -56.5°C.)

**TABLE A-3**

Properties of solid metals

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k(\text{W/m}\cdot\text{K})/c_p(\text{J/kg}\cdot\text{K})$					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg·K	$k$ W/m·K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Aluminum:											
Pure	933	2702	903	237	97.1	302	237	240	231	218	
Alloy 2024-T6 (4.5% Cu, 1.5% Mg, 0.6% Mn)	775	2770	875	177	73.0	482	798	949	1033	1146	
Alloy 195, Cast (4.5% Cu)						65	163	186	186		
Beryllium	1550	2790	883	168	68.2	473	787	925	1042		
Bismuth	545	1850	1825	200	59.2	990	301	161	126	106	90.8
Boron	2573	9780	122	7.86	6.59	203	1114	2191	2604	2823	3018
Cadmium	594	2500	1107	27.0	9.76	112	120	127			
Chromium	2118	8650	231	96.8	48.4	190	55.5	16.8	10.6	9.60	9.85
Cobalt	1769	7160	449	93.7	29.1	128	600	1463	1892	2160	2338
Copper:						203	99.3	94.7			
Pure	1358	8933	385	401	117	159	111	90.9	80.7	71.3	65.4
Commercial bronze (90% Cu, 10% Al)	1293	8800	420	52	14	192	384	484	542	581	616
Phosphor gear bronze (89% Cu, 11% Sn)	1104	8780	355	54	17	167	122	85.4	67.4	58.2	52.1
Cartridge brass (70% Cu, 30% Zn)	1188	8530	380	110	33.9	236	379	450	503	550	628
Constantan (55% Cu, 45% Ni)	1493	8920	384	23	6.71	17	19				
Germanium	1211	5360	322	59.9	34.7	237	362				
Gold	1336	19,300	129	317	127	232	96.8	43.2	27.3	19.8	17.4
Iridium	2720	22,500	130	147	50.3	190	290	337	348	357	375
Iron:						327	323	311	298	284	270
Pure	1810	7870	447	80.2	23.1	109	124	131	135	140	145
Armco (99.75% pure)		7870	447	72.7	20.7	172	153	144	138	132	126
Carbon steels:						90	122	133	138	144	153
Plain carbon (Mn ≤ 1% Si ≤ 0.1%)		7854	434	60.5	17.7	134	94.0	69.5	54.7	43.3	32.8
AISI 1010		7832	434	63.9	18.8	216	384	490	574	680	975
Carbon- silicon (Mn ≤ 1% 0.1% < Si ≤ 0.6%)		7817	446	51.9	14.9	215	384	490	574	680	975
								56.7	48.0	39.2	30.0
								487	559	685	1169
								58.7	48.8	39.2	31.3
								487	559	685	1168
								49.8	44.0	37.4	29.3
								501	582	699	971

TABLE A-3

Properties of solid metals (Continued)

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k(\text{W/m}\cdot\text{K})/c_p(\text{J/kg}\cdot\text{K})$					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg·K	$k$ W/m·K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Carbon–manganese–silicon (1% < Mn < 1.65% 0.1% < Si < 0.6%)		8131	434	41.0	11.6			42.2 487	39.7 559	35.0 685	27.6 1090
Chromium (low) steels: $\frac{1}{2}$ Cr– $\frac{1}{4}$ Mo–Si (0.18% C, 0.65% Cr, 0.23% Mo, 0.6% Si)		7822	444	37.7	10.9			38.2 492	36.7 575	33.3 688	26.9 969
1 Cr– $\frac{1}{2}$ Mo (0.16% C, 1% Cr, 0.54% Mo, 0.39% Si)		7858	442	42.3	12.2			42.0 492	39.1 575	34.5 688	27.4 969
1 Cr–V (0.2% C, 1.02% Cr, 0.15% V)		7836	443	48.9	14.1			46.8 492	42.1 575	36.3 688	28.2 969
Stainless steels: AISI 302		8055	480	15.1	3.91			17.3 512	20.0 559	22.8 585	25.4 606
AISI 304	1670	7900	477	14.9	3.95	9.2 272	12.6 402	16.6 515	19.8 557	22.6 582	25.4 611
AISI 316		8238	468	13.4	3.48			15.2 504	18.3 550	21.3 576	24.2 602
AISI 347		7978	480	14.2	3.71			15.8 513	18.9 559	21.9 585	24.7 606
Lead	601	11,340	129	35.3	24.1	39.7	36.7	34.0 118	31.4 125	132 146	142 1267
Magnesium	923	1740	1024	156	87.6	169	159	153 649	149 934	146 1074	1170 1267
Molybdenum	2894	10,240	251	138	53.7	179 141	143 224	134 261	126 275	118 285	112 295
Nickel: Pure	1728	8900	444	90.7	23.0	164 232	107 383	80.2 485	65.6 592	67.6 530	71.8 562
Nichrome (80% Ni, 20% Cr)	1672	8400	420	12	3.4			14 480	16 525	21 545	
Inconel X-750 (73% Ni, 15% Cr, 6.7% Fe)	1665	8510	439	11.7	3.1	8.7	10.3	13.5 372	17.0 510	20.5 546	24.0 626
Niobium	2741	8570	265	53.7	23.6	55.2 188	52.6 249	55.2 274	58.2 283	61.3 292	64.4 301
Palladium	1827	12,020	244	71.8	24.5	76.5 168	71.6 227	73.6 251	79.7 261	86.9 271	94.2 281
Platinum: Pure	2045	21,450	133	71.6	25.1	77.5 100	72.6 125	71.8 136	73.2 141	75.6 146	78.7 152
Alloy 60Pt–40Rh (60% Pt, 40% Rh)	1800	16,630	162	47	17.4			52 —	59 —	65 —	69 —
Rhenium	3453	21,100	136	47.9	16.7	58.9 97	51.0 127	46.1 139	44.2 145	44.1 151	44.6 156
Rhodium	2236	12,450	243	150	49.6	186 147	154 220	146 253	136 274	127 293	121 311

TABLE A-3

Properties of solid metals (Concluded)

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k(\text{W/m}\cdot\text{K})/c_p(\text{J/kg}\cdot\text{K})$					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg·K	$k$ W/m·K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Silicon	1685	2330	712	148	89.2	884	264	98.9	61.9	42.4	31.2
Silver	1235	10,500	235	429	174	259	556	790	867	913	946
						444	430	425	412	396	379
Tantalum	3269	16,600	140	57.5	24.7	187	225	239	250	262	277
						59.2	57.5	57.8	58.6	59.4	60.2
Thorium	2023	11,700	118	54.0	39.1	110	133	144	146	149	152
						59.8	54.6	54.5	55.8	56.9	56.9
Tin	505	7310	227	66.6	40.1	99	112	124	134	145	156
						85.2	73.3	62.2			
Titanium	1953	4500	522	21.9	9.32	188	215	243			
						30.5	24.5	20.4	19.4	19.7	20.7
Tungsten	3660	19,300	132	174	68.3	300	465	551	591	633	675
						208	186	159	137	125	118
Uranium	1406	19,070	116	27.6	12.5	87	122	137	142	146	148
						21.7	25.1	29.6	34.0	38.8	43.9
Vanadium	2192	6100	489	30.7	10.3	94	108	125	146	176	180
						35.8	31.3	31.3	33.3	35.7	38.2
Zinc	693	7140	389	116	41.8	258	430	515	540	563	597
						117	118	111	103		
Zirconium	2125	6570	278	22.7	12.4	297	367	402	436		
						33.2	25.2	21.6	20.7	21.6	23.7
						205	264	300	332	342	362

Source: Frank P. Incropera and David P. DeWitt, *Fundamentals of Heat and Mass Transfer*, 3rd ed., 1990.

TABLE A-4

## Properties of solid nonmetals

Composition	Melting Point, K	Properties at 300 K				Properties at Various Temperatures (K), $k(\text{W/m}\cdot\text{K})/c_p(\text{J/kg}\cdot\text{K})$					
		$\rho$ kg/m <sup>3</sup>	$c_p$ J/kg·K	$k$ W/m·K	$\alpha \times 10^6$ m <sup>2</sup> /s	100	200	400	600	800	1000
Aluminum oxide, sapphire	2323	3970	765	46	15.1	450	82	32.4	18.9	13.0	10.5
Aluminum oxide, polycrystalline	2323	3970	765	36.0	11.9	—	—	940	1110	1180	1225
Beryllium oxide	2725	3000	1030	272	88.0	133	55	26.4	15.8	10.4	7.85
Boron	2573	2500	1105	27.6	9.99	—	—	940	1110	1180	1225
Boron fiber epoxy (30% vol.) composite	590	2080						196	111	70	47
$k$ ,    to fibers				2.29		2.10	2.23	1350	1690	1865	1975
$k$ , $\perp$ to fibers				0.59		0.37	0.49	18.7	11.3	8.1	6.3
$c_p$			1122			364	757	1490	1880	2135	2350
Carbon, amorphous	1500	1950	—	1.60	—	0.67	1.18	1.89	21.9	2.37	2.53
Diamond, type IIa insulator	—	3500	509	2300		10,000	4000	1540	—	—	—
Graphite, pyrolytic	2273	2210				21	194	853			
$k$ ,    to layers				1950		4970	3230	1390	892	667	534
$k$ , $\perp$ to layers				5.70		16.8	9.23	4.09	2.68	2.01	1.60
$c_p$			709			136	411	992	1406	1650	1793
Graphite fiber epoxy (25% vol.) composite	450	1400									
$k$ , heat flow    to fibers				11.1		5.7	8.7	13.0			
$k$ , heat flow $\perp$ to fibers			0.87		0.46	0.68	1.1				
$c_p$			935			337	642	1216			
Pyroceram, Corning 9606	1623	2600	808	3.98	1.89	5.25	4.78	3.64	3.28	3.08	2.96
Silicon carbide	3100	3160	675	490	230	—	—	908	1038	1122	1197
Silicon dioxide, crystalline (quartz)	1883	2650						880	1050	1135	1195
$k$ ,    to $c$ -axis				10.4		39	16.4	7.6	5.0	4.2	
$k$ , $\perp$ to $c$ -axis				6.21		20.8	9.5	4.70	3.4	3.1	
$c_p$			745			—	—	885	1075	1250	
Silicon dioxide, polycrystalline (fused silica)	1883	2220	745	1.38	0.834	0.69	1.14	1.51	1.75	2.17	2.87
Silicon nitride	2173	2400	691	16.0	9.65	—	—	905	1040	1105	1155
Sulfur	392	2070	708	0.206	0.141	—	578	13.9	11.3	9.88	8.76
Thorium dioxide	3573	9110	235	13	6.1	0.165	0.185	778	937	1063	1155
Titanium dioxide, polycrystalline	2133	4157	710	8.4	2.8			403	606		
								10.2	6.6	4.7	3.68
								255	274	285	295
								7.01	5.02	8.94	3.46
								805	880	910	930

TABLE A-5

Properties of building materials (at a mean temperature of 24°C)

Material	Thickness, <i>L</i> mm	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, <i>k</i> W/m·K	Specific Heat, $c_p$ kJ/kg·K	<i>R</i> -value (for listed thickness, <i>L/k</i> ), K·m <sup>2</sup> /W
<b>Building Boards</b>					
Asbestos-cement board	6 mm	1922	—	1.00	0.011
Gypsum of plaster board	10 mm	800	—	1.09	0.057
	13 mm	800	—	—	0.078
	—	—	—	—	—
Plywood (Douglas fir)	—	545	0.12	1.21	—
	6 mm	545	—	1.21	0.055
	10 mm	545	—	1.21	0.083
	13 mm	545	—	1.21	0.110
	20 mm	545	—	1.21	0.165
Insulated board and sheathing (regular density)	13 mm	288	—	1.30	0.232
	20 mm	288	—	1.30	0.359
Hardboard (high density, standard tempered)	—	1010	0.14	1.34	—
Particle board:					
Medium density	—	800	0.14	1.30	—
Underlayment	16 mm	640	—	1.21	0.144
Wood subfloor	20 mm	—	—	1.38	0.166
<b>Building Membrane</b>					
Vapor-permeable felt	—	—	—	—	0.011
Vapor seal (2 layers of mopped 0.73 kg <sup>2</sup> /m <sup>2</sup> felt)	—	—	—	—	0.021
<b>Flooring Materials</b>					
Carpet and fibrous pad	—	—	—	1.42	0.367
Carpet and rubber pad	—	—	—	1.38	0.217
Tile (asphalt, linoleum, vinyl)	—	—	—	1.26	0.009
<b>Masonry Materials</b>					
<i>Masonry units:</i>					
Brick, common	—	1922	0.72	—	—
Brick, face	—	2082	1.30	—	—
Brick, fire clay	—	2400	1.34	—	—
	—	1920	0.90	0.79	—
	—	1120	0.41	—	—
Concrete blocks (3 oval cores, sand and gravel aggregate)	100 mm	—	0.77	—	0.13
	200 mm	—	1.0	—	0.20
	300 mm	—	1.30	—	0.23
<i>Concretes:</i>					
Lightweight aggregates, (including expanded shale, clay, or slate; expanded slags; cinders; pumice; and scoria)	—	1920	1.1	—	—
	—	1600	0.79	0.84	—
	—	1280	0.54	0.84	—
	—	960	0.33	—	—
	940	0.18	—	—	—
Cement/lime, mortar, and stucco	—	1920	1.40	—	—
	—	1280	0.65	—	—
Stucco	—	1857	0.72	—	—



TABLE A-5

Properties of building materials (at a mean temperature of 24°C) (Concluded)

Material	Thickness, <i>L</i> mm	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, <i>k</i> W/m·K	Specific Heat, $c_p$ kJ/kg·K	<i>R</i> -value (for listed thickness, <i>L/k</i> ), K·m <sup>2</sup> /W
<b>Roofing</b>					
Asbestos-cement shingles		1900	—	1.00	0.037
Asphalt roll roofing		1100	—	1.51	0.026
Asphalt shingles		1100	—	1.26	0.077
Built-in roofing	10 mm	1100	—	1.46	0.058
Slate	13 mm	—	—	1.26	0.009
Wood shingles (plain and plastic/film faced)		—	—	1.30	0.166
<b>Plastering Materials</b>					
Cement plaster, sand aggregate	19 mm	1860	0.72	0.84	0.026
Gypsum plaster:					
Lightweight aggregate	13 mm	720	—	—	0.055
Sand aggregate	13 mm	1680	0.81	0.84	0.016
Perlite aggregate	—	720	0.22	1.34	—
<b>Siding Material (on flat surfaces)</b>					
Asbestos-cement shingles	—	1900	—	—	0.037
Hardboard siding	11 mm	—	—	1.17	0.12
Wood (drop) siding	25 mm	—	—	1.30	0.139
Wood (plywood) siding lapped	10 mm	—	—	1.21	0.111
Aluminum or steel siding (over sheeting):					
Hollow backed	10 mm	—	—	1.22	0.11
Insulating-board backed	10 mm	—	—	1.34	0.32
Architectural glass	—	2530	1.0	0.84	0.018
<b>Woods</b>					
Hardwoods (maple, oak, etc.)	—	721	0.159	1.26	—
Softwoods (fir, pine, etc.)	—	513	0.115	1.38	—
<b>Metals</b>					
Aluminum (1100)	—	2739	222	0.896	—
Steel, mild	—	7833	45.3	0.502	—
Steel, Stainless	—	7913	15.6	0.456	—

Source: Table A-5 and A-6 are adapted from ASHRAE, *Handbook of Fundamentals* (Atlanta, GA: American Society of Heating, Refrigerating, and Air-Conditioning Engineers, 1993), Chap. 22, Table 4. Used with permission.

TABLE A-6

Properties of insulating materials (at a mean temperature of 24°C)

Material	Thickness, $L$ mm	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Specific Heat, $c_p$ kJ/kg·K	$R$ -value (for listed thickness, $L/k$ ), K·m <sup>2</sup> /W
<b>Blanket and Batt</b>					
Mineral fiber (fibrous form processed from rock, slag, or glass)	50 to 70 mm	4.8–32	—	0.71–0.96	1.23
	75 to 90 mm	4.8–32	—	0.71–0.96	1.94
	135 to 165 mm	4.8–32	—	0.71–0.96	3.32
<b>Board and Slab</b>					
Cellular glass		136	0.055	1.0	—
Glass fiber (organic bonded)		64–144	0.036	0.96	—
Expanded polystyrene (molded beads)		16	0.040	1.2	—
Expanded polyurethane ( $R$ -11 expanded)		24	0.023	1.6	—
Expanded perlite (organic bonded)		16	0.052	1.26	—
Expanded rubber (rigid)		72	0.032	1.68	—
Mineral fiber with resin binder		240	0.042	0.71	—
Cork		120	0.039	1.80	—
<b>Sprayed or Formed in Place</b>					
Polyurethane foam		24–40	0.023–0.026	—	—
Glass fiber		56–72	0.038–0.039	—	—
Urethane, two-part mixture (rigid foam)		70	0.026	1.045	—
Mineral wool granules with asbestos/inorganic binders (sprayed)		190	0.046	—	—
<b>Loose Fill</b>					
Mineral fiber (rock, slag, or glass)	~75 to 125 mm	9.6–32	—	0.71	1.94
	~165 to 222 mm	9.6–32	—	0.71	3.35
	~191 to 254 mm	—	—	0.71	3.87
	~185 mm	—	—	0.71	5.28
Silica aerogel		122	0.025	—	—
Vermiculite (expanded)		122	0.068	—	—
Perlite, expanded		32–66	0.039–0.045	1.09	—
Sawdust or shavings		128–240	0.065	1.38	—
Cellulosic insulation (milled paper or wood pulp)		37–51	0.039–0.046	—	—
<b>Roof Insulation</b>					
Cellular glass	—	144	0.058	1.0	—
Preformed, for use above deck	13 mm	—	—	1.0	0.24
	25 mm	—	—	2.1	0.49
	50 mm	—	—	3.9	0.93
<b>Reflective Insulation</b>					
Silica powder (evacuated)		160	0.0017	—	—
Aluminum foil separating fluffy glass mats; 10–12 layers (evacuated); for cryogenic applications (150 K)		40	0.00016	—	—
Aluminum foil and glass paper laminate; 75–150 layers (evacuated); for cryogenic applications (150 K)		120	0.000017	—	—

Source: Table A-5 and A-6 are adapted from ASHRAE, *Handbook of Fundamentals* (Atlanta, GA: American Society of Heating, Refrigerating, and Air-Conditioning Engineers, 1993), Chap. 22, Table 4. Used with permission.

TABLE A-7

Properties of common foods

(a) Specific heats and freezing-point properties

Food	Specific heat, <sup>b</sup> kJ/kg·K				Water content, <sup>a</sup> % (mass)	Freezing point <sup>a</sup> °C	Specific heat, <sup>b</sup> kJ/kg·K				Latent Heat of Fusion, <sup>c</sup> kJ/kg			
	Above Freezing	Below Freezing	Above Freezing	Below Freezing			Freezing point <sup>a</sup> °C	Above Freezing	Below Freezing	Latent Heat of Fusion, <sup>c</sup> kJ/kg				
<b>Vegetables</b>														
Artichokes	84	-1.2	3.65	1.90	84	-1.2	3.65	1.90	281	89	-0.9	3.82	1.96	297
Asparagus	93	-0.6	3.96	2.01	93	-0.6	3.96	2.01	311	83	-1.6	3.62	1.89	277
Beans, snap	89	-0.7	3.82	1.96	89	-0.7	3.82	1.96	297	85	-1.0	3.69	1.91	284
Broccoli	90	-0.6	3.86	1.97	90	-0.6	3.86	1.97	301	86	-0.8	3.72	1.92	287
Cabbage	92	-0.9	3.92	2.00	92	-0.9	3.92	2.00	307	85	-2.0	3.69	1.91	284
Carrots	88	-1.4	3.79	1.95	88	-1.4	3.79	1.95	294	18	—	—	1.07	60
Cauliflower	92	-0.8	3.92	2.00	92	-0.8	3.92	2.00	307	90	-0.8	3.86	1.97	301
Celery	94	-0.5	3.99	2.02	94	-0.5	3.99	2.02	314	87	-1.1	3.75	1.94	291
Corn, sweet	74	-0.6	3.32	1.77	74	-0.6	3.32	1.77	247	93	-0.4	3.96	2.01	311
Cucumbers	96	-0.5	4.06	2.05	96	-0.5	4.06	2.05	321					
Eggplant	93	-0.8	3.96	2.01	93	-0.8	3.96	2.01	311	<b>Fish/Seafood</b>				
Horse radish	75	-1.8	3.35	1.78	75	-1.8	3.35	1.78	251	Cod, whole	-2.2	3.45	1.82	261
Leeks	85	-0.7	3.69	1.91	85	-0.7	3.69	1.91	284	Halibut, whole	-2.2	3.35	1.78	251
Lettuce	95	-0.2	4.02	2.04	95	-0.2	4.02	2.04	317	Lobster	-2.2	3.49	1.84	264
Mushrooms	91	-0.9	3.89	1.99	91	-0.9	3.89	1.99	304	Mackerel	-2.2	2.75	1.56	190
Okra	90	-1.8	3.86	1.97	90	-1.8	3.86	1.97	301	Salmon, whole	-2.2	2.98	1.65	214
Onions, green	89	-0.9	3.82	1.96	89	-0.9	3.82	1.96	297	Shrimp	-2.2	3.62	1.89	277
Onions, dry	88	-0.8	3.79	1.95	88	-0.8	3.79	1.95	294	<b>Meats</b>				
Parsley	85	-1.1	3.69	1.91	85	-1.1	3.69	1.91	284	Beef carcass	-1.7	2.48	1.46	164
Peas, green	74	-0.6	3.32	1.77	74	-0.6	3.32	1.77	247	Liver	-1.7	3.18	1.72	234
Peppers, sweet	92	-0.7	3.92	2.00	92	-0.7	3.92	2.00	307	Round, beef	—	3.08	1.68	224
Potatoes	78	-0.6	3.45	1.82	78	-0.6	3.45	1.82	261	Sirloin, beef	—	2.72	1.55	187
Pumpkins	91	-0.8	3.89	1.99	91	-0.8	3.89	1.99	304	Chicken	-2.8	3.32	1.77	247
Spinach	93	-0.3	3.96	2.01	93	-0.3	3.96	2.01	311	Lamb leg	—	3.02	1.66	217
Tomatoes, ripe	94	-0.5	3.99	2.02	94	-0.5	3.99	2.02	314	Port carcass	—	2.08	1.31	124
Turnips	92	-1.1	3.92	2.00	92	-1.1	3.92	2.00	307	Ham	-1.7	2.72	1.55	187
										Pork sausage	—	2.11	1.32	127
										Turkey	—	2.98	1.65	214
<b>Fruits</b>										<b>Other</b>				
Apples	84	-1.1	3.65	1.90	84	-1.1	3.65	1.90	281	Almonds	—	—	0.89	17
Apricots	85	-1.1	3.69	1.91	85	-1.1	3.69	1.91	284	Butter	—	—	1.04	53
Avocados	65	-0.3	3.02	1.66	65	-0.3	3.02	1.66	217	Cheese,				
Bananas	75	-0.8	3.35	1.78	75	-0.8	3.35	1.78	251	Cheddar	-12.9	2.08	1.31	124
Blueberries	82	-1.6	3.59	1.87	82	-1.6	3.59	1.87	274	Cheese, Swiss	-10.0	2.15	1.33	130
Cantaloupes	92	-1.2	3.92	2.00	92	-1.2	3.92	2.00	307	Chocolate milk	—	—	0.85	3
Cherries, sour	84	-1.7	3.65	1.90	84	-1.7	3.65	1.90	281	Eggs, whole	-0.6	3.32	1.77	247
Cherries, sweet	80	-1.8	3.52	1.85	80	-1.8	3.52	1.85	267	Honey	—	—	1.05	57
Figs, dried	23	—	—	1.13	23	—	—	1.13	77	Ice cream	-5.6	2.95	1.63	210
Figs, fresh	78	-2.4	3.45	1.82	78	-2.4	3.45	1.82	261	Milk, whole	-0.6	3.79	1.95	294
Grapefruit	89	-1.1	3.82	1.96	89	-1.1	3.82	1.96	297	Peanuts	—	—	0.92	20
Grapes	82	-1.1	3.59	1.87	82	-1.1	3.59	1.87	274	Peanuts, roasted	—	—	0.87	7
Lemons	89	-1.4	3.82	1.96	89	-1.4	3.82	1.96	297	Pecans	—	—	0.87	10
Olives	75	-1.4	3.35	1.78	75	-1.4	3.35	1.78	251	Walnuts	—	—	0.88	13
Oranges	87	-0.8	3.75	1.94	87	-0.8	3.75	1.94	291					

Sources: <sup>a</sup>Water content and freezing-point data are from ASHRAE, *Handbook of Fundamentals*, SI version (Atlanta, GA: American Society of Heating, Refrigerating and Air-Conditioning Engineers, Inc., 1993), Chap. 30, Table 1.

<sup>b</sup>Specific heat data are based on the specific heat values of a water and ice at 0°C and are determined from Siebel's formulas:  $c_{p, \text{fresh}} = 3.35 \times (\text{Water content}) + 0.84$ , above freezing, and  $c_{p, \text{frozen}} = 1.26 \times (\text{Water content}) + 0.84$ , below freezing.

<sup>c</sup>The latent heat of fusion is determined by multiplying the heat of fusion of water (334 kJ/kg) by the water content of the food.

TABLE A-7

Properties of common foods  
(b) Other properties

Food	Water Content, % (mass)	Temperature, $T$ °C	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Thermal Diffusivity, $\alpha$ m <sup>2</sup> /s	Specific Heat $c_p$ kJ/kg·K
<b>Fruits/Vegetables</b>						
Apple juice	87	20	1000	0.559	$0.14 \times 10^{-6}$	3.86
Apples	85	8	840	0.418	$0.13 \times 10^{-6}$	3.81
Apples, dried	41.6	23	856	0.219	$0.096 \times 10^{-6}$	2.72
Apricots, dried	43.6	23	1320	0.375	$0.11 \times 10^{-6}$	2.77
Bananas, fresh	76	27	980	0.481	$0.14 \times 10^{-6}$	3.59
Broccoli	—	26	560	0.385	—	—
Cherries, fresh	92	0–30	1050	0.545	$0.13 \times 10^{-6}$	3.99
Figs	40.4	23	1241	0.310	$0.096 \times 10^{-6}$	2.69
Grape juice	89	20	1000	0.567	$0.14 \times 10^{-6}$	3.91
Peaches	89	2–32	960	0.526	$0.14 \times 10^{-6}$	3.91
Plums	—	–16	610	0.247	—	—
Potatoes	78	0–70	1055	0.498	$0.13 \times 10^{-6}$	3.64
Raisins	32	23	1380	0.376	$0.11 \times 10^{-6}$	2.48
<b>Meats</b>						
Beef, ground	67	6	950	0.406	$0.13 \times 10^{-6}$	3.36
Beef, lean	74	3	1090	0.471	$0.13 \times 10^{-6}$	3.54
Beef fat	0	35	810	0.190	—	—
Beef liver	72	35	—	0.448	—	3.49
Cat food	39.7	23	1140	0.326	$0.11 \times 10^{-6}$	2.68
Chicken breast	75	0	1050	0.476	$0.13 \times 10^{-6}$	3.56
Dog food	30.6	23	1240	0.319	$0.11 \times 10^{-6}$	2.45
Fish, cod	81	3	1180	0.534	$0.12 \times 10^{-6}$	3.71
Fish, salmon	67	3	—	0.531	—	3.36
Ham	71.8	20	1030	0.480	$0.14 \times 10^{-6}$	3.48
Lamb	72	20	1030	0.456	$0.13 \times 10^{-6}$	3.49
Pork, lean	72	4	1030	0.456	$0.13 \times 10^{-6}$	3.49
Turkey breast	74	3	1050	0.496	$0.13 \times 10^{-6}$	3.54
Veal	75	20	1060	0.470	$0.13 \times 10^{-6}$	3.56
<b>Other</b>						
Butter	16	4	—	0.197	—	2.08
Chocolate cake	31.9	23	340	0.106	$0.12 \times 10^{-6}$	2.48
Margarine	16	5	1000	0.233	$0.11 \times 10^{-6}$	2.08
Milk, skimmed	91	20	—	0.566	—	3.96
Milk, whole	88	28	—	0.580	—	3.89
Olive oil	0	32	910	0.168	—	—
Peanut oil	0	4	920	0.168	—	—
Water	100	0	1000	0.569	$0.14 \times 10^{-6}$	4.217
	100	30	995	0.618	$0.15 \times 10^{-6}$	4.178
White cake	32.3	23	450	0.082	$0.10 \times 10^{-6}$	2.49

Source: Data obtained primarily from ASHRAE, *Handbook of Fundamentals*, SI version (Atlanta, GA: American Society of Heating, Refrigerating and Air-Conditioning Engineers, Inc., 1993), Chap. 30, Tables 7 and 9. Used with permission.

Most specific heats are calculated from  $c_p = 1.68 + 2.51 \times (\text{Water content})$ , which is a good approximation in the temperature range of 3 to 32°C. Most thermal diffusivities are calculated from  $\alpha = k/\rho c_p$ . Property values given here are valid for the specific water content.

TABLE A-8

Properties of miscellaneous materials

(Values are at 300 K unless indicated otherwise)

Material	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Specific Heat, $c_p$ J/kg·K	Material	Density, $\rho$ kg/m <sup>3</sup>	Thermal Conductivity, $k$ W/m·K	Specific Heat, $c_p$ J/kg·K
Asphalt	2115	0.062	920	Ice			
Bakelite	1300	1.4	1465	273 K	920	1.88	2040
Brick, refractory				253 K	922	2.03	1945
Chrome brick				173 K	928	3.49	1460
473 K	3010	2.3	835	Leather, sole	998	0.159	—
823 K	—	2.5	—	Linoleum	535	0.081	—
1173 K	—	2.0	—		1180	0.186	—
Fire clay, burnt 1600 K				Mica	2900	0.523	—
773 K	2050	1.0	960	Paper	930	0.180	1340
1073 K	—	1.1	—	Plastics			
1373 K	—	1.1	—	Plexiglass	1190	0.19	1465
Fire clay, burnt 1725 K				Teflon			
773 K	2325	1.3	960	300 K	2200	0.35	1050
1073 K	—	1.4	—	400 K	—	0.45	—
1373 K	—	1.4	—	Lexan	1200	0.19	1260
Fire clay brick				Nylon	1145	0.29	—
478 K	2645	1.0	960	Polypropylene	910	0.12	1925
922 K	—	1.5	—	Polyester	1395	0.15	1170
1478 K	—	1.8	—	PVC, vinyl	1470	0.1	840
Magnesite				Porcelain	2300	1.5	—
478 K	—	3.8	1130	Rubber, natural	1150	0.28	—
922 K	—	2.8	—	Rubber, vulcanized			
1478 K	—	1.9	—	Soft	1100	0.13	2010
Chicken meat,				Hard	1190	0.16	—
white (74.4%				Sand	1515	0.2–1.0	800
water content)				Snow, fresh	100	0.60	—
198 K	—	1.60	—	Snow, 273 K	500	2.2	—
233 K	—	1.49	—	Soil, dry	1500	1.0	1900
253 K	—	1.35	—	Soil, wet	1900	2.0	2200
273 K	—	0.48	—	Sugar	1600	0.58	—
293 K	—	0.49	—	Tissue, human			
Clay, dry	1550	0.930	—	Skin	—	0.37	—
Clay, wet	1495	1.675	—	Fat layer	—	0.2	—
Coal, anthracite	1350	0.26	1260	Muscle	—	0.41	—
Concrete (stone				Vaseline	—	0.17	—
mix)	2300	1.4	880	Wood, cross-grain			
Cork	86	0.048	2030	Balsa	140	0.055	—
Cotton	80	0.06	1300	Fir	415	0.11	2720
Fat	—	0.17	—	Oak	545	0.17	2385
Glass				White pine	435	0.11	—
Window	2800	0.7	750	Yellow pine	640	0.15	2805
Pyrex	2225	1–1.4	835	Wood, radial			
Crown	2500	1.05	—	Oak	545	0.19	2385
Lead	3400	0.85	—	Fir	420	0.14	2720
				Wool, ship	145	0.05	—

Source: Compiled from various sources.

TABLE A-9

## Properties of saturated water

Temp. $T, ^\circ\text{C}$	Saturation Pressure $P_{\text{sat}}, \text{kPa}$	Density $\rho, \text{kg/m}^3$		Enthalpy of Vaporization $h_{fg}, \text{kJ/kg}$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$		Thermal Conductivity $k, \text{W/m}\cdot\text{K}$		Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$		Prandtl Number Pr		Volume Expansion Coefficient $\beta, 1/\text{K}$ Liquid
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	
0.01	0.6113	999.8	0.0048	2501	4217	1854	0.561	0.0171	$1.792 \times 10^{-3}$	$0.922 \times 10^{-5}$	13.5	1.00	$-0.068 \times 10^{-3}$
5	0.8721	999.9	0.0068	2490	4205	1857	0.571	0.0173	$1.519 \times 10^{-3}$	$0.934 \times 10^{-5}$	11.2	1.00	$0.015 \times 10^{-3}$
10	1.2276	999.7	0.0094	2478	4194	1862	0.580	0.0176	$1.307 \times 10^{-3}$	$0.946 \times 10^{-5}$	9.45	1.00	$0.733 \times 10^{-3}$
15	1.7051	999.1	0.0128	2466	4185	1863	0.589	0.0179	$1.138 \times 10^{-3}$	$0.959 \times 10^{-5}$	8.09	1.00	$0.138 \times 10^{-3}$
20	2.339	998.0	0.0173	2454	4182	1867	0.598	0.0182	$1.002 \times 10^{-3}$	$0.973 \times 10^{-5}$	7.01	1.00	$0.195 \times 10^{-3}$
25	3.169	997.0	0.0231	2442	4180	1870	0.607	0.0186	$0.891 \times 10^{-3}$	$0.987 \times 10^{-5}$	6.14	1.00	$0.247 \times 10^{-3}$
30	4.246	996.0	0.0304	2431	4178	1875	0.615	0.0189	$0.798 \times 10^{-3}$	$1.001 \times 10^{-5}$	5.42	1.00	$0.294 \times 10^{-3}$
35	5.628	994.0	0.0397	2419	4178	1880	0.623	0.0192	$0.720 \times 10^{-3}$	$1.016 \times 10^{-5}$	4.83	1.00	$0.337 \times 10^{-3}$
40	7.384	992.1	0.0512	2407	4179	1885	0.631	0.0196	$0.653 \times 10^{-3}$	$1.031 \times 10^{-5}$	4.32	1.00	$0.377 \times 10^{-3}$
45	9.593	990.1	0.0655	2395	4180	1892	0.637	0.0200	$0.596 \times 10^{-3}$	$1.046 \times 10^{-5}$	3.91	1.00	$0.415 \times 10^{-3}$
50	12.35	988.1	0.0831	2383	4181	1900	0.644	0.0204	$0.547 \times 10^{-3}$	$1.062 \times 10^{-5}$	3.55	1.00	$0.451 \times 10^{-3}$
55	15.76	985.2	0.1045	2371	4183	1908	0.649	0.0208	$0.504 \times 10^{-3}$	$1.077 \times 10^{-5}$	3.25	1.00	$0.484 \times 10^{-3}$
60	19.94	983.3	0.1304	2359	4185	1916	0.654	0.0212	$0.467 \times 10^{-3}$	$1.093 \times 10^{-5}$	2.99	1.00	$0.517 \times 10^{-3}$
65	25.03	980.4	0.1614	2346	4187	1926	0.659	0.0216	$0.433 \times 10^{-3}$	$1.110 \times 10^{-5}$	2.75	1.00	$0.548 \times 10^{-3}$
70	31.19	977.5	0.1983	2334	4190	1936	0.663	0.0221	$0.404 \times 10^{-3}$	$1.126 \times 10^{-5}$	2.55	1.00	$0.578 \times 10^{-3}$
75	38.58	974.7	0.2421	2321	4193	1948	0.667	0.0225	$0.378 \times 10^{-3}$	$1.142 \times 10^{-5}$	2.38	1.00	$0.607 \times 10^{-3}$
80	47.39	971.8	0.2935	2309	4197	1962	0.670	0.0230	$0.355 \times 10^{-3}$	$1.159 \times 10^{-5}$	2.22	1.00	$0.653 \times 10^{-3}$
85	57.83	968.1	0.3536	2296	4201	1977	0.673	0.0235	$0.333 \times 10^{-3}$	$1.176 \times 10^{-5}$	2.08	1.00	$0.670 \times 10^{-3}$
90	70.14	965.3	0.4235	2283	4206	1993	0.675	0.0240	$0.315 \times 10^{-3}$	$1.193 \times 10^{-5}$	1.96	1.00	$0.702 \times 10^{-3}$
95	84.55	961.5	0.5045	2270	4212	2010	0.677	0.0246	$0.297 \times 10^{-3}$	$1.210 \times 10^{-5}$	1.85	1.00	$0.716 \times 10^{-3}$
100	101.33	957.9	0.5978	2257	4217	2029	0.679	0.0251	$0.282 \times 10^{-3}$	$1.227 \times 10^{-5}$	1.75	1.00	$0.750 \times 10^{-3}$
110	143.27	950.6	0.8263	2230	4229	2071	0.682	0.0262	$0.255 \times 10^{-3}$	$1.261 \times 10^{-5}$	1.58	1.00	$0.798 \times 10^{-3}$
120	198.53	943.4	1.121	2203	4244	2120	0.683	0.0275	$0.232 \times 10^{-3}$	$1.296 \times 10^{-5}$	1.44	1.00	$0.858 \times 10^{-3}$
130	270.1	934.6	1.496	2174	4263	2177	0.684	0.0288	$0.213 \times 10^{-3}$	$1.330 \times 10^{-5}$	1.33	1.01	$0.913 \times 10^{-3}$
140	361.3	921.7	1.965	2145	4286	2244	0.683	0.0301	$0.197 \times 10^{-3}$	$1.365 \times 10^{-5}$	1.24	1.02	$0.970 \times 10^{-3}$
150	475.8	916.6	2.546	2114	4311	2314	0.682	0.0316	$0.183 \times 10^{-3}$	$1.399 \times 10^{-5}$	1.16	1.02	$1.025 \times 10^{-3}$
160	617.8	907.4	3.256	2083	4340	2420	0.680	0.0331	$0.170 \times 10^{-3}$	$1.434 \times 10^{-5}$	1.09	1.05	$1.145 \times 10^{-3}$
170	791.7	897.7	4.119	2050	4370	2490	0.677	0.0347	$0.160 \times 10^{-3}$	$1.468 \times 10^{-5}$	1.03	1.05	$1.178 \times 10^{-3}$
180	1,002.1	887.3	5.153	2015	4410	2590	0.673	0.0364	$0.150 \times 10^{-3}$	$1.502 \times 10^{-5}$	0.983	1.07	$1.210 \times 10^{-3}$
190	1,254.4	876.4	6.388	1979	4460	2710	0.669	0.0382	$0.142 \times 10^{-3}$	$1.537 \times 10^{-5}$	0.947	1.09	$1.280 \times 10^{-3}$
200	1,553.8	864.3	7.852	1941	4500	2840	0.663	0.0401	$0.134 \times 10^{-3}$	$1.571 \times 10^{-5}$	0.910	1.11	$1.350 \times 10^{-3}$
220	2,318	840.3	11.60	1859	4610	3110	0.650	0.0442	$0.122 \times 10^{-3}$	$1.641 \times 10^{-5}$	0.865	1.15	$1.520 \times 10^{-3}$
240	3,344	813.7	16.73	1767	4760	3520	0.632	0.0487	$0.111 \times 10^{-3}$	$1.712 \times 10^{-5}$	0.836	1.24	$1.720 \times 10^{-3}$
260	4,688	783.7	23.69	1663	4970	4070	0.609	0.0540	$0.102 \times 10^{-3}$	$1.788 \times 10^{-5}$	0.832	1.35	$2.000 \times 10^{-3}$
280	6,412	750.8	33.15	1544	5280	4835	0.581	0.0605	$0.094 \times 10^{-3}$	$1.870 \times 10^{-5}$	0.854	1.49	$2.380 \times 10^{-3}$
300	8,581	713.8	46.15	1405	5750	5980	0.548	0.0695	$0.086 \times 10^{-3}$	$1.965 \times 10^{-5}$	0.902	1.69	$2.950 \times 10^{-3}$
320	11,274	667.1	64.57	1239	6540	7900	0.509	0.0836	$0.078 \times 10^{-3}$	$2.084 \times 10^{-5}$	1.00	1.97	
340	14,586	610.5	92.62	1028	8240	11,870	0.469	0.110	$0.070 \times 10^{-3}$	$2.255 \times 10^{-5}$	1.23	2.43	
360	18,651	528.3	144.0	720	14,690	25,800	0.427	0.178	$0.060 \times 10^{-3}$	$2.571 \times 10^{-5}$	2.06	3.73	
374.14	22,090	317.0	317.0	0	—	—	—	—	$0.043 \times 10^{-3}$	$4.313 \times 10^{-5}$			

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/\text{Pr}$ . The temperatures 0.01°C, 100°C, and 374.14°C are the triple-, boiling-, and critical-point temperatures of water, respectively. The properties listed above (except the vapor density) can be used at any pressure with negligible error except at temperatures near the critical-point value.

Note 2: The unit  $\text{kJ/kg}\cdot^\circ\text{C}$  for specific heat is equivalent to  $\text{kJ/kg}\cdot\text{K}$ , and the unit  $\text{W/m}\cdot^\circ\text{C}$  for thermal conductivity is equivalent to  $\text{W/m}\cdot\text{K}$ .

Source: Viscosity and thermal conductivity data are from J. V. Sengers and J. T. R. Watson, *Journal of Physical and Chemical Reference Data* 15 (1986), pp. 1291–1322. Other data are obtained from various sources or calculated.

TABLE A-10

Properties of saturated refrigerant-134a

Temp. $T, ^\circ\text{C}$	Saturation Pressure $P, \text{kPa}$	Density $\rho, \text{kg/m}^3$		Enthalpy of Vaporization $h_{fg}, \text{kJ/kg}$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$		Thermal Conductivity $k, \text{W/m}\cdot\text{K}$		Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$		Prandtl Number Pr		Volume Expansion Coefficient $\beta, 1/\text{K}$	Surface Tension, N/m
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-40	51.2	1418	2.773	225.9	1254	748.6	0.1101	0.00811	$4.878 \times 10^{-4}$	$2.550 \times 10^{-6}$	5.558	0.235	0.00205	0.01760
-35	66.2	1403	3.524	222.7	1264	764.1	0.1084	0.00862	$4.509 \times 10^{-4}$	$3.003 \times 10^{-6}$	5.257	0.266	0.00209	0.01682
-30	84.4	1389	4.429	219.5	1273	780.2	0.1066	0.00913	$4.178 \times 10^{-4}$	$3.504 \times 10^{-6}$	4.992	0.299	0.00215	0.01604
-25	106.5	1374	5.509	216.3	1283	797.2	0.1047	0.00963	$3.882 \times 10^{-4}$	$4.054 \times 10^{-6}$	4.757	0.335	0.00220	0.01527
-20	132.8	1359	6.787	213.0	1294	814.9	0.1028	0.01013	$3.614 \times 10^{-4}$	$4.651 \times 10^{-6}$	4.548	0.374	0.00227	0.01451
-15	164.0	1343	8.288	209.5	1306	833.5	0.1009	0.01063	$3.371 \times 10^{-4}$	$5.295 \times 10^{-6}$	4.363	0.415	0.00233	0.01376
-10	200.7	1327	10.04	206.0	1318	853.1	0.0989	0.01112	$3.150 \times 10^{-4}$	$5.982 \times 10^{-6}$	4.198	0.459	0.00241	0.01302
-5	243.5	1311	12.07	202.4	1330	873.8	0.0968	0.01161	$2.947 \times 10^{-4}$	$6.709 \times 10^{-6}$	4.051	0.505	0.00249	0.01229
0	293.0	1295	14.42	198.7	1344	895.6	0.0947	0.01210	$2.761 \times 10^{-4}$	$7.471 \times 10^{-6}$	3.919	0.553	0.00258	0.01156
5	349.9	1278	17.12	194.8	1358	918.7	0.0925	0.01259	$2.589 \times 10^{-4}$	$8.264 \times 10^{-6}$	3.802	0.603	0.00269	0.01084
10	414.9	1261	20.22	190.8	1374	943.2	0.0903	0.01308	$2.430 \times 10^{-4}$	$9.081 \times 10^{-6}$	3.697	0.655	0.00280	0.01014
15	488.7	1244	23.75	186.6	1390	969.4	0.0880	0.01357	$2.281 \times 10^{-4}$	$9.915 \times 10^{-6}$	3.604	0.708	0.00293	0.00944
20	572.1	1226	27.77	182.3	1408	997.6	0.0856	0.01406	$2.142 \times 10^{-4}$	$1.075 \times 10^{-5}$	3.521	0.763	0.00307	0.00876
25	665.8	1207	32.34	177.8	1427	1028	0.0833	0.01456	$2.012 \times 10^{-4}$	$1.160 \times 10^{-5}$	3.448	0.819	0.00324	0.00808
30	770.6	1188	37.53	173.1	1448	1061	0.0808	0.01507	$1.888 \times 10^{-4}$	$1.244 \times 10^{-5}$	3.383	0.877	0.00342	0.00742
35	887.5	1168	43.41	168.2	1471	1098	0.0783	0.01558	$1.772 \times 10^{-4}$	$1.327 \times 10^{-5}$	3.328	0.935	0.00364	0.00677
40	1017.1	1147	50.08	163.0	1498	1138	0.0757	0.01610	$1.660 \times 10^{-4}$	$1.408 \times 10^{-5}$	3.285	0.995	0.00390	0.00613
45	1160.5	1125	57.66	157.6	1529	1184	0.0731	0.01664	$1.554 \times 10^{-4}$	$1.486 \times 10^{-5}$	3.253	1.058	0.00420	0.00550
50	1318.6	1102	66.27	151.8	1566	1237	0.0704	0.01720	$1.453 \times 10^{-4}$	$1.562 \times 10^{-5}$	3.231	1.123	0.00455	0.00489
55	1492.3	1078	76.11	145.7	1608	1298	0.0676	0.01777	$1.355 \times 10^{-4}$	$1.634 \times 10^{-5}$	3.223	1.193	0.00500	0.00429
60	1682.8	1053	87.38	139.1	1659	1372	0.0647	0.01838	$1.260 \times 10^{-4}$	$1.704 \times 10^{-5}$	3.229	1.272	0.00554	0.00372
65	1891.0	1026	100.4	132.1	1722	1462	0.0618	0.01902	$1.167 \times 10^{-4}$	$1.771 \times 10^{-5}$	3.255	1.362	0.00624	0.00315
70	2118.2	996.2	115.6	124.4	1801	1577	0.0587	0.01972	$1.077 \times 10^{-4}$	$1.839 \times 10^{-5}$	3.307	1.471	0.00716	0.00261
75	2365.8	964	133.6	115.9	1907	1731	0.0555	0.02048	$9.891 \times 10^{-5}$	$1.908 \times 10^{-5}$	3.400	1.612	0.00843	0.00209
80	2635.2	928.2	155.3	106.4	2056	1948	0.0521	0.02133	$9.011 \times 10^{-5}$	$1.982 \times 10^{-5}$	3.558	1.810	0.01031	0.00160
85	2928.2	887.1	182.3	95.4	2287	2281	0.0484	0.02233	$8.124 \times 10^{-5}$	$2.071 \times 10^{-5}$	3.837	2.116	0.01336	0.00114
90	3246.9	837.7	217.8	82.2	2701	2865	0.0444	0.02357	$7.203 \times 10^{-5}$	$2.187 \times 10^{-5}$	4.385	2.658	0.01911	0.00071
95	3594.1	772.5	269.3	64.9	3675	4144	0.0396	0.02544	$6.190 \times 10^{-5}$	$2.370 \times 10^{-5}$	5.746	3.862	0.03343	0.00033
100	3975.1	651.7	376.3	33.9	7959	8785	0.0322	0.02989	$4.765 \times 10^{-5}$	$2.833 \times 10^{-5}$	11.77	8.326	0.10047	0.00004

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/\text{Pr}$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit  $\text{kJ/kg}\cdot^\circ\text{C}$  for specific heat is equivalent to  $\text{kJ/kg}\cdot\text{K}$ , and the unit  $\text{W/m}\cdot^\circ\text{C}$  for thermal conductivity is equivalent to  $\text{W/m}\cdot\text{K}$ .

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: R. Tillner-Roth and H. D. Baehr, "An International Standard Formulation for the Thermodynamic Properties of 1,1,1,2-Tetrafluoroethane (HFC-134a) for Temperatures from 170 K to 455 K and Pressures up to 70 MPa," *J. Phys. Chem., Ref. Data*, Vol. 23, No. 5, 1994; M.J. Assael, N. K. Dalaouti, A. A. Griva, and J. H. Dymond, "Viscosity and Thermal Conductivity of Halogenated Methane and Ethane Refrigerants," *IJR*, Vol. 22, pp. 525-535, 1999; NIST REFPROP 6 program (M. O. McLinden, S. A. Klein, E. W. Lemmon, and A. P. Peskin, Physical and Chemical Properties Division, National Institute of Standards and Technology, Boulder, CO 80303, 1995).

TABLE A-11

Properties of saturated ammonia

Temp. <i>T</i> , °C	Saturation Pressure <i>P</i> , kPa	Density $\rho$ , kg/m <sup>3</sup>		Enthalpy of Vaporization $h_{fg}$ , kJ/kg	Specific Heat $c_p$ , J/kg·K		Thermal Conductivity <i>k</i> , W/m·K		Dynamic Viscosity $\mu$ , kg/m·s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/K	Surface Tension, N/m
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-40	71.66	690.2	0.6435	1389	4414	2242	—	0.01792	$2.926 \times 10^{-4}$	$7.957 \times 10^{-6}$	—	0.9955	0.00176	0.03565
-30	119.4	677.8	1.037	1360	4465	2322	—	0.01898	$2.630 \times 10^{-4}$	$8.311 \times 10^{-6}$	—	1.017	0.00185	0.03341
-25	151.5	671.5	1.296	1345	4489	2369	0.5968	0.01957	$2.492 \times 10^{-4}$	$8.490 \times 10^{-6}$	1.875	1.028	0.00190	0.03229
-20	190.1	665.1	1.603	1329	4514	2420	0.5853	0.02015	$2.361 \times 10^{-4}$	$8.669 \times 10^{-6}$	1.821	1.041	0.00194	0.03118
-15	236.2	658.6	1.966	1313	4538	2476	0.5737	0.02075	$2.236 \times 10^{-4}$	$8.851 \times 10^{-6}$	1.769	1.056	0.00199	0.03007
-10	290.8	652.1	2.391	1297	4564	2536	0.5621	0.02138	$2.117 \times 10^{-4}$	$9.034 \times 10^{-6}$	1.718	1.072	0.00205	0.02896
-5	354.9	645.4	2.886	1280	4589	2601	0.5505	0.02203	$2.003 \times 10^{-4}$	$9.218 \times 10^{-6}$	1.670	1.089	0.00210	0.02786
0	429.6	638.6	3.458	1262	4617	2672	0.5390	0.02270	$1.896 \times 10^{-4}$	$9.405 \times 10^{-6}$	1.624	1.107	0.00216	0.02676
5	516	631.7	4.116	1244	4645	2749	0.5274	0.02341	$1.794 \times 10^{-4}$	$9.593 \times 10^{-6}$	1.580	1.126	0.00223	0.02566
10	615.3	624.6	4.870	1226	4676	2831	0.5158	0.02415	$1.697 \times 10^{-4}$	$9.784 \times 10^{-6}$	1.539	1.147	0.00230	0.02457
15	728.8	617.5	5.729	1206	4709	2920	0.5042	0.02492	$1.606 \times 10^{-4}$	$9.978 \times 10^{-6}$	1.500	1.169	0.00237	0.02348
20	857.8	610.2	6.705	1186	4745	3016	0.4927	0.02573	$1.519 \times 10^{-4}$	$1.017 \times 10^{-5}$	1.463	1.193	0.00245	0.02240
25	1003	602.8	7.809	1166	4784	3120	0.4811	0.02658	$1.438 \times 10^{-4}$	$1.037 \times 10^{-5}$	1.430	1.218	0.00254	0.02132
30	1167	595.2	9.055	1144	4828	3232	0.4695	0.02748	$1.361 \times 10^{-4}$	$1.057 \times 10^{-5}$	1.399	1.244	0.00264	0.02024
35	1351	587.4	10.46	1122	4877	3354	0.4579	0.02843	$1.288 \times 10^{-4}$	$1.078 \times 10^{-5}$	1.372	1.272	0.00275	0.01917
40	1555	579.4	12.03	1099	4932	3486	0.4464	0.02943	$1.219 \times 10^{-4}$	$1.099 \times 10^{-5}$	1.347	1.303	0.00287	0.01810
45	1782	571.3	13.8	1075	4993	3631	0.4348	0.03049	$1.155 \times 10^{-4}$	$1.121 \times 10^{-5}$	1.327	1.335	0.00301	0.01704
50	2033	562.9	15.78	1051	5063	3790	0.4232	0.03162	$1.094 \times 10^{-4}$	$1.143 \times 10^{-5}$	1.310	1.371	0.00316	0.01598
55	2310	554.2	18.00	1025	5143	3967	0.4116	0.03283	$1.037 \times 10^{-4}$	$1.166 \times 10^{-5}$	1.297	1.409	0.00334	0.01493
60	2614	545.2	20.48	997.4	5234	4163	0.4001	0.03412	$9.846 \times 10^{-5}$	$1.189 \times 10^{-5}$	1.288	1.452	0.00354	0.01389
65	2948	536.0	23.26	968.9	5340	4384	0.3885	0.03550	$9.347 \times 10^{-5}$	$1.213 \times 10^{-5}$	1.285	1.499	0.00377	0.01285
70	3312	526.3	26.39	939.0	5463	4634	0.3769	0.03700	$8.879 \times 10^{-5}$	$1.238 \times 10^{-5}$	1.287	1.551	0.00404	0.01181
75	3709	516.2	29.90	907.5	5608	4923	0.3653	0.03862	$8.440 \times 10^{-5}$	$1.264 \times 10^{-5}$	1.296	1.612	0.00436	0.01079
80	4141	505.7	33.87	874.1	5780	5260	0.3538	0.04038	$8.030 \times 10^{-5}$	$1.292 \times 10^{-5}$	1.312	1.683	0.00474	0.00977
85	4609	494.5	38.36	838.6	5988	5659	0.3422	0.04232	$7.646 \times 10^{-5}$	$1.322 \times 10^{-5}$	1.338	1.768	0.00521	0.00876
90	5116	482.8	43.48	800.6	6242	6142	0.3306	0.04447	$7.284 \times 10^{-5}$	$1.354 \times 10^{-5}$	1.375	1.871	0.00579	0.00776
95	5665	470.2	49.35	759.8	6561	6740	0.3190	0.04687	$6.946 \times 10^{-5}$	$1.389 \times 10^{-5}$	1.429	1.999	0.00652	0.00677
100	6257	456.6	56.15	715.5	6972	7503	0.3075	0.04958	$6.628 \times 10^{-5}$	$1.429 \times 10^{-5}$	1.503	2.163	0.00749	0.00579

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/\text{Pr}$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit kJ/kg·°C for specific heat is equivalent to kJ/kg·K, and the unit W/m·°C for thermal conductivity is equivalent to W/m·K.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Tillner-Roth, Harms-Watzenberg, and Baehr, "Eine neue Fundamentalgleichung für Ammoniak," DKV-Tagungsbericht 20:167–181, 1993; Liley and Desai, "Thermophysical Properties of Refrigerants," ASHRAE, 1993, ISBN 1-1883413-10-9.



TABLE A-12

## Properties of saturated propane

Temp. <i>T</i> , °C	Saturation Pressure <i>P</i> , kPa	Density $\rho$ , kg/m <sup>3</sup>		Enthalpy of Vaporization $h_{fg}$ , kJ/kg	Specific Heat $c_p$ , J/kg·K		Thermal Conductivity <i>k</i> , W/m·K		Dynamic Viscosity $\mu$ , kg/m·s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/K Liquid	Surface Tension, N/m
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-120	0.4053	664.7	0.01408	498.3	2003	1115	0.1802	0.00589	$6.136 \times 10^{-4}$	$4.372 \times 10^{-6}$	6.820	0.827	0.00153	0.02630
-110	1.157	654.5	0.03776	489.3	2021	1148	0.1738	0.00645	$5.054 \times 10^{-4}$	$4.625 \times 10^{-6}$	5.878	0.822	0.00157	0.02486
-100	2.881	644.2	0.08872	480.4	2044	1183	0.1672	0.00705	$4.252 \times 10^{-4}$	$4.881 \times 10^{-6}$	5.195	0.819	0.00161	0.02344
-90	6.406	633.8	0.1870	471.5	2070	1221	0.1606	0.00769	$3.635 \times 10^{-4}$	$5.143 \times 10^{-6}$	4.686	0.817	0.00166	0.02202
-80	12.97	623.2	0.3602	462.4	2100	1263	0.1539	0.00836	$3.149 \times 10^{-4}$	$5.409 \times 10^{-6}$	4.297	0.817	0.00171	0.02062
-70	24.26	612.5	0.6439	453.1	2134	1308	0.1472	0.00908	$2.755 \times 10^{-4}$	$5.680 \times 10^{-6}$	3.994	0.818	0.00177	0.01923
-60	42.46	601.5	1.081	443.5	2173	1358	0.1407	0.00985	$2.430 \times 10^{-4}$	$5.956 \times 10^{-6}$	3.755	0.821	0.00184	0.01785
-50	70.24	590.3	1.724	433.6	2217	1412	0.1343	0.01067	$2.158 \times 10^{-4}$	$6.239 \times 10^{-6}$	3.563	0.825	0.00192	0.01649
-40	110.7	578.8	2.629	423.1	2258	1471	0.1281	0.01155	$1.926 \times 10^{-4}$	$6.529 \times 10^{-6}$	3.395	0.831	0.00201	0.01515
-30	167.3	567.0	3.864	412.1	2310	1535	0.1221	0.01250	$1.726 \times 10^{-4}$	$6.827 \times 10^{-6}$	3.266	0.839	0.00213	0.01382
-20	243.8	554.7	5.503	400.3	2368	1605	0.1163	0.01351	$1.551 \times 10^{-4}$	$7.136 \times 10^{-6}$	3.158	0.848	0.00226	0.01251
-10	344.4	542.0	7.635	387.8	2433	1682	0.1107	0.01459	$1.397 \times 10^{-4}$	$7.457 \times 10^{-6}$	3.069	0.860	0.00242	0.01122
0	473.3	528.7	10.36	374.2	2507	1768	0.1054	0.01576	$1.259 \times 10^{-4}$	$7.794 \times 10^{-6}$	2.996	0.875	0.00262	0.00996
5	549.8	521.8	11.99	367.0	2547	1814	0.1028	0.01637	$1.195 \times 10^{-4}$	$7.970 \times 10^{-6}$	2.964	0.883	0.00273	0.00934
10	635.1	514.7	13.81	359.5	2590	1864	0.1002	0.01701	$1.135 \times 10^{-4}$	$8.151 \times 10^{-6}$	2.935	0.893	0.00286	0.00872
15	729.8	507.5	15.85	351.7	2637	1917	0.0977	0.01767	$1.077 \times 10^{-4}$	$8.339 \times 10^{-6}$	2.909	0.905	0.00301	0.00811
20	834.4	500.0	18.13	343.4	2688	1974	0.0952	0.01836	$1.022 \times 10^{-4}$	$8.534 \times 10^{-6}$	2.886	0.918	0.00318	0.00751
25	949.7	492.2	20.68	334.8	2742	2036	0.0928	0.01908	$9.702 \times 10^{-5}$	$8.738 \times 10^{-6}$	2.866	0.933	0.00337	0.00691
30	1076	484.2	23.53	325.8	2802	2104	0.0904	0.01982	$9.197 \times 10^{-5}$	$8.952 \times 10^{-6}$	2.850	0.950	0.00358	0.00633
35	1215	475.8	26.72	316.2	2869	2179	0.0881	0.02061	$8.710 \times 10^{-5}$	$9.178 \times 10^{-6}$	2.837	0.971	0.00384	0.00575
40	1366	467.1	30.29	306.1	2943	2264	0.0857	0.02142	$8.240 \times 10^{-5}$	$9.417 \times 10^{-6}$	2.828	0.995	0.00413	0.00518
45	1530	458.0	34.29	295.3	3026	2361	0.0834	0.02228	$7.785 \times 10^{-5}$	$9.674 \times 10^{-6}$	2.824	1.025	0.00448	0.00463
50	1708	448.5	38.79	283.9	3122	2473	0.0811	0.02319	$7.343 \times 10^{-5}$	$9.950 \times 10^{-6}$	2.826	1.061	0.00491	0.00408
60	2110	427.5	49.66	258.4	3283	2769	0.0765	0.02517	$6.487 \times 10^{-5}$	$1.058 \times 10^{-5}$	2.784	1.164	0.00609	0.00303
70	2580	403.2	64.02	228.0	3595	3241	0.0717	0.02746	$5.649 \times 10^{-5}$	$1.138 \times 10^{-5}$	2.834	1.343	0.00811	0.00204
80	3127	373.0	84.28	189.7	4501	4173	0.0663	0.03029	$4.790 \times 10^{-5}$	$1.249 \times 10^{-5}$	3.251	1.722	0.01248	0.00114
90	3769	329.1	118.6	133.2	6977	7239	0.0595	0.03441	$3.807 \times 10^{-5}$	$1.448 \times 10^{-5}$	4.465	3.047	0.02847	0.00037

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\mu c_p = \nu/Pr$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit kJ/kg·°C for specific heat is equivalent to kJ/kg·K, and the unit W/m·°C for thermal conductivity is equivalent to W/m·K.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Reiner Tillner-Roth, "Fundamental Equations of State," Shaker, Verlag, Aachen, 1998; B. A. Younglove and J. F. Ely, "Thermophysical Properties of Fluids. II Methane, Ethane, Propane, Isobutane, and Normal Butane," *J. Phys. Chem. Ref. Data*, Vol. 16, No. 4, 1987; G.R. Somayajulu, "A Generalized Equation for Surface Tension from the Triple-Point to the Critical-Point," *International Journal of Thermophysics*, Vol. 9, No. 4, 1988.

TABLE A-13

## Properties of liquids

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr	Volume Expansion Coeff. $\beta, 1/\text{K}$
<i>Methane [CH<sub>4</sub>]</i>								
-160	420.2	3492	0.1863	$1.270 \times 10^{-7}$	$1.133 \times 10^{-4}$	$2.699 \times 10^{-7}$	2.126	0.00352
-150	405.0	3580	0.1703	$1.174 \times 10^{-7}$	$9.169 \times 10^{-5}$	$2.264 \times 10^{-7}$	1.927	0.00391
-140	388.8	3700	0.1550	$1.077 \times 10^{-7}$	$7.551 \times 10^{-5}$	$1.942 \times 10^{-7}$	1.803	0.00444
-130	371.1	3875	0.1402	$9.749 \times 10^{-8}$	$6.288 \times 10^{-5}$	$1.694 \times 10^{-7}$	1.738	0.00520
-120	351.4	4146	0.1258	$8.634 \times 10^{-8}$	$5.257 \times 10^{-5}$	$1.496 \times 10^{-7}$	1.732	0.00637
-110	328.8	4611	0.1115	$7.356 \times 10^{-8}$	$4.377 \times 10^{-5}$	$1.331 \times 10^{-7}$	1.810	0.00841
-100	301.0	5578	0.0967	$5.761 \times 10^{-8}$	$3.577 \times 10^{-5}$	$1.188 \times 10^{-7}$	2.063	0.01282
-90	261.7	8902	0.0797	$3.423 \times 10^{-8}$	$2.761 \times 10^{-5}$	$1.055 \times 10^{-7}$	3.082	0.02922
<i>Methanol [CH<sub>3</sub>(OH)]</i>								
20	788.4	2515	0.1987	$1.002 \times 10^{-7}$	$5.857 \times 10^{-4}$	$7.429 \times 10^{-7}$	7.414	0.00118
30	779.1	2577	0.1980	$9.862 \times 10^{-8}$	$5.088 \times 10^{-4}$	$6.531 \times 10^{-7}$	6.622	0.00120
40	769.6	2644	0.1972	$9.690 \times 10^{-8}$	$4.460 \times 10^{-4}$	$5.795 \times 10^{-7}$	5.980	0.00123
50	760.1	2718	0.1965	$9.509 \times 10^{-8}$	$3.942 \times 10^{-4}$	$5.185 \times 10^{-7}$	5.453	0.00127
60	750.4	2798	0.1957	$9.320 \times 10^{-8}$	$3.510 \times 10^{-4}$	$4.677 \times 10^{-7}$	5.018	0.00132
70	740.4	2885	0.1950	$9.128 \times 10^{-8}$	$3.146 \times 10^{-4}$	$4.250 \times 10^{-7}$	4.655	0.00137
<i>Isobutane (R600a)</i>								
-100	683.8	1881	0.1383	$1.075 \times 10^{-7}$	$9.305 \times 10^{-4}$	$1.360 \times 10^{-6}$	12.65	0.00142
-75	659.3	1970	0.1357	$1.044 \times 10^{-7}$	$5.624 \times 10^{-4}$	$8.531 \times 10^{-7}$	8.167	0.00150
-50	634.3	2069	0.1283	$9.773 \times 10^{-8}$	$3.769 \times 10^{-4}$	$5.942 \times 10^{-7}$	6.079	0.00161
-25	608.2	2180	0.1181	$8.906 \times 10^{-8}$	$2.688 \times 10^{-4}$	$4.420 \times 10^{-7}$	4.963	0.00177
0	580.6	2306	0.1068	$7.974 \times 10^{-8}$	$1.993 \times 10^{-4}$	$3.432 \times 10^{-7}$	4.304	0.00199
25	550.7	2455	0.0956	$7.069 \times 10^{-8}$	$1.510 \times 10^{-4}$	$2.743 \times 10^{-7}$	3.880	0.00232
50	517.3	2640	0.0851	$6.233 \times 10^{-8}$	$1.155 \times 10^{-4}$	$2.233 \times 10^{-7}$	3.582	0.00286
75	478.5	2896	0.0757	$5.460 \times 10^{-8}$	$8.785 \times 10^{-5}$	$1.836 \times 10^{-7}$	3.363	0.00385
100	429.6	3361	0.0669	$4.634 \times 10^{-8}$	$6.483 \times 10^{-5}$	$1.509 \times 10^{-7}$	3.256	0.00628
<i>Glycerin</i>								
0	1276	2262	0.2820	$9.773 \times 10^{-8}$	10.49	$8.219 \times 10^{-3}$	84,101	
5	1273	2288	0.2835	$9.732 \times 10^{-8}$	6.730	$5.287 \times 10^{-3}$	54,327	
10	1270	2320	0.2846	$9.662 \times 10^{-8}$	4.241	$3.339 \times 10^{-3}$	34,561	
15	1267	2354	0.2856	$9.576 \times 10^{-8}$	2.496	$1.970 \times 10^{-3}$	20,570	
20	1264	2386	0.2860	$9.484 \times 10^{-8}$	1.519	$1.201 \times 10^{-3}$	12,671	
25	1261	2416	0.2860	$9.388 \times 10^{-8}$	0.9934	$7.878 \times 10^{-4}$	8,392	
30	1258	2447	0.2860	$9.291 \times 10^{-8}$	0.6582	$5.232 \times 10^{-4}$	5,631	
35	1255	2478	0.2860	$9.195 \times 10^{-8}$	0.4347	$3.464 \times 10^{-4}$	3,767	
40	1252	2513	0.2863	$9.101 \times 10^{-8}$	0.3073	$2.455 \times 10^{-4}$	2,697	
<i>Engine Oil (unused)</i>								
0	899.0	1797	0.1469	$9.097 \times 10^{-8}$	3.814	$4.242 \times 10^{-3}$	46,636	0.00070
20	888.1	1881	0.1450	$8.680 \times 10^{-8}$	0.8374	$9.429 \times 10^{-4}$	10,863	0.00070
40	876.0	1964	0.1444	$8.391 \times 10^{-8}$	0.2177	$2.485 \times 10^{-4}$	2,962	0.00070
60	863.9	2048	0.1404	$7.934 \times 10^{-8}$	0.07399	$8.565 \times 10^{-5}$	1,080	0.00070
80	852.0	2132	0.1380	$7.599 \times 10^{-8}$	0.03232	$3.794 \times 10^{-5}$	499.3	0.00070
100	840.0	2220	0.1367	$7.330 \times 10^{-8}$	0.01718	$2.046 \times 10^{-5}$	279.1	0.00070
120	828.9	2308	0.1347	$7.042 \times 10^{-8}$	0.01029	$1.241 \times 10^{-5}$	176.3	0.00070
140	816.8	2395	0.1330	$6.798 \times 10^{-8}$	0.006558	$8.029 \times 10^{-6}$	118.1	0.00070
150	810.3	2441	0.1327	$6.708 \times 10^{-8}$	0.005344	$6.595 \times 10^{-6}$	98.31	0.00070

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-14

## Properties of liquid metals

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr	Volume Expansion Coeff. $\beta, 1/\text{K}$
<i>Mercury (Hg) Melting Point: <math>-39^\circ\text{C}</math></i>								
0	13595	140.4	8.18200	$4.287 \times 10^{-6}$	$1.687 \times 10^{-3}$	$1.241 \times 10^{-7}$	0.0289	$1.810 \times 10^{-4}$
25	13534	139.4	8.51533	$4.514 \times 10^{-6}$	$1.534 \times 10^{-3}$	$1.133 \times 10^{-7}$	0.0251	$1.810 \times 10^{-4}$
50	13473	138.6	8.83632	$4.734 \times 10^{-6}$	$1.423 \times 10^{-3}$	$1.056 \times 10^{-7}$	0.0223	$1.810 \times 10^{-4}$
75	13412	137.8	9.15632	$4.956 \times 10^{-6}$	$1.316 \times 10^{-3}$	$9.819 \times 10^{-8}$	0.0198	$1.810 \times 10^{-4}$
100	13351	137.1	9.46706	$5.170 \times 10^{-6}$	$1.245 \times 10^{-3}$	$9.326 \times 10^{-8}$	0.0180	$1.810 \times 10^{-4}$
150	13231	136.1	10.07780	$5.595 \times 10^{-6}$	$1.126 \times 10^{-3}$	$8.514 \times 10^{-8}$	0.0152	$1.810 \times 10^{-4}$
200	13112	135.5	10.65465	$5.996 \times 10^{-6}$	$1.043 \times 10^{-3}$	$7.959 \times 10^{-8}$	0.0133	$1.815 \times 10^{-4}$
250	12993	135.3	11.18150	$6.363 \times 10^{-6}$	$9.820 \times 10^{-4}$	$7.558 \times 10^{-8}$	0.0119	$1.829 \times 10^{-4}$
300	12873	135.3	11.68150	$6.705 \times 10^{-6}$	$9.336 \times 10^{-4}$	$7.252 \times 10^{-8}$	0.0108	$1.854 \times 10^{-4}$
<i>Bismuth (Bi) Melting Point: <math>271^\circ\text{C}</math></i>								
350	9969	146.0	16.28	$1.118 \times 10^{-5}$	$1.540 \times 10^{-3}$	$1.545 \times 10^{-7}$	0.01381	
400	9908	148.2	16.10	$1.096 \times 10^{-5}$	$1.422 \times 10^{-3}$	$1.436 \times 10^{-7}$	0.01310	
500	9785	152.8	15.74	$1.052 \times 10^{-5}$	$1.188 \times 10^{-3}$	$1.215 \times 10^{-7}$	0.01154	
600	9663	157.3	15.60	$1.026 \times 10^{-5}$	$1.013 \times 10^{-3}$	$1.048 \times 10^{-7}$	0.01022	
700	9540	161.8	15.60	$1.010 \times 10^{-5}$	$8.736 \times 10^{-4}$	$9.157 \times 10^{-8}$	0.00906	
<i>Lead (Pb) Melting Point: <math>327^\circ\text{C}</math></i>								
400	10506	158	15.97	$9.623 \times 10^{-6}$	$2.277 \times 10^{-3}$	$2.167 \times 10^{-7}$	0.02252	
450	10449	156	15.74	$9.649 \times 10^{-6}$	$2.065 \times 10^{-3}$	$1.976 \times 10^{-7}$	0.02048	
500	10390	155	15.54	$9.651 \times 10^{-6}$	$1.884 \times 10^{-3}$	$1.814 \times 10^{-7}$	0.01879	
550	10329	155	15.39	$9.610 \times 10^{-6}$	$1.758 \times 10^{-3}$	$1.702 \times 10^{-7}$	0.01771	
600	10267	155	15.23	$9.568 \times 10^{-6}$	$1.632 \times 10^{-3}$	$1.589 \times 10^{-7}$	0.01661	
650	10206	155	15.07	$9.526 \times 10^{-6}$	$1.505 \times 10^{-3}$	$1.475 \times 10^{-7}$	0.01549	
700	10145	155	14.91	$9.483 \times 10^{-6}$	$1.379 \times 10^{-3}$	$1.360 \times 10^{-7}$	0.01434	
<i>Sodium (Na) Melting Point: <math>98^\circ\text{C}</math></i>								
100	927.3	1378	85.84	$6.718 \times 10^{-5}$	$6.892 \times 10^{-4}$	$7.432 \times 10^{-7}$	0.01106	
200	902.5	1349	80.84	$6.639 \times 10^{-5}$	$5.385 \times 10^{-4}$	$5.967 \times 10^{-7}$	0.008987	
300	877.8	1320	75.84	$6.544 \times 10^{-5}$	$3.878 \times 10^{-4}$	$4.418 \times 10^{-7}$	0.006751	
400	853.0	1296	71.20	$6.437 \times 10^{-5}$	$2.720 \times 10^{-4}$	$3.188 \times 10^{-7}$	0.004953	
500	828.5	1284	67.41	$6.335 \times 10^{-5}$	$2.411 \times 10^{-4}$	$2.909 \times 10^{-7}$	0.004593	
600	804.0	1272	63.63	$6.220 \times 10^{-5}$	$2.101 \times 10^{-4}$	$2.614 \times 10^{-7}$	0.004202	
<i>Potassium (K) Melting Point: <math>64^\circ\text{C}</math></i>								
200	795.2	790.8	43.99	$6.995 \times 10^{-5}$	$3.350 \times 10^{-4}$	$4.213 \times 10^{-7}$	0.006023	
300	771.6	772.8	42.01	$7.045 \times 10^{-5}$	$2.667 \times 10^{-4}$	$3.456 \times 10^{-7}$	0.004906	
400	748.0	754.8	40.03	$7.090 \times 10^{-5}$	$1.984 \times 10^{-4}$	$2.652 \times 10^{-7}$	0.00374	
500	723.9	750.0	37.81	$6.964 \times 10^{-5}$	$1.668 \times 10^{-4}$	$2.304 \times 10^{-7}$	0.003309	
600	699.6	750.0	35.50	$6.765 \times 10^{-5}$	$1.487 \times 10^{-4}$	$2.126 \times 10^{-7}$	0.003143	
<i>Sodium-Potassium (%22Na-%78K) Melting Point: <math>-11^\circ\text{C}</math></i>								
100	847.3	944.4	25.64	$3.205 \times 10^{-5}$	$5.707 \times 10^{-4}$	$6.736 \times 10^{-7}$	0.02102	
200	823.2	922.5	26.27	$3.459 \times 10^{-5}$	$4.587 \times 10^{-4}$	$5.572 \times 10^{-7}$	0.01611	
300	799.1	900.6	26.89	$3.736 \times 10^{-5}$	$3.467 \times 10^{-4}$	$4.339 \times 10^{-7}$	0.01161	
400	775.0	879.0	27.50	$4.037 \times 10^{-5}$	$2.357 \times 10^{-4}$	$3.041 \times 10^{-7}$	0.00753	
500	751.5	880.1	27.89	$4.217 \times 10^{-5}$	$2.108 \times 10^{-4}$	$2.805 \times 10^{-7}$	0.00665	
600	728.0	881.2	28.28	$4.408 \times 10^{-5}$	$1.859 \times 10^{-4}$	$2.553 \times 10^{-7}$	0.00579	

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-15

Properties of air at 1 atm pressure

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr
-150	2.866	983	0.01171	$4.158 \times 10^{-6}$	$8.636 \times 10^{-6}$	$3.013 \times 10^{-6}$	0.7246
-100	2.038	966	0.01582	$8.036 \times 10^{-6}$	$1.189 \times 10^{-5}$	$5.837 \times 10^{-6}$	0.7263
-50	1.582	999	0.01979	$1.252 \times 10^{-5}$	$1.474 \times 10^{-5}$	$9.319 \times 10^{-6}$	0.7440
-40	1.514	1002	0.02057	$1.356 \times 10^{-5}$	$1.527 \times 10^{-5}$	$1.008 \times 10^{-5}$	0.7436
-30	1.451	1004	0.02134	$1.465 \times 10^{-5}$	$1.579 \times 10^{-5}$	$1.087 \times 10^{-5}$	0.7425
-20	1.394	1005	0.02211	$1.578 \times 10^{-5}$	$1.630 \times 10^{-5}$	$1.169 \times 10^{-5}$	0.7408
-10	1.341	1006	0.02288	$1.696 \times 10^{-5}$	$1.680 \times 10^{-5}$	$1.252 \times 10^{-5}$	0.7387
0	1.292	1006	0.02364	$1.818 \times 10^{-5}$	$1.729 \times 10^{-5}$	$1.338 \times 10^{-5}$	0.7362
5	1.269	1006	0.02401	$1.880 \times 10^{-5}$	$1.754 \times 10^{-5}$	$1.382 \times 10^{-5}$	0.7350
10	1.246	1006	0.02439	$1.944 \times 10^{-5}$	$1.778 \times 10^{-5}$	$1.426 \times 10^{-5}$	0.7336
15	1.225	1007	0.02476	$2.009 \times 10^{-5}$	$1.802 \times 10^{-5}$	$1.470 \times 10^{-5}$	0.7323
20	1.204	1007	0.02514	$2.074 \times 10^{-5}$	$1.825 \times 10^{-5}$	$1.516 \times 10^{-5}$	0.7309
25	1.184	1007	0.02551	$2.141 \times 10^{-5}$	$1.849 \times 10^{-5}$	$1.562 \times 10^{-5}$	0.7296
30	1.164	1007	0.02588	$2.208 \times 10^{-5}$	$1.872 \times 10^{-5}$	$1.608 \times 10^{-5}$	0.7282
35	1.145	1007	0.02625	$2.277 \times 10^{-5}$	$1.895 \times 10^{-5}$	$1.655 \times 10^{-5}$	0.7268
40	1.127	1007	0.02662	$2.346 \times 10^{-5}$	$1.918 \times 10^{-5}$	$1.702 \times 10^{-5}$	0.7255
45	1.109	1007	0.02699	$2.416 \times 10^{-5}$	$1.941 \times 10^{-5}$	$1.750 \times 10^{-5}$	0.7241
50	1.092	1007	0.02735	$2.487 \times 10^{-5}$	$1.963 \times 10^{-5}$	$1.798 \times 10^{-5}$	0.7228
60	1.059	1007	0.02808	$2.632 \times 10^{-5}$	$2.008 \times 10^{-5}$	$1.896 \times 10^{-5}$	0.7202
70	1.028	1007	0.02881	$2.780 \times 10^{-5}$	$2.052 \times 10^{-5}$	$1.995 \times 10^{-5}$	0.7177
80	0.9994	1008	0.02953	$2.931 \times 10^{-5}$	$2.096 \times 10^{-5}$	$2.097 \times 10^{-5}$	0.7154
90	0.9718	1008	0.03024	$3.086 \times 10^{-5}$	$2.139 \times 10^{-5}$	$2.201 \times 10^{-5}$	0.7132
100	0.9458	1009	0.03095	$3.243 \times 10^{-5}$	$2.181 \times 10^{-5}$	$2.306 \times 10^{-5}$	0.7111
120	0.8977	1011	0.03235	$3.565 \times 10^{-5}$	$2.264 \times 10^{-5}$	$2.522 \times 10^{-5}$	0.7073
140	0.8542	1013	0.03374	$3.898 \times 10^{-5}$	$2.345 \times 10^{-5}$	$2.745 \times 10^{-5}$	0.7041
160	0.8148	1016	0.03511	$4.241 \times 10^{-5}$	$2.420 \times 10^{-5}$	$2.975 \times 10^{-5}$	0.7014
180	0.7788	1019	0.03646	$4.593 \times 10^{-5}$	$2.504 \times 10^{-5}$	$3.212 \times 10^{-5}$	0.6992
200	0.7459	1023	0.03779	$4.954 \times 10^{-5}$	$2.577 \times 10^{-5}$	$3.455 \times 10^{-5}$	0.6974
250	0.6746	1033	0.04104	$5.890 \times 10^{-5}$	$2.760 \times 10^{-5}$	$4.091 \times 10^{-5}$	0.6946
300	0.6158	1044	0.04418	$6.871 \times 10^{-5}$	$2.934 \times 10^{-5}$	$4.765 \times 10^{-5}$	0.6935
350	0.5664	1056	0.04721	$7.892 \times 10^{-5}$	$3.101 \times 10^{-5}$	$5.475 \times 10^{-5}$	0.6937
400	0.5243	1069	0.05015	$8.951 \times 10^{-5}$	$3.261 \times 10^{-5}$	$6.219 \times 10^{-5}$	0.6948
450	0.4880	1081	0.05298	$1.004 \times 10^{-4}$	$3.415 \times 10^{-5}$	$6.997 \times 10^{-5}$	0.6965
500	0.4565	1093	0.05572	$1.117 \times 10^{-4}$	$3.563 \times 10^{-5}$	$7.806 \times 10^{-5}$	0.6986
600	0.4042	1115	0.06093	$1.352 \times 10^{-4}$	$3.846 \times 10^{-5}$	$9.515 \times 10^{-5}$	0.7037
700	0.3627	1135	0.06581	$1.598 \times 10^{-4}$	$4.111 \times 10^{-5}$	$1.133 \times 10^{-4}$	0.7092
800	0.3289	1153	0.07037	$1.855 \times 10^{-4}$	$4.362 \times 10^{-5}$	$1.326 \times 10^{-4}$	0.7149
900	0.3008	1169	0.07465	$2.122 \times 10^{-4}$	$4.600 \times 10^{-5}$	$1.529 \times 10^{-4}$	0.7206
1000	0.2772	1184	0.07868	$2.398 \times 10^{-4}$	$4.826 \times 10^{-5}$	$1.741 \times 10^{-4}$	0.7260
1500	0.1990	1234	0.09599	$3.908 \times 10^{-4}$	$5.817 \times 10^{-5}$	$2.922 \times 10^{-4}$	0.7478
2000	0.1553	1264	0.11113	$5.664 \times 10^{-4}$	$6.630 \times 10^{-5}$	$4.270 \times 10^{-4}$	0.7539

Note: For ideal gases, the properties  $c_p$ ,  $k$ ,  $\mu$ , and Pr are independent of pressure. The properties  $\rho$ ,  $\nu$ , and  $\alpha$  at a pressure  $P$  (in atm) other than 1 atm are determined by multiplying the values of  $P$  at the given temperature by  $\rho$  and by dividing  $\nu$  and  $\alpha$  by  $P$ .

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Keenan, Chao, Keyes, Gas Tables, Wiley, 1984; and Thermophysical Properties of Matter. Vol. 3: Thermal Conductivity, Y. S. Touloukian, P. E. Liley, S. C. Saxena, Vol. 11: Viscosity, Y. S. Touloukian, S. C. Saxena, and P. Hestermans, IFI/Plenum, NY, 1970, ISBN 0-306067020-8.

TABLE A-16

Properties of gases at 1 atm pressure

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr
<i>Carbon Dioxide, CO<sub>2</sub></i>							
-50	2.4035	746	0.01051	$5.860 \times 10^{-6}$	$1.129 \times 10^{-5}$	$4.699 \times 10^{-6}$	0.8019
0	1.9635	811	0.01456	$9.141 \times 10^{-6}$	$1.375 \times 10^{-5}$	$7.003 \times 10^{-6}$	0.7661
50	1.6597	866.6	0.01858	$1.291 \times 10^{-5}$	$1.612 \times 10^{-5}$	$9.714 \times 10^{-6}$	0.7520
100	1.4373	914.8	0.02257	$1.716 \times 10^{-5}$	$1.841 \times 10^{-5}$	$1.281 \times 10^{-5}$	0.7464
150	1.2675	957.4	0.02652	$2.186 \times 10^{-5}$	$2.063 \times 10^{-5}$	$1.627 \times 10^{-5}$	0.7445
200	1.1336	995.2	0.03044	$2.698 \times 10^{-5}$	$2.276 \times 10^{-5}$	$2.008 \times 10^{-5}$	0.7442
300	0.9358	1060	0.03814	$3.847 \times 10^{-5}$	$2.682 \times 10^{-5}$	$2.866 \times 10^{-5}$	0.7450
400	0.7968	1112	0.04565	$5.151 \times 10^{-5}$	$3.061 \times 10^{-5}$	$3.842 \times 10^{-5}$	0.7458
500	0.6937	1156	0.05293	$6.600 \times 10^{-5}$	$3.416 \times 10^{-5}$	$4.924 \times 10^{-5}$	0.7460
1000	0.4213	1292	0.08491	$1.560 \times 10^{-4}$	$4.898 \times 10^{-5}$	$1.162 \times 10^{-4}$	0.7455
1500	0.3025	1356	0.10688	$2.606 \times 10^{-4}$	$6.106 \times 10^{-5}$	$2.019 \times 10^{-4}$	0.7745
2000	0.2359	1387	0.11522	$3.521 \times 10^{-4}$	$7.322 \times 10^{-5}$	$3.103 \times 10^{-4}$	0.8815
<i>Carbon Monoxide, CO</i>							
-50	1.5297	1081	0.01901	$1.149 \times 10^{-5}$	$1.378 \times 10^{-5}$	$9.012 \times 10^{-6}$	0.7840
0	1.2497	1048	0.02278	$1.739 \times 10^{-5}$	$1.629 \times 10^{-5}$	$1.303 \times 10^{-5}$	0.7499
50	1.0563	1039	0.02641	$2.407 \times 10^{-5}$	$1.863 \times 10^{-5}$	$1.764 \times 10^{-5}$	0.7328
100	0.9148	1041	0.02992	$3.142 \times 10^{-5}$	$2.080 \times 10^{-5}$	$2.274 \times 10^{-5}$	0.7239
150	0.8067	1049	0.03330	$3.936 \times 10^{-5}$	$2.283 \times 10^{-5}$	$2.830 \times 10^{-5}$	0.7191
200	0.7214	1060	0.03656	$4.782 \times 10^{-5}$	$2.472 \times 10^{-5}$	$3.426 \times 10^{-5}$	0.7164
300	0.5956	1085	0.04277	$6.619 \times 10^{-5}$	$2.812 \times 10^{-5}$	$4.722 \times 10^{-5}$	0.7134
400	0.5071	1111	0.04860	$8.628 \times 10^{-5}$	$3.111 \times 10^{-5}$	$6.136 \times 10^{-5}$	0.7111
500	0.4415	1135	0.05412	$1.079 \times 10^{-4}$	$3.379 \times 10^{-5}$	$7.653 \times 10^{-5}$	0.7087
1000	0.2681	1226	0.07894	$2.401 \times 10^{-4}$	$4.557 \times 10^{-5}$	$1.700 \times 10^{-4}$	0.7080
1500	0.1925	1279	0.10458	$4.246 \times 10^{-4}$	$6.321 \times 10^{-5}$	$3.284 \times 10^{-4}$	0.7733
2000	0.1502	1309	0.13833	$7.034 \times 10^{-4}$	$9.826 \times 10^{-5}$	$6.543 \times 10^{-4}$	0.9302
<i>Methane, CH<sub>4</sub></i>							
-50	0.8761	2243	0.02367	$1.204 \times 10^{-5}$	$8.564 \times 10^{-6}$	$9.774 \times 10^{-6}$	0.8116
0	0.7158	2217	0.03042	$1.917 \times 10^{-5}$	$1.028 \times 10^{-5}$	$1.436 \times 10^{-5}$	0.7494
50	0.6050	2302	0.03766	$2.704 \times 10^{-5}$	$1.191 \times 10^{-5}$	$1.969 \times 10^{-5}$	0.7282
100	0.5240	2443	0.04534	$3.543 \times 10^{-5}$	$1.345 \times 10^{-5}$	$2.567 \times 10^{-5}$	0.7247
150	0.4620	2611	0.05344	$4.431 \times 10^{-5}$	$1.491 \times 10^{-5}$	$3.227 \times 10^{-5}$	0.7284
200	0.4132	2791	0.06194	$5.370 \times 10^{-5}$	$1.630 \times 10^{-5}$	$3.944 \times 10^{-5}$	0.7344
300	0.3411	3158	0.07996	$7.422 \times 10^{-5}$	$1.886 \times 10^{-5}$	$5.529 \times 10^{-5}$	0.7450
400	0.2904	3510	0.09918	$9.727 \times 10^{-5}$	$2.119 \times 10^{-5}$	$7.297 \times 10^{-5}$	0.7501
500	0.2529	3836	0.11933	$1.230 \times 10^{-4}$	$2.334 \times 10^{-5}$	$9.228 \times 10^{-5}$	0.7502
1000	0.1536	5042	0.22562	$2.914 \times 10^{-4}$	$3.281 \times 10^{-5}$	$2.136 \times 10^{-4}$	0.7331
1500	0.1103	5701	0.31857	$5.068 \times 10^{-4}$	$4.434 \times 10^{-5}$	$4.022 \times 10^{-4}$	0.7936
2000	0.0860	6001	0.36750	$7.120 \times 10^{-4}$	$6.360 \times 10^{-5}$	$7.395 \times 10^{-4}$	1.0386
<i>Hydrogen, H<sub>2</sub></i>							
-50	0.11010	12635	0.1404	$1.009 \times 10^{-4}$	$7.293 \times 10^{-6}$	$6.624 \times 10^{-5}$	0.6562
0	0.08995	13920	0.1652	$1.319 \times 10^{-4}$	$8.391 \times 10^{-6}$	$9.329 \times 10^{-5}$	0.7071
50	0.07603	14349	0.1881	$1.724 \times 10^{-4}$	$9.427 \times 10^{-6}$	$1.240 \times 10^{-4}$	0.7191
100	0.06584	14473	0.2095	$2.199 \times 10^{-4}$	$1.041 \times 10^{-5}$	$1.582 \times 10^{-4}$	0.7196
150	0.05806	14492	0.2296	$2.729 \times 10^{-4}$	$1.136 \times 10^{-5}$	$1.957 \times 10^{-4}$	0.7174
200	0.05193	14482	0.2486	$3.306 \times 10^{-4}$	$1.228 \times 10^{-5}$	$2.365 \times 10^{-4}$	0.7155

TABLE A-16

Properties of gases at 1 atm pressure (Concluded)

Temp. $T, ^\circ\text{C}$	Density $\rho, \text{kg/m}^3$	Specific Heat $c_p, \text{J/kg}\cdot\text{K}$	Thermal Conductivity $k, \text{W/m}\cdot\text{K}$	Thermal Diffusivity $\alpha, \text{m}^2/\text{s}$	Dynamic Viscosity $\mu, \text{kg/m}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{m}^2/\text{s}$	Prandtl Number Pr
300	0.04287	14481	0.2843	$4.580 \times 10^{-4}$	$1.403 \times 10^{-5}$	$3.274 \times 10^{-4}$	0.7149
400	0.03650	14540	0.3180	$5.992 \times 10^{-4}$	$1.570 \times 10^{-5}$	$4.302 \times 10^{-4}$	0.7179
500	0.03178	14653	0.3509	$7.535 \times 10^{-4}$	$1.730 \times 10^{-5}$	$5.443 \times 10^{-4}$	0.7224
1000	0.01930	15577	0.5206	$1.732 \times 10^{-3}$	$2.455 \times 10^{-5}$	$1.272 \times 10^{-3}$	0.7345
1500	0.01386	16553	0.6581	$2.869 \times 10^{-3}$	$3.099 \times 10^{-5}$	$2.237 \times 10^{-3}$	0.7795
2000	0.01081	17400	0.5480	$2.914 \times 10^{-3}$	$3.690 \times 10^{-5}$	$3.414 \times 10^{-3}$	1.1717
<i>Nitrogen, N<sub>2</sub></i>							
-50	1.5299	957.3	0.02001	$1.366 \times 10^{-5}$	$1.390 \times 10^{-5}$	$9.091 \times 10^{-6}$	0.6655
0	1.2498	1035	0.02384	$1.843 \times 10^{-5}$	$1.640 \times 10^{-5}$	$1.312 \times 10^{-5}$	0.7121
50	1.0564	1042	0.02746	$2.494 \times 10^{-5}$	$1.874 \times 10^{-5}$	$1.774 \times 10^{-5}$	0.7114
100	0.9149	1041	0.03090	$3.244 \times 10^{-5}$	$2.094 \times 10^{-5}$	$2.289 \times 10^{-5}$	0.7056
150	0.8068	1043	0.03416	$4.058 \times 10^{-5}$	$2.300 \times 10^{-5}$	$2.851 \times 10^{-5}$	0.7025
200	0.7215	1050	0.03727	$4.921 \times 10^{-5}$	$2.494 \times 10^{-5}$	$3.457 \times 10^{-5}$	0.7025
300	0.5956	1070	0.04309	$6.758 \times 10^{-5}$	$2.849 \times 10^{-5}$	$4.783 \times 10^{-5}$	0.7078
400	0.5072	1095	0.04848	$8.727 \times 10^{-5}$	$3.166 \times 10^{-5}$	$6.242 \times 10^{-5}$	0.7153
500	0.4416	1120	0.05358	$1.083 \times 10^{-4}$	$3.451 \times 10^{-5}$	$7.816 \times 10^{-5}$	0.7215
1000	0.2681	1213	0.07938	$2.440 \times 10^{-4}$	$4.594 \times 10^{-5}$	$1.713 \times 10^{-4}$	0.7022
1500	0.1925	1266	0.11793	$4.839 \times 10^{-4}$	$5.562 \times 10^{-5}$	$2.889 \times 10^{-4}$	0.5969
2000	0.1502	1297	0.18590	$9.543 \times 10^{-4}$	$6.426 \times 10^{-5}$	$4.278 \times 10^{-4}$	0.4483
<i>Oxygen, O<sub>2</sub></i>							
-50	1.7475	984.4	0.02067	$1.201 \times 10^{-5}$	$1.616 \times 10^{-5}$	$9.246 \times 10^{-6}$	0.7694
0	1.4277	928.7	0.02472	$1.865 \times 10^{-5}$	$1.916 \times 10^{-5}$	$1.342 \times 10^{-5}$	0.7198
50	1.2068	921.7	0.02867	$2.577 \times 10^{-5}$	$2.194 \times 10^{-5}$	$1.818 \times 10^{-5}$	0.7053
100	1.0451	931.8	0.03254	$3.342 \times 10^{-5}$	$2.451 \times 10^{-5}$	$2.346 \times 10^{-5}$	0.7019
150	0.9216	947.6	0.03637	$4.164 \times 10^{-5}$	$2.694 \times 10^{-5}$	$2.923 \times 10^{-5}$	0.7019
200	0.8242	964.7	0.04014	$5.048 \times 10^{-5}$	$2.923 \times 10^{-5}$	$3.546 \times 10^{-5}$	0.7025
300	0.6804	997.1	0.04751	$7.003 \times 10^{-5}$	$3.350 \times 10^{-5}$	$4.923 \times 10^{-5}$	0.7030
400	0.5793	1025	0.05463	$9.204 \times 10^{-5}$	$3.744 \times 10^{-5}$	$6.463 \times 10^{-5}$	0.7023
500	0.5044	1048	0.06148	$1.163 \times 10^{-4}$	$4.114 \times 10^{-5}$	$8.156 \times 10^{-5}$	0.7010
1000	0.3063	1121	0.09198	$2.678 \times 10^{-4}$	$5.732 \times 10^{-5}$	$1.871 \times 10^{-4}$	0.6986
1500	0.2199	1165	0.11901	$4.643 \times 10^{-4}$	$7.133 \times 10^{-5}$	$3.243 \times 10^{-4}$	0.6985
2000	0.1716	1201	0.14705	$7.139 \times 10^{-4}$	$8.417 \times 10^{-5}$	$4.907 \times 10^{-4}$	0.6873
<i>Water Vapor, H<sub>2</sub>O</i>							
-50	0.9839	1892	0.01353	$7.271 \times 10^{-6}$	$7.187 \times 10^{-6}$	$7.305 \times 10^{-6}$	1.0047
0	0.8038	1874	0.01673	$1.110 \times 10^{-5}$	$8.956 \times 10^{-6}$	$1.114 \times 10^{-5}$	1.0033
50	0.6794	1874	0.02032	$1.596 \times 10^{-5}$	$1.078 \times 10^{-5}$	$1.587 \times 10^{-5}$	0.9944
100	0.5884	1887	0.02429	$2.187 \times 10^{-5}$	$1.265 \times 10^{-5}$	$2.150 \times 10^{-5}$	0.9830
150	0.5189	1908	0.02861	$2.890 \times 10^{-5}$	$1.456 \times 10^{-5}$	$2.806 \times 10^{-5}$	0.9712
200	0.4640	1935	0.03326	$3.705 \times 10^{-5}$	$1.650 \times 10^{-5}$	$3.556 \times 10^{-5}$	0.9599
300	0.3831	1997	0.04345	$5.680 \times 10^{-5}$	$2.045 \times 10^{-5}$	$5.340 \times 10^{-5}$	0.9401
400	0.3262	2066	0.05467	$8.114 \times 10^{-5}$	$2.446 \times 10^{-5}$	$7.498 \times 10^{-5}$	0.9240
500	0.2840	2137	0.06677	$1.100 \times 10^{-4}$	$2.847 \times 10^{-5}$	$1.002 \times 10^{-4}$	0.9108
1000	0.1725	2471	0.13623	$3.196 \times 10^{-4}$	$4.762 \times 10^{-5}$	$2.761 \times 10^{-4}$	0.8639
1500	0.1238	2736	0.21301	$6.288 \times 10^{-4}$	$6.411 \times 10^{-5}$	$5.177 \times 10^{-4}$	0.8233
2000	0.0966	2928	0.29183	$1.032 \times 10^{-3}$	$7.808 \times 10^{-5}$	$8.084 \times 10^{-4}$	0.7833

Note: For ideal gases, the properties  $c_p$ ,  $k$ ,  $\mu$ , and Pr are independent of pressure. The properties  $\rho$ ,  $\nu$ , and  $\alpha$  at a pressure  $P$  (in atm) other than 1 atm are determined by multiplying the values of  $P$  at the given temperature by  $\rho$  and by dividing  $\nu$  and  $\alpha$  by  $P$ .

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-17

Properties of the atmosphere at high altitude

Altitude, $z$ , m	Temperature, $T$ , °C	Pressure, $P$ , kPa	Gravity $g$ , m/s <sup>2</sup>	Speed of Sound, $c$ , m/s	Density, $\rho$ , kg/m <sup>3</sup>	Viscosity $\mu$ , kg/m·s	Thermal Conductivity, $k$ , W/m·K
0	15.00	101.33	9.807	340.3	1.225	$1.789 \times 10^{-5}$	0.0253
200	13.70	98.95	9.806	339.5	1.202	$1.783 \times 10^{-5}$	0.0252
400	12.40	96.61	9.805	338.8	1.179	$1.777 \times 10^{-5}$	0.0252
600	11.10	94.32	9.805	338.0	1.156	$1.771 \times 10^{-5}$	0.0251
800	9.80	92.08	9.804	337.2	1.134	$1.764 \times 10^{-5}$	0.0250
1000	8.50	89.88	9.804	336.4	1.112	$1.758 \times 10^{-5}$	0.0249
1200	7.20	87.72	9.803	335.7	1.090	$1.752 \times 10^{-5}$	0.0248
1400	5.90	85.60	9.802	334.9	1.069	$1.745 \times 10^{-5}$	0.0247
1600	4.60	83.53	9.802	334.1	1.048	$1.739 \times 10^{-5}$	0.0245
1800	3.30	81.49	9.801	333.3	1.027	$1.732 \times 10^{-5}$	0.0244
2000	2.00	79.50	9.800	332.5	1.007	$1.726 \times 10^{-5}$	0.0243
2200	0.70	77.55	9.800	331.7	0.987	$1.720 \times 10^{-5}$	0.0242
2400	-0.59	75.63	9.799	331.0	0.967	$1.713 \times 10^{-5}$	0.0241
2600	-1.89	73.76	9.799	330.2	0.947	$1.707 \times 10^{-5}$	0.0240
2800	-3.19	71.92	9.798	329.4	0.928	$1.700 \times 10^{-5}$	0.0239
3000	-4.49	70.12	9.797	328.6	0.909	$1.694 \times 10^{-5}$	0.0238
3200	-5.79	68.36	9.797	327.8	0.891	$1.687 \times 10^{-5}$	0.0237
3400	-7.09	66.63	9.796	327.0	0.872	$1.681 \times 10^{-5}$	0.0236
3600	-8.39	64.94	9.796	326.2	0.854	$1.674 \times 10^{-5}$	0.0235
3800	-9.69	63.28	9.795	325.4	0.837	$1.668 \times 10^{-5}$	0.0234
4000	-10.98	61.66	9.794	324.6	0.819	$1.661 \times 10^{-5}$	0.0233
4200	-12.3	60.07	9.794	323.8	0.802	$1.655 \times 10^{-5}$	0.0232
4400	-13.6	58.52	9.793	323.0	0.785	$1.648 \times 10^{-5}$	0.0231
4600	-14.9	57.00	9.793	322.2	0.769	$1.642 \times 10^{-5}$	0.0230
4800	-16.2	55.51	9.792	321.4	0.752	$1.635 \times 10^{-5}$	0.0229
5000	-17.5	54.05	9.791	320.5	0.736	$1.628 \times 10^{-5}$	0.0228
5200	-18.8	52.62	9.791	319.7	0.721	$1.622 \times 10^{-5}$	0.0227
5400	-20.1	51.23	9.790	318.9	0.705	$1.615 \times 10^{-5}$	0.0226
5600	-21.4	49.86	9.789	318.1	0.690	$1.608 \times 10^{-5}$	0.0224
5800	-22.7	48.52	9.785	317.3	0.675	$1.602 \times 10^{-5}$	0.0223
6000	-24.0	47.22	9.788	316.5	0.660	$1.595 \times 10^{-5}$	0.0222
6200	-25.3	45.94	9.788	315.6	0.646	$1.588 \times 10^{-5}$	0.0221
6400	-26.6	44.69	9.787	314.8	0.631	$1.582 \times 10^{-5}$	0.0220
6600	-27.9	43.47	9.786	314.0	0.617	$1.575 \times 10^{-5}$	0.0219
6800	-29.2	42.27	9.785	313.1	0.604	$1.568 \times 10^{-5}$	0.0218
7000	-30.5	41.11	9.785	312.3	0.590	$1.561 \times 10^{-5}$	0.0217
8000	-36.9	35.65	9.782	308.1	0.526	$1.527 \times 10^{-5}$	0.0212
9000	-43.4	30.80	9.779	303.8	0.467	$1.493 \times 10^{-5}$	0.0206
10,000	-49.9	26.50	9.776	299.5	0.414	$1.458 \times 10^{-5}$	0.0201
12,000	-56.5	19.40	9.770	295.1	0.312	$1.422 \times 10^{-5}$	0.0195
14,000	-56.5	14.17	9.764	295.1	0.228	$1.422 \times 10^{-5}$	0.0195
16,000	-56.5	10.53	9.758	295.1	0.166	$1.422 \times 10^{-5}$	0.0195
18,000	-56.5	7.57	9.751	295.1	0.122	$1.422 \times 10^{-5}$	0.0195

Source: U.S. Standard Atmosphere Supplements, U.S. Government Printing Office, 1966.

TABLE A-18

## Emissivities of surfaces

## (a) Metals

Material	Temperature, K	Emissivity, $\epsilon$	Material	Temperature, K	Emissivity, $\epsilon$
Aluminum			Magnesium, polished	300–500	0.07–0.13
Polished	300–900	0.04–0.06	Mercury	300–400	0.09–0.12
Commercial sheet	400	0.09	Molybdenum		
Heavily oxidized	400–800	0.20–0.33	Polished	300–2000	0.05–0.21
Anodized	300	0.8	Oxidized	600–800	0.80–0.82
Bismuth, bright	350	0.34	Nickel		
Brass			Polished	500–1200	0.07–0.17
Highly polished	500–650	0.03–0.04	Oxidized	450–1000	0.37–0.57
Polished	350	0.09	Platinum, polished	500–1500	0.06–0.18
Dull plate	300–600	0.22	Silver, polished	300–1000	0.02–0.07
Oxidized	450–800	0.6	Stainless steel		
Chromium, polished	300–1400	0.08–0.40	Polished	300–1000	0.17–0.30
Copper			Lightly oxidized	600–1000	0.30–0.40
Highly polished	300	0.02	Highly oxidized	600–1000	0.70–0.80
Polished	300–500	0.04–0.05	Steel		
Commercial sheet	300	0.15	Polished sheet	300–500	0.08–0.14
Oxidized	600–1000	0.5–0.8	Commercial sheet	500–1200	0.20–0.32
Black oxidized	300	0.78	Heavily oxidized	300	0.81
Gold			Tin, polished	300	0.05
Highly polished	300–1000	0.03–0.06	Tungsten		
Bright foil	300	0.07	Polished	300–2500	0.03–0.29
Iron			Filament	3500	0.39
Highly polished	300–500	0.05–0.07	Zinc		
Case iron	300	0.44	Polished	300–800	0.02–0.05
Wrought iron	300–500	0.28	Oxidized	300	0.25
Rusted	300	0.61			
Oxidized	500–900	0.64–0.78			
Lead					
Polished	300–500	0.06–0.08			
Unoxidized, rough	300	0.43			
Oxidized	300	0.63			



TABLE A-18

Emissivities of surfaces

(b) Nonmetals (Concluded)

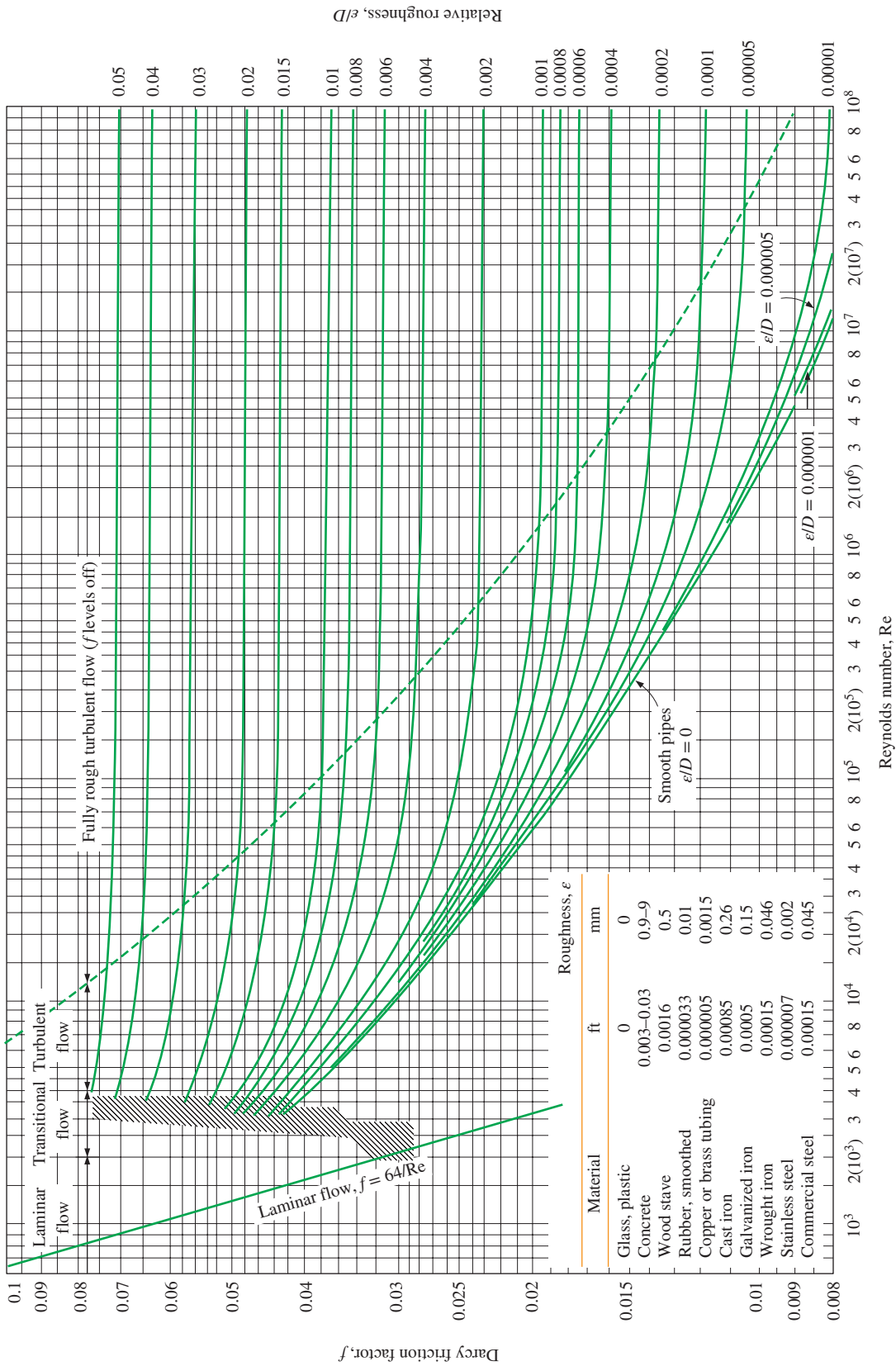
Material	Temperature, K	Emissivity, $\epsilon$	Material	Temperature, K	Emissivity, $\epsilon$
Alumina	800–1400	0.65–0.45	Paper, white	300	0.90
Aluminum oxide	600–1500	0.69–0.41	Plaster, white	300	0.93
Asbestos	300	0.96	Porcelain, glazed	300	0.92
Asphalt pavement	300	0.85–0.93	Quartz, rough, fused	300	0.93
Brick			Rubber		
Common	300	0.93–0.96	Hard	300	0.93
Fireclay	1200	0.75	Soft	300	0.86
Carbon filament	2000	0.53	Sand	300	0.90
Cloth	300	0.75–0.90	Silicon carbide	600–1500	0.87–0.85
Concrete	300	0.88–0.94	Skin, human	300	0.95
Glass			Snow	273	0.80–0.90
Window	300	0.90–0.95	Soil, earth	300	0.93–0.96
Pyrex	300–1200	0.82–0.62	Soot	300–500	0.95
Pyroceram	300–1500	0.85–0.57	Teflon	300–500	0.85–0.92
Ice	273	0.95–0.99	Water, deep	273–373	0.95–0.96
Magnesium oxide	400–800	0.69–0.55	Wood		
Masonry	300	0.80	Beech	300	0.94
Paints			Oak	300	0.90
Aluminum	300	0.40–0.50			
Black, lacquer, shiny	300	0.88			
Oils, all colors	300	0.92–0.96			
Red primer	300	0.93			
White acrylic	300	0.90			
White enamel	300	0.90			

TABLE A-19

## Solar radiative properties of materials

Description/composition	Solar Absorptivity, $\alpha_s$	Emissivity, $\epsilon$ , at 300 K	Ratio, $\alpha_s/\epsilon$	Solar Transmissivity, $\tau_s$
Aluminum				
Polished	0.09	0.03	3.0	
Anodized	0.14	0.84	0.17	
Quartz-overcoated	0.11	0.37	0.30	
Foil	0.15	0.05	3.0	
Brick, red (Purdue)	0.63	0.93	0.68	
Concrete	0.60	0.88	0.68	
Galvanized sheet metal				
Clean, new	0.65	0.13	5.0	
Oxidized, weathered	0.80	0.28	2.9	
Glass, 3.2-mm thickness				
Float or tempered				0.79
Low iron oxide type				0.88
Marble, slightly off-white (nonreflective)	0.40	0.88	0.45	
Metal, plated				
Black sulfide	0.92	0.10	9.2	
Black cobalt oxide	0.93	0.30	3.1	
Black nickel oxide	0.92	0.08	11	
Black chrome	0.87	0.09	9.7	
Mylar, 0.13-mm thickness				0.87
Paints				
Black (Parsons)	0.98	0.98	1.0	
White, acrylic	0.26	0.90	0.29	
White, zinc oxide	0.16	0.93	0.17	
Paper, white	0.27	0.83	0.32	
Plexiglas, 3.2-mm thickness				0.90
Porcelain tiles, white (reflective glazed surface)	0.26	0.85	0.30	
Roofing tiles, bright red				
Dry surface	0.65	0.85	0.76	
Wet surface	0.88	0.91	0.96	
Sand, dry				
Off-white	0.52	0.82	0.63	
Dull red	0.73	0.86	0.82	
Snow				
Fine particles, fresh	0.13	0.82	0.16	
Ice granules	0.33	0.89	0.37	
Steel				
Mirror-finish	0.41	0.05	8.2	
Heavily rusted	0.89	0.92	0.96	
Stone (light pink)	0.65	0.87	0.74	
Tedlar, 0.10-mm thickness				0.92
Teflon, 0.13-mm thickness				0.92
Wood	0.59	0.90	0.66	

Source: V. C. Sharma and A. Sharma, "Solar Properties of Some Building Elements," *Energy* 14 (1989), pp. 805–810, and other sources.



**FIGURE A-20**

The Moody chart for the friction factor for fully developed flow in circular pipes for use in the head loss relation  $\Delta P_L = f \frac{L \rho V^2}{D 2}$ . Friction factors in the turbulent flow are evaluated from the Colebrook equation  $\frac{1}{\sqrt{f}} = -2 \log_{10} \left( \frac{\epsilon/D}{3.7} + \frac{2.51}{Re \sqrt{f}} \right)$ .



# PROPERTY TABLES AND CHARTS (ENGLISH UNITS)

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TABLE A-1E

Molar mass, gas constant, and ideal-gas specific heats of some substances

Substance	Molar Mass, $M$ , lbm/lbmol	Gas Constant $R^*$		Specific Heat Data at 77°F		
		Btu/ lbm·R	psia·ft <sup>3</sup> / lbm·R	$c_p$ , Btu/lbm·R	$c_v$ , Btu/lbm·R	$k = c_p/c_v$
Air	28.97	0.06855	0.3704	0.2400	0.1715	1.400
Ammonia, NH <sub>3</sub>	17.03	0.1166	0.6301	0.4999	0.3834	1.304
Argon, Ar	39.95	0.04970	0.2686	0.1243	0.07457	1.667
Bromine, Br <sub>2</sub>	159.81	0.01242	0.06714	0.0538	0.04137	1.300
Isobutane, C <sub>4</sub> H <sub>10</sub>	58.12	0.03415	0.1846	0.3972	0.3631	1.094
<i>n</i> -Butane, C <sub>4</sub> H <sub>10</sub>	58.12	0.03415	0.1846	0.4046	0.3705	1.092
Carbon dioxide, CO <sub>2</sub>	44.01	0.04512	0.2438	0.2016	0.1564	1.288
Carbon monoxide, CO	28.01	0.07089	0.3831	0.2482	0.1772	1.400
Chlorine, Cl <sub>2</sub>	70.905	0.02802	0.1514	0.1142	0.08618	1.325
Chlorodifluoromethane (R-22), CHClF <sub>2</sub>	86.47	0.02297	0.1241	0.1552	0.1322	1.174
Ethane, C <sub>2</sub> H <sub>6</sub>	30.070	0.06604	0.3569	0.4166	0.3506	1.188
Ethylene, C <sub>2</sub> H <sub>4</sub>	28.054	0.07079	0.3826	0.3647	0.2940	1.241
Fluorine, F <sub>2</sub>	38.00	0.05224	0.2823	0.1967	0.1445	1.362
Helium, He	4.003	0.4961	2.681	1.2403	0.7442	1.667
<i>n</i> -Heptane, C <sub>7</sub> H <sub>16</sub>	100.20	0.01982	0.1071	0.3939	0.3740	1.053
<i>n</i> -Hexane, C <sub>6</sub> H <sub>14</sub>	86.18	0.02304	0.1245	0.3951	0.3721	1.062
Hydrogen, H <sub>2</sub>	2.016	0.9850	5.323	3.416	2.431	1.405
Krypton, Kr	83.80	0.02370	0.1281	0.05923	0.03554	1.667
Methane, CH <sub>4</sub>	16.04	0.1238	0.6688	0.5317	0.4080	1.303
Neon, Ne	20.183	0.09838	0.5316	0.2460	0.1476	1.667
Nitrogen, N <sub>2</sub>	28.01	0.07089	0.3831	0.2484	0.1774	1.400
Nitric oxide, NO	30.006	0.06618	0.3577	0.2387	0.1725	1.384
Nitrogen dioxide, NO <sub>2</sub>	46.006	0.04512	0.2438	0.1925	0.1474	1.306
Oxygen, O <sub>2</sub>	32.00	0.06205	0.3353	0.2193	0.1572	1.395
<i>n</i> -Pentane, C <sub>5</sub> H <sub>12</sub>	72.15	0.02752	0.1487	0.3974	0.3700	1.074
Propane, C <sub>3</sub> H <sub>8</sub>	44.097	0.04502	0.2433	0.3986	0.3535	1.127
Propylene, C <sub>3</sub> H <sub>6</sub>	42.08	0.04720	0.2550	0.3657	0.3184	1.148
Steam, H <sub>2</sub> O	18.015	0.1102	0.5957	0.4455	0.3351	1.329
Sulfur dioxide, SO <sub>2</sub>	64.06	0.03100	0.1675	0.1488	0.1178	1.263
Tetrachloromethane, CCl <sub>4</sub>	153.82	0.01291	0.06976	0.1293	0.1164	1.111
Tetrafluoroethane (R-134a), C <sub>2</sub> H <sub>2</sub> F <sub>4</sub>	102.03	0.01946	0.1052	0.1991	0.1796	1.108
Trifluoroethane (R-143a), C <sub>2</sub> H <sub>3</sub> F <sub>3</sub>	84.04	0.02363	0.1277	0.2219	0.1983	1.119
Xenon, Xe	131.30	0.01512	0.08173	0.03781	0.02269	1.667

\*The gas constant is calculated from  $R = R_u/M$ , where  $R_u = 1.9859$  Btu/lbmol·R = 10.732 psia·ft<sup>3</sup>/lbmol·R is the universal gas constant and  $M$  is the molar mass.

Source: Specific heat values are mostly obtained from the property routines prepared by The National Institute of Standards and Technology (NIST), Gaithersburg, MD.

TABLE A-2E

## Boiling and freezing point properties

Substance	Boiling Data at 1 atm		Freezing Data		Liquid Properties		
	Normal Boiling Point, °F	Latent Heat of Vaporization $h_{fg}$ , Btu/lbm	Freezing Point, °F	Latent Heat of Fusion $h_{if}$ , Btu/lbm	Temperature, °F	Density $\rho$ , lbm/ft <sup>3</sup>	Specific Heat $c_p$ , Btu/lbm·R
Ammonia	-27.9	24.54	-107.9	138.6	-27.9	42.6	1.06
					0	41.3	1.083
					40	39.5	1.103
					80	37.5	1.135
Argon	-302.6	69.5	-308.7	12.0	-302.6	87.0	0.272
Benzene	176.4	169.4	41.9	54.2	68	54.9	0.411
Brine (20% sodium chloride by mass)	219.0	—	0.7	—	68	71.8	0.743
<i>n</i> -Butane	31.1	165.6	-217.3	34.5	31.1	37.5	0.552
Carbon dioxide	-109.2*	99.6 (at 32°F)	-69.8	—	32	57.8	0.583
Ethanol	172.8	360.5	-173.6	46.9	77	48.9	0.588
Ethyl alcohol	173.5	368	-248.8	46.4	68	49.3	0.678
Ethylene glycol	388.6	344.0	12.6	77.9	68	69.2	0.678
Glycerin	355.8	419	66.0	86.3	68	78.7	0.554
Helium	-452.1	9.80	—	—	-452.1	9.13	5.45
Hydrogen	-423.0	191.7	-434.5	25.6	-423.0	4.41	2.39
Isobutane	10.9	157.8	-255.5	45.5	10.9	37.1	0.545
Kerosene	399–559	108	-12.8	—	68	51.2	0.478
Mercury	674.1	126.7	-38.0	4.90	77	847	0.033
Methane	-258.7	219.6	296.0	25.1	-258.7	26.4	0.834
					-160	20.0	1.074
Methanol	148.1	473	-143.9	42.7	77	49.1	0.609
Nitrogen	-320.4	85.4	-346.0	10.9	-320.4	50.5	0.492
					-260	38.2	0.643
Octane	256.6	131.7	-71.5	77.9	68	43.9	0.502
Oil (light)	—	—	—	—	77	56.8	0.430
Oxygen	-297.3	91.5	-361.8	5.9	-297.3	71.2	0.408
Petroleum	—	99–165	—	—	68	40.0	0.478
Propane	-43.7	184.0	-305.8	34.4	-43.7	36.3	0.538
					32	33.0	0.604
					100	29.4	0.673
					-40	88.5	0.283
Refrigerant-134a	-15.0	93.2	-141.9	—	-15	86.0	0.294
					32	80.9	0.318
					90	73.6	0.348
					32	62.4	1.01
Water	212	970.5	32	143.5	32	62.4	1.01
					90	62.1	1.00
					150	61.2	1.00
					212	59.8	1.01

\*Sublimation temperature. (At pressures below the triple-point pressure of 75.1 psia, carbon dioxide exists as a solid or gas. Also, the freezing-point temperature of carbon dioxide is the triple-point temperature of -69.8°F.)

**TABLE A-3E**

Properties of solid metals

Composition	Melting Point, R	Properties at 540 R				Properties at Various Temperatures (R), $k(\text{Btu}/\text{h}\cdot\text{ft}\cdot\text{R})/c_p(\text{Btu}/\text{lbm}\cdot\text{R})$					
		$\rho$ lbm/ft <sup>3</sup>	$c_p$ (Btu/ lbm·R)	$k$ (Btu/ h·ft·R)	$\alpha \times 10^6$ ft <sup>2</sup> /s	180	360	720	1080	1440	1800
Aluminum	1679	168	0.216	137	1045	174.5	137	138.6	133.4	126	
Pure						0.115	0.191	0.226	0.246	0.273	
Alloy 2024-T6 (4.5% Cu, 1.5% Mg, 0.6% Mn)	1395	173	0.209	102.3	785.8	37.6	94.2	107.5	107.5		
Alloy 195, cast (4.5% Cu)		174.2	0.211	97	734	0.113	0.188	0.22	0.249		
Beryllium	2790	115.5	0.436	115.6	637.2	572	174	93	72.8	61.3	52.5
						0.048	0.266	0.523	0.621	0.624	0.72
Bismuth	981	610.5	0.029	4.6	71	9.5	5.6	4.06			
						0.026	0.028	0.03			
Boron	4631	156	0.264	15.6	105	109.7	32.06	9.7	6.1	5.5	5.7
						0.03	0.143	0.349	0.451	0.515	0.558
Cadmium	1069	540	0.055	55.6	521	117.3	57.4	54.7			
						0.047	0.053	0.057			
Chromium	3812	447	0.107	54.1	313.2	91.9	64.1	52.5	46.6	41.2	37.8
						0.045	0.091	0.115	0.129	0.138	0.147
Cobalt	3184	553.2	0.101	57.3	286.3	96.5	70.5	49.3	39	33.6	80.1
						0.056	0.09	0.107	0.12	0.131	0.145
Copper	2445	559	0.092	231.7	1259.3	278.5	238.6	227.07	219	212	203.4
Pure						0.06	0.085	0.094	0.01	0.103	0.107
Commercial bronze (90% Cu, 10% Al)	2328	550	0.1	30	150.7	24.3	30	34			
Phosphor gear bronze (89% Cu, 11% Sn)	1987	548.1	0.084	31.2	183	23.7	37.6	42.8			
Cartridge brass (70% Cu, 30% Zn)	2139	532.5	0.09	63.6	364.9	43.3	54.9	79.2	86.0		
Constantan (55% Cu, 45% Ni)	2687	557	0.092	13.3	72.3	9.8	1.1	0.09			
Germanium	2180	334.6	0.08	34.6	373.5	134	56	25	15.7	11.4	10.05
						0.045	0.069	0.08	0.083	0.085	0.089
Gold	2405	1205	0.03	183.2	1367	189	186.6	179.7	172.2	164.09	156
						0.026	0.029	0.031	0.032	0.033	0.034
Iridium	4896	1404.6	0.031	85	541.4	99.4	88.4	83.2	79.7	76.3	72.8
						0.021	0.029	0.031	0.032	0.034	0.036
Iron:	3258	491.3	0.106	46.4	248.6	77.4	54.3	40.2	31.6	25.01	19
Pure						0.051	0.091	0.117	0.137	0.162	0.232
Armco (99.75% pure)		491.3	0.106	42	222.8	55.2	46.6	38	30.7	24.4	18.7
Carbon steels		490.3	0.103	35	190.6	0.051	0.091	0.117	0.137	0.162	0.233
Plain carbon (Mn ≤ 1%, Si ≤ 0.1%)								32.8	27.7	22.7	17.4
AISI 1010		489	0.103	37	202.4			0.116	0.113	0.163	0.279
Carbon-silicon (Mn ≤ 1%, 0.1% < Si ≤ 0.6%)		488	0.106	30	160.4			0.116	0.133	0.163	0.278
Carbon-manganese-silicon (1% < Mn ≤ 1.65%, 0.1% < Si ≤ 0.6%)		508	0.104	23.7	125			0.119	0.139	0.166	0.231
Chromium (low) steels:		488.3	0.106	21.8	117.4			22	21.2	19.3	15.6
$\frac{1}{2}$ Cr– $\frac{1}{4}$ Mo–Si (0.18% C, 0.65% Cr, 0.23% Mo, 0.6% Si)								0.117	0.137	0.164	0.23
1 Cr– $\frac{1}{2}$ Mo (0.16% C, 1% Cr, 0.54% Mo, 0.39% Si)		490.6	0.106	24.5	131.3			24.3	22.6	20	15.8
1 Cr–V (0.2% C, 1.02% Cr, 0.15% V)		489.2	0.106	28.3	151.8			0.117	0.137	0.164	0.231



TABLE A-3E

Properties of solid metals (Concluded)

Composition	Melting Point, R	Properties at 540 R				Properties at Various Temperatures (R), $k(\text{Btu}/\text{h}\cdot\text{ft}\cdot\text{R})/c_p(\text{Btu}/\text{lbm}\cdot\text{R})$					
		$\rho$	$c_p$	$k$	$\alpha \times 10^6$	180	360	720	1080	1440	1800
		lbm/ft <sup>3</sup>	lbm·R)	h·ft·R)	ft <sup>2</sup> /s						
Stainless steels:		503	0.114	8.7	42			10	11.6	13.2	14.7
AISI 302								0.122	0.133	0.140	0.144
AISI 304	3006	493.2	0.114	8.6	42.5	5.31	7.3	9.6	11.5	13	14.7
AISI 316		514.3	0.111	7.8	37.5	0.064	0.096	0.123	0.133	0.139	0.145
AISI 347		498	0.114	8.2	40	0.12	0.131	0.137	0.143		14
AISI 347								0.122	0.133	0.14	0.144
Lead	1082	708	0.03	20.4	259.4	23	21.2	19.7	18.1		
						0.028	0.029	0.031	0.034		
Magnesium	1661	109	0.245	90.2	943	87.9	91.9	88.4	86.0	84.4	
						0.155	0.223	0.256	0.279	0.302	
Molybdenum	5209	639.3	0.06	79.7	578	1034	82.6	77.4	72.8	68.2	64.7
						0.038	0.053	0.062	0.065	0.068	0.070
Nickel:	3110	555.6	0.106	52.4	247.6	94.8	61.8	46.3	37.9	39	41.4
Pure						0.055	0.091	0.115	0.141	0.126	0.134
Nichrome (80% Ni, 20% Cr)	3010	524.4	0.1	6.9	36.6			8.0	9.3	12.2	
Inconel X-750 (73% Ni, 15% Cr, 6.7% Fe)	2997	531.3	0.104	6.8	33.4	5	5.9	7.8	9.8	11.8	13.9
Niobium	4934	535	0.063	31	254	—	0.088	0.112	0.121	0.13	0.149
						31.9	30.4	32	33.6	35.4	32.2
						0.044	0.059	0.065	0.067	0.069	0.071
Palladium	3289	750.4	0.058	41.5	263.7	44.2	41.4	42.5	46	50	54.4
						0.04	0.054	0.059	0.062	0.064	0.067
Platinum:	3681	1339	0.031	41.4	270	44.7	42	41.5	42.3	43.7	45.5
Pure						0.024	0.03	0.032	0.034	0.035	0.036
Alloy 60Pt-40Rh (60% Pt, 40% Rh)	3240	1038.2	0.038	27.2	187.3			30	34	37.5	40
Rhenium	6215	1317.2	0.032	27.7	180	34	30	26.6	25.5	25.4	25.8
						0.023	0.03	0.033	0.034	0.036	0.037
Rhodium	4025	777.2	0.058	86.7	534	107.5	89	84.3	78.5	73.4	70
						0.035	0.052	0.06	0.065	0.069	0.074
Silicon	3033	145.5	0.17	85.5	960.2	510.8	152.5	57.2	35.8	24.4	18.0
						0.061	0.132	0.189	0.207	0.218	0.226
Silver	2223	656	0.056	248	1873	257	248.4	245.5	238	228.8	219
						0.044	0.053	0.057	0.059	0.062	0.066
Tantalum	5884	1036.3	0.033	33.2	266	34.2	33.2	33.4	34	34.3	34.8
						0.026	0.031	0.034	0.035	0.036	0.036
Thorium	3641	730.4	0.028	31.2	420.9	34.6	31.5	31.4	32.2	32.9	32.9
						0.024	0.027	0.029	0.032	0.035	0.037
Tin	909	456.3	0.054	38.5	431.6	49.2	42.4	35.9			
						0.044	0.051	0.058			
Titanium	3515	281	0.013	12.7	100.3	17.6	14.2	11.8	11.2	11.4	12
						0.071	0.111	0.131	0.141	0.151	0.161
Tungsten	6588	1204.9	0.031	100.5	735.2	120.2	107.5	92	79.2	72.2	68.2
						0.020	0.029	0.032	0.033	0.034	0.035
Uranium	2531	1190.5	0.027	16	134.5	12.5	14.5	17.1	19.6	22.4	25.4
						0.022	0.026	0.029	0.035	0.042	0.043
Vanadium	3946	381	0.117	17.7	110.9	20.7	18	18	19.3	20.6	22.0
						0.061	0.102	0.123	0.128	0.134	0.142
Zinc	1247	445.7	0.093	67	450	67.6	68.2	64.1	59.5		
						0.07	0.087	0.096	0.104		
Zirconium	3825	410.2	0.067	13.1	133.5	19.2	14.6	12.5	12	12.5	13.7
						0.049	0.063	0.072	0.77	0.082	0.087

Source: Tables A-3E and A-4E are obtained from the respective tables in SI units in Appendix 1 using proper conversion factors.

TABLE A-4E

## Properties of solid nonmetals

Composition	Melting Point, R	Properties at 540 R				Properties at Various Temperatures (R), $k(\text{Btu/h}\cdot\text{ft}\cdot\text{R})/c_p(\text{Btu/lbm}\cdot\text{R})$					
		$\rho$ lbm/ft <sup>3</sup>	$c_p(\text{Btu/lbm}\cdot\text{R})$	$k(\text{Btu/h}\cdot\text{ft}\cdot\text{R})$	$\alpha \times 10^6$ ft <sup>2</sup> /s	180	360	720	1080	1440	1800
Aluminum oxide, sapphire	4181	247.8	0.182	26.6	162.5	260	47.4	18.7	11	7.5	6
Aluminum oxide polycrystalline	4181	247.8	0.182	20.8	128	—	—	0.224	0.265	0.281	0.293
Beryllium oxide	4905	187.3	0.246	157.2	947.3	76.8	31.7	15.3	9.3	6	4.5
Boron	4631	156	0.264	16	107.5	—	—	0.244	0.265	0.281	0.293
Boron fiber epoxy (30% vol.) composite	4631	156	0.264	16	107.5	109.8	30.3	113.2	64.2	40.4	27.2
$k$ ,    to fibers								0.322	0.40	0.44	0.459
$k$ , $\perp$ to fibers								10.8	6.5	4.6	3.6
$c_p$								0.355	0.445	0.509	0.561
Carbon	1062	130									
Amorphous diamond, type IIa	2700	121.7	—	0.92	—	1.2	1.3	1.31			
insulator	—	219	0.121	1329	—	0.21	0.28	0.34			
Graphite, pyrolytic	4091	138				0.086	0.18	0.34			
$k$ ,    to layers						0.38	0.68	1.09	1.26	1.36	1.46
$k$ , $\perp$ to layers						5778	2311.2	889.8			
$c_p$							0.005	0.046	0.203		
Graphite fiber epoxy (25% vol.) composite	810	87.4				2871.6	1866.3	803.2	515.4	385.4	308.5
$k$ , heat flow    to fibers						9.7	5.3	2.4	1.5	1.16	0.92
$k$ , heat flow $\perp$ to fibers			0.169			0.32	0.098	0.236	0.335	0.394	0.428
$c_p$											
Pyroceram, Corning 9606	2921	162.3	0.193	2.3	20.3	3.0	2.3	2.1	1.9	1.7	1.7
Silicon carbide	5580	197.3	0.161	283.1	2475.7			—	—	—	50.3
Silicon dioxide, crystalline (quartz)	3389	165.4						0.210	0.25	0.27	0.285
$k$ ,    to $c$ -axis				6		22.5	9.5	4.4	2.9	2.4	
$k$ , $\perp$ to $c$ -axis				3.6		12.0	5.9	2.7	2	1.8	
$c_p$			0.177					0.211	0.256	0.298	
Silicon dioxide, polycrystalline (fused silica)	3389	138.6	0.177	0.79	9	0.4	0.65	0.87	1.01	1.25	1.65
Silicon nitride	3911	150	0.165	9.2	104	—	—	0.216	0.248	0.264	0.276
Sulfur	706	130	0.169	0.1	1.51	—	0.138	8.0	6.5	5.7	5.0
Thorium dioxide	6431	568.7	0.561	7.5	65.7	0.095	0.1	0.185	0.223	0.253	0.275
Titanium dioxide, polycrystalline	3840	259.5	0.170	4.9	30.1	0.962	0.144	—	—	—	—
								5.9	3.8	2.7	2.12
								0.609	0.654	0.680	0.704
								4.0	2.9	2.3	2
								0.192	0.210	0.217	0.222

Source: Tables A-3E and A-4E are obtained from the respective tables in SI units in Appendix 1 using proper conversion factors.

TABLE A-5E

Properties of building materials  
(at a mean temperature of 75°F)

Material	Thickness, $L$ in	Density, $\rho$ lbm/ft <sup>3</sup>	Thermal Conductivity, $k$ Btu·in/h·ft <sup>2</sup> ·°F	Specific Heat, $c_p$ Btu/lbm·R	$R$ -value (for listed thickness, $L/k$ ), °F·h·ft <sup>2</sup> /Btu
<b>Building Boards</b>					
Asbestos-cement board	¼ in.	120	—	0.24	0.06
Gypsum of plaster board	⅜ in.	50	—	0.26	0.32
	½ in.	50	—	—	0.45
Plywood (Douglas fir)	—	34	0.80	0.29	—
	¼ in.	34	—	0.29	0.31
	⅜ in.	34	—	0.29	0.47
	½ in.	34	—	0.29	0.62
	¾ in.	34	—	0.29	0.93
Insulated board and sheathing (regular density)	½ in.	18	—	0.31	1.32
	<sup>25</sup> / <sub>32</sub> in.	18	—	0.31	2.06
Hardboard (high density, standard tempered)	—	63	1.00	0.32	—
Particle board					
Medium density	—	50	0.94	0.31	—
Underlayment	⅝ in.	40	—	0.29	0.82
Wood subfloor	¾ in.	—	—	0.33	0.94
<b>Building Membranes</b>					
Vapor-permeable felt	—	—	—	—	0.06
Vapor seal (2 layers of mopped 17.3 lbm/ft <sup>2</sup> felt)	—	—	—	—	0.12
<b>Flooring Materials</b>					
Carpet and fibrous pad	—	—	—	0.34	2.08
Carpet and rubber pad	—	—	—	0.33	1.23
Tile (asphalt, linoleum, vinyl)	—	—	—	0.30	0.05
<b>Masonry Materials</b>					
<i>Masonry units:</i>					
Brick, common		120	5.0	—	—
Brick, face		130	9.0	—	—
Brick, fire clay		150	9.3	—	—
		120	6.2	0.19	—
		70	2.8	—	—
Concrete blocks (3 oval cores, sand and gravel aggregate)	4 in.	—	5.34	—	0.71
	8 in.	—	6.94	—	1.11
	12 in.	—	9.02	—	1.28
<i>Concretes</i>					
Lightweight aggregates		120	5.2	—	—
(including expanded shale, clay, or slate, expanded slags, cinders; pumice; and scoria)		100	3.6	0.2	—
		80	2.5	0.2	—
		60	1.7	—	—
		40	1.15	—	—
Cement/lime, mortar, and stucco		120	9.7	—	—
		80	4.5	—	—
Stucco		116	5.0	—	—

TABLE A-5E

Properties of building materials (*Concluded*)  
(at a mean temperature of 75°F)

Material	Thickness, $L$ in	Density, $\rho$ lbm/ft <sup>3</sup>	Thermal Conductivity, $k$ Btu·in/h·ft <sup>2</sup> ·°F	Specific Heat, $c_p$ Btu/lbm·R	$R$ -value (for listed thickness, $L/k$ ), °F·h·ft <sup>2</sup> /Btu
<b>Roofing</b>					
Asbestos-cement shingles		120	—	0.24	0.21
Asphalt roll roofing		70	—	0.36	0.15
Asphalt shingles		70	—	0.30	0.44
Built-in roofing	3/8 in.	70	—	0.35	0.33
Slate	1/2 in.	—	—	0.30	0.05
Wood shingles (plain and plastic film faced)		—	—	0.31	0.94
<b>Plastering Materials</b>					
Cement plaster, sand aggregate	3/4 in.	1.16	5.0	0.20	0.15
Gypsum plaster					
Lightweight aggregate	1/2 in.	45	—	—	0.32
Sand aggregate	1/2 in.	105	5.6	0.20	0.09
Perlite aggregate	—	45	1.5	0.32	—
<b>Siding Material (on flat surfaces)</b>					
Asbestos-cement shingles	—	120	—	—	0.21
Hardboard siding	7/16 in.	—	—	0.28	0.67
Wood (drop) siding	1 in.	—	—	0.31	0.79
Wood (plywood) siding, lapped	3/8 in.	—	—	0.29	0.59
Aluminum or steel siding (over sheeting):					
Hollow backed	3/8 in.	—	—	0.29	0.61
Insulating-board backed	3/8 in.	—	—	0.32	1.82
Architectural glass	—	158	6.9	0.21	0.10
<b>Woods</b>					
Hardwoods (maple, oak, etc.)	—	45	1.10	0.30	—
Softwoods (fir, pine, etc.)	—	32	0.80	0.33	—
<b>Metals</b>					
Aluminum (1100)	—	171	1536	0.214	—
Steel, mild	—	489	314	0.120	—
Steel, stainless	—	494	108	0.109	—

Source: Tables A-5E and A-6E are adapted from ASHRAE, *Handbook of Fundamentals* (Atlanta, GA: American Society of Heating, Refrigerating, and Air-Conditioning Engineers, 1993), Chap. 22, Table 4. Used with permission.

TABLE A-6E

Properties of insulating materials  
(at a mean temperature of 75°F)

Material	Thickness, <i>L</i> in	Density, $\rho$ lbm/ft <sup>3</sup>	Thermal Conductivity, $k$ Btu·in/h·ft <sup>2</sup> ·°F	Specific Heat, $c_p$ Btu/lbm·R	<i>R</i> -value (for listed thickness, $L/k$ ) °F·h·ft <sup>2</sup> /Btu
<b>Blanket and Batt</b>					
Mineral fiber (fibrous form	~ 2 to 2¾ in	0.3–2.0	—	0.17–0.23	7
processed from rock, slag,	~ 3 to 3½ in	0.3–2.0	—	0.17–0.23	11
or glass)	~ 5¼ to 6½ in	0.3–2.0	—	0.17–0.23	19
<b>Board and Slab</b>					
Cellular glass		8.5	0.38	0.24	—
Glass fiber (organic bonded)		4–9	0.25	0.23	—
Expanded polystyrene (molded beads)		1.0	0.28	0.29	—
Expanded polyurethane ( <i>R</i> -11 expanded)		1.5	0.16	0.38	—
Expanded perlite (organic bonded)		1.0	0.36	0.30	—
Expanded rubber (rigid)		4.5	0.22	0.40	—
Mineral fiber with resin binder		15	0.29	0.17	—
Cork		7.5	0.27	0.43	—
<b>Sprayed or Formed in Place</b>					
Polyurethane foam		1.5–2.5	0.16–0.18	—	—
Glass fiber		3.5–4.5	0.26–0.27	—	—
Urethane, two-part mixture (rigid foam)		4.4	0.18	0.25	—
Mineral wool granules with asbestos/inorganic binders (sprayed)		12	0.32	—	—
<b>Loose Fill</b>					
Mineral fiber (rock, slag, or glass)	~ 3.75 to 5 in	0.6–0.20	—	0.17	11
	~ 6.5 to 8.75 in	0.6–0.20	—	0.17	19
	~ 7.5 to 10 in	—	—	0.17	22
	~ 7.25 in	—	—	0.17	30
Silica aerogel		7.6	0.17	—	—
Vermiculite (expanded)		7–8	0.47	—	—
Perlite, expanded		2–4.1	0.27–0.31	—	—
Sawdust or shavings		8–15	0.45	—	—
Cellulosic insulation (milled paper or wood pulp)		0.3–3.2	0.27–0.32	—	—
Cork, granulated		10	0.31	—	—
<b>Roof Insulation</b>					
Cellular glass	—	9	0.4	0.24	—
Preformed, for use above deck	½ in	—	—	0.24	1.39
	1 in	—	—	0.50	2.78
	2 in	—	—	0.94	5.56
<b>Reflective Insulation</b>					
Silica powder (evacuated)		10	0.0118	—	—
Aluminum foil separating fluffy glass mats; 10–12 layers (evacuated); for cryogenic applications (270 R)		2.5	0.0011	—	—
Aluminum foil and glass paper laminate; 75–150 layers (evacuated); for cryogenic applications (270 R)		7.5	0.00012	—	—

**TABLE A-7E**

Properties of common foods

(a) Specific heats and freezing-point properties

Food	Water Content, <sup>a</sup> % (mass)	Freezing Point, <sup>a</sup> °F	Specific Heat, <sup>b</sup> Btu/lbm·°F		Latent Heat of Fusion <sup>c</sup> Btu/lbm	Food	Water Content, <sup>a</sup> % (mass)	Freezing Point, <sup>a</sup> °F	Specific Heat, <sup>b</sup> Btu/lbm·°F		Latent Heat of Fusion <sup>c</sup> Btu/lbm
			Above Freezing	Below Freezing					Above Freezing	Below Freezing	
<b>Vegetables</b>											
Artichokes	84	30	0.873	0.453	121	Pears	83	29	0.865	0.450	119
Asparagus	93	31	0.945	0.481	134	Pineapples	85	30	0.881	0.456	122
Beans, snap	89	31	0.913	0.468	128	Plums	86	31	0.889	0.459	124
Broccoli	90	30	0.921	0.471	129	Quinces	85	28	0.881	0.456	122
Cabbage	92	30	0.937	0.478	132	Raisins	18	—	—	0.255	26
Carrots	88	29	0.905	0.465	126	Strawberries	90	31	0.921	0.471	129
Cauliflower	92	31	0.937	0.478	132	Tangerines	87	30	0.897	0.462	125
Celery	94	31	0.953	0.484	135	Watermelon	93	31	0.945	0.481	134
Corn, sweet	74	31	0.793	0.423	106	<b>Fish/Seafood</b>					
Cucumbers	96	31	0.969	0.490	138	Cod, whole	78	28	0.825	0.435	112
Eggplant	93	31	0.945	0.481	134	Halibut, whole	75	28	0.801	0.426	108
Horseradish	75	29	0.801	0.426	108	Lobster	79	28	0.833	0.438	113
Leeks	85	31	0.881	0.456	122	Mackerel	57	28	0.657	0.372	82
Lettuce	95	32	0.961	0.487	136	Salmon, whole	64	28	0.713	0.393	92
Mushrooms	91	30	0.929	0.474	131	Shrimp	83	28	0.865	0.450	119
Okra	90	29	0.921	0.471	129	<b>Meats</b>					
Onions, green	89	30	0.913	0.468	128	Beef carcass	49	29	0.593	0.348	70
Onions, dry	88	31	0.905	0.465	126	Liver	70	29	0.761	0.411	101
Parsley	85	30	0.881	0.456	122	Round, beef	67	—	0.737	0.402	96
Peas, green	74	31	0.793	0.423	106	Sirloin, beef	56	—	0.649	0.369	80
Peppers, sweet	92	31	0.937	0.478	132	Chicken	74	27	0.793	0.423	106
Potatoes	78	31	0.825	0.435	112	Lamb leg	65	—	0.721	0.396	93
Pumpkins	91	31	0.929	0.474	131	Pork carcass	37	—	0.497	0.312	53
Spinach	93	31	0.945	0.481	134	Ham	56	29	0.649	0.369	80
Tomatoes, ripe	94	31	0.953	0.484	135	Pork sausage	38	—	0.505	0.315	55
Tumips	92	30	0.937	0.478	132	Turkey	64	—	0.713	0.393	92
<b>Fruits</b>						<b>Other</b>					
Apples	84	30	0.873	0.453	121	Almonds	5	—	—	0.216	7
Apricots	85	30	0.881	0.456	122	Butter	16	—	—	0.249	23
Avocados	65	31	0.721	0.396	93	Cheese, cheddar	37	9	0.497	0.312	53
Bananas	75	31	0.801	0.426	108	Cheese, Swiss	39	14	0.513	0.318	56
Blueberries	82	29	0.857	0.447	118	Chocolate, milk	1	—	—	0.204	1
Cantaloupes	92	30	0.937	0.478	132	Eggs, whole	74	31	0.793	0.423	106
Cherries, sour	84	29	0.873	0.453	121	Honey	17	—	—	0.252	24
Cherries, sweet	80	29	0.841	0.441	115	Ice cream	63	22	0.705	0.390	90
Figs, dried	23	—	—	0.270	33	Milk, whole	88	31	0.905	0.465	126
Figs, fresh	78	28	0.825	0.435	112	Peanuts	6	—	—	0.219	9
Grapefruit	89	30	0.913	0.468	128	Peanuts, roasted	2	—	—	0.207	3
Grapes	82	29	0.857	0.447	118	Pecans	3	—	—	0.210	4
Lemons	89	29	0.913	0.468	128	Walnuts	4	—	—	0.213	6
Olives	75	29	0.801	0.426	108						
Oranges	87	31	0.897	0.462	125						
Peaches	89	30	0.913	0.468	128						

Source: <sup>a</sup>Water content and freezing point data are from ASHRAE, *Handbook of Fundamentals*, I-P version (Atlanta, GA: American Society of Heating, Refrigerating, and Air-Conditioning Engineers, Inc., 1993), Chap. 30, Table 1. Used with permission.

<sup>b</sup>Specific heat data are based on the specific heat values of water and ice at 32°F and are determined from Siebel's formulas:  $c_{p, \text{frozen}} = 0.300 \times (\text{Water content}) + 0.200$ , below freezing, and  $c_{p, \text{frozen}} = 0.800 \times (\text{Water content}) + 0.200$ , above freezing, and

<sup>c</sup>The latent heat of fusion is determined by multiplying the heat of fusion of water (143 Btu/lbm) by the water content of the food.

TABLE A-7E

Properties of common foods (Concluded)

(b) Other properties

Food	Water Content, % (mass)	Temperature, $T$ °F	Density, $\rho$ lbm/ft <sup>3</sup>	Thermal Conductivity, $k$ Btu/h·ft·°F	Thermal Diffusivity, $\alpha$ ft <sup>2</sup> /s	Specific Heat, $c_p$ Btu/lbm·R
<b>Fruits/Vegetables</b>						
Apple juice	87	68	62.4	0.323	$1.51 \times 10^{-6}$	0.922
Apples	85	32–86	52.4	0.242	$1.47 \times 10^{-6}$	0.910
Apples, dried	41.6	73	53.4	0.127	$1.03 \times 10^{-6}$	0.650
Apricots, dried	43.6	73	82.4	0.217	$1.22 \times 10^{-6}$	0.662
Bananas, fresh	76	41	61.2	0.278	$1.51 \times 10^{-6}$	0.856
Broccoli	—	21	35.0	0.223	—	—
Cherries, fresh	92	32–86	65.5	0.315	$1.42 \times 10^{-6}$	0.952
Figs	40.4	73	77.5	0.179	$1.03 \times 10^{-6}$	0.642
Grape juice	89	68	62.4	0.328	$1.51 \times 10^{-6}$	0.934
Peaches	36–90	2–32	59.9	0.304	$1.51 \times 10^{-6}$	0.934
Plums	—	3	38.1	0.143	—	—
Potatoes	32–158	0–70	65.7	0.288	$1.40 \times 10^{-6}$	0.868
Raisins	32	73	86.2	0.217	$1.18 \times 10^{-6}$	0.592
<b>Meats</b>						
Beef, ground	67	43	59.3	0.235	$1.40 \times 10^{-6}$	0.802
Beef, lean	74	37	68.0	0.272	$1.40 \times 10^{-6}$	0.844
Beef fat	0	95	50.5	0.110	—	—
Beef liver	72	95	—	0.259	—	0.832
Cat food	39.7	73	71.2	0.188	$1.18 \times 10^{-6}$	0.638
Chicken breast	75	32	65.5	0.275	$1.40 \times 10^{-6}$	0.850
Dog food	30.6	73	77.4	0.184	$1.18 \times 10^{-6}$	0.584
Fish, cod	81	37	73.7	0.309	$1.29 \times 10^{-6}$	0.886
Fish, salmon	67	37	—	0.307	—	0.802
Ham	71.8	72	64.3	0.277	$1.51 \times 10^{-6}$	0.831
Lamb	72	72	64.3	0.263	$1.40 \times 10^{-6}$	0.832
Pork, lean	72	39	64.3	0.263	$1.40 \times 10^{-6}$	0.832
Turkey breast	74	37	65.5	0.287	$1.40 \times 10^{-6}$	0.844
Veal	75	72	66.2	0.272	$1.40 \times 10^{-6}$	0.850
<b>Other</b>						
Butter	16	39	—	0.114	—	0.496
Chocolate cake	31.9	73	21.2	0.061	$1.29 \times 10^{-6}$	0.591
Margarine	16	40	62.4	0.135	$1.18 \times 10^{-6}$	0.496
Milk, skimmed	91	72	—	0.327	—	0.946
Milk, whole	88	82	—	0.335	—	0.928
Olive oil	0	90	56.8	0.097	—	—
Peanut oil	0	39	57.4	0.097	—	—
Water	100	0	62.4	0.329	$1.51 \times 10^{-6}$	1.000
	100	30	59.6	0.357	$1.61 \times 10^{-6}$	1.000
White cake	32.3	73	28.1	0.047	$1.08 \times 10^{-6}$	0.594

Source: Data obtained primarily from ASHRAE, *Handbook of Fundamentals*, I-P version (Atlanta, GA: American Society of Heating, Refrigerating, and Air-Conditioning Engineers, Inc., 1993), Chap. 30, Tables 7 and 9. Used with permission.

Most specific heats are calculated from  $c_p = 0.4 + 0.6 \times (\text{Water content})$ , which is a good approximation in the temperature range of 40 to 90°F. Most thermal diffusivities are calculated from  $\alpha = k/\rho c_p$ . Property values given above are valid for the specified water content.

TABLE A-8E

Properties of miscellaneous materials

(values are at 540 R unless indicated otherwise)

Material	Density, $\rho$ lbm/ft <sup>3</sup>	Thermal Conductivity, $k$ Btu/h-ft-R	Specific Heat, $c_p$ Btu/lbm-R	Material	Density, $\rho$ lbm/ft <sup>3</sup>	Thermal Conductivity, $k$ Btu/h-ft-R	Specific Heat, $c_p$ Btu/lbm-R
Asphalt	132.0	0.036	0.220	Ice			
Bakelite	81.2	0.81	0.350	492 R	57.4	1.09	0.487
Brick, refractory				455 R	57.6	1.17	0.465
Chrome brick				311 R	57.9	2.02	0.349
851 R	187.9	1.33	0.199	Leather, sole	62.3	0.092	—
1481 R	—	1.44	—	Linoleum	33.4	0.047	—
2111 R	—	1.16	—		73.7	0.11	—
Fire clay, burnt 2880 R				Mica	181.0	0.30	—
1391 R	128.0	0.58	0.229	Paper	58.1	0.10	0.320
1931 R	—	0.64	—	Plastics			
2471 R	—	0.64	—	Plexiglass	74.3	0.11	0.350
Fire clay, burnt 3105 R				Teflon			
1391 R	145.1	0.75	0.229	540 R	137.3	0.20	0.251
1931 R	—	0.81	—	720 R	—	0.26	—
2471 R	—	0.81	—	Lexan	74.9	0.11	0.301
Fire clay brick				Nylon	71.5	0.17	—
860 R	165.1	0.58	0.229	Polypropylene	56.8	0.069	0.388
1660 R	—	0.87	—	Polyester	87.1	0.087	0.279
2660 R	—	1.04	—	PVC, vinyl	91.8	0.058	0.201
Magnesite				Porcelain	143.6	0.87	—
860 R	—	2.20	0.270	Rubber, natural	71.8	0.16	—
1660 R	—	1.62	—	Rubber, vulcanized			
2660 R	—	1.10	—	Soft	68.7	0.075	0.480
Chicken meat, white (74.4% water content)				Hard	74.3	0.092	—
356 R	—	0.92	—	Sand	94.6	0.1–0.6	0.191
419 R	—	0.86	—	Snow, fresh	6.24	0.35	—
455 R	—	0.78	—	Snow 492 R	31.2	1.27	—
492 R	—	0.28	—	Soil, dry	93.6	0.58	0.454
527 R	—	0.28	—	Soil, wet	118.6	1.16	0.525
Clay, dry	96.8	0.54	—	Sugar	99.9	0.34	—
Clay, wet	93.3	0.97	—	Tissue, human			
Coal, anthracite	84.3	0.15	0.301	Skin	—	0.21	—
Concrete (stone mix)	143.6	0.81	0.210	Fat layer	—	0.12	—
Cork	5.37	0.028	0.485	Muscle	—	0.24	—
Cotton	5.0	0.035	0.311	Vaseline	—	0.098	—
Fat	—	0.10	—	Wood, cross-grain			
Glass				Balsa	8.74	0.032	—
Window	174.8	0.40	0.179	Fir	25.9	0.064	0.650
Pyrex	138.9	0.6–0.8	0.199	Oak	34.0	0.098	0.570
Crown	156.1	0.61	—	White pine	27.2	0.064	—
Lead	212.2	0.49	—	Yellow pine	40.0	0.087	0.670
				Wood, radial			
				Oak	34.0	0.11	0.570
				Fir	26.2	0.081	0.650
				Wool, ship	9.05	0.029	—



TABLE A-9E

## Properties of saturated water

Temp. <i>T</i> , F°	Saturation Pressure <i>P</i> <sub>sat</sub> , psia	Density $\rho$ , lbm/ft <sup>3</sup>		Enthalpy of Vaporization <i>h</i> <sub>fg</sub> , Btu/lbm	Specific Heat <i>c</i> <sub>p</sub> , Btu/lbm-R		Thermal Conductivity <i>k</i> , Btu/h-ft-R		Dynamic Viscosity $\mu$ , lbm/ft-s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/R
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	
32.02	0.0887	62.41	0.00030	1075	1.010	0.446	0.324	0.0099	$1.204 \times 10^{-3}$	$6.194 \times 10^{-6}$	13.5	1.00	$-0.038 \times 10^{-3}$
40	0.1217	62.42	0.00034	1071	1.004	0.447	0.329	0.0100	$1.308 \times 10^{-3}$	$6.278 \times 10^{-6}$	11.4	1.01	$A0.003 \times 10^{-3}$
50	0.1780	62.41	0.00059	1065	1.000	0.448	0.335	0.0102	$8.781 \times 10^{-4}$	$6.361 \times 10^{-6}$	9.44	1.01	$0.047 \times 10^{-3}$
60	0.2563	62.36	0.00083	1060	0.999	0.449	0.341	0.0104	$7.536 \times 10^{-4}$	$6.444 \times 10^{-6}$	7.95	1.00	$0.080 \times 10^{-3}$
70	0.3632	62.30	0.00115	1054	0.999	0.450	0.347	0.0106	$6.556 \times 10^{-4}$	$6.556 \times 10^{-6}$	6.79	1.00	$0.115 \times 10^{-3}$
80	0.5073	62.22	0.00158	1048	0.999	0.451	0.352	0.0108	$5.764 \times 10^{-4}$	$6.667 \times 10^{-6}$	5.89	1.00	$0.145 \times 10^{-3}$
90	0.6988	62.12	0.00214	1043	0.999	0.453	0.358	0.0110	$5.117 \times 10^{-4}$	$6.778 \times 10^{-6}$	5.14	1.00	$0.174 \times 10^{-3}$
100	0.9503	62.00	0.00286	1037	0.999	0.454	0.363	0.0112	$4.578 \times 10^{-4}$	$6.889 \times 10^{-6}$	4.54	1.01	$0.200 \times 10^{-3}$
110	1.2763	61.86	0.00377	1031	0.999	0.456	0.367	0.0115	$4.128 \times 10^{-4}$	$7.000 \times 10^{-6}$	4.05	1.00	$0.224 \times 10^{-3}$
120	1.6945	61.71	0.00493	1026	0.999	0.458	0.371	0.0117	$3.744 \times 10^{-4}$	$7.111 \times 10^{-6}$	3.63	1.00	$0.246 \times 10^{-3}$
130	2.225	61.55	0.00636	1020	0.999	0.460	0.375	0.0120	$3.417 \times 10^{-4}$	$7.222 \times 10^{-6}$	3.28	1.00	$0.267 \times 10^{-3}$
140	2.892	61.38	0.00814	1014	0.999	0.463	0.378	0.0122	$3.136 \times 10^{-4}$	$7.333 \times 10^{-6}$	2.98	1.00	$0.287 \times 10^{-3}$
150	3.722	61.19	0.0103	1008	1.000	0.465	0.381	0.0125	$2.889 \times 10^{-4}$	$7.472 \times 10^{-6}$	2.73	1.00	$0.306 \times 10^{-3}$
160	4.745	60.99	0.0129	1002	1.000	0.468	0.384	0.0128	$2.675 \times 10^{-4}$	$7.583 \times 10^{-6}$	2.51	1.00	$0.325 \times 10^{-3}$
170	5.996	60.79	0.0161	996	1.001	0.472	0.386	0.0131	$2.483 \times 10^{-4}$	$7.722 \times 10^{-6}$	2.90	1.00	$0.346 \times 10^{-3}$
180	7.515	60.57	0.0199	990	1.002	0.475	0.388	0.0134	$2.317 \times 10^{-4}$	$7.833 \times 10^{-6}$	2.15	1.00	$0.367 \times 10^{-3}$
190	9.343	60.35	0.0244	984	1.004	0.479	0.390	0.0137	$2.169 \times 10^{-4}$	$7.972 \times 10^{-6}$	2.01	1.00	$0.382 \times 10^{-3}$
200	11.53	60.12	0.0297	978	1.005	0.483	0.391	0.0141	$2.036 \times 10^{-4}$	$8.083 \times 10^{-6}$	1.88	1.00	$0.395 \times 10^{-3}$
210	14.125	59.87	0.0359	972	1.007	0.487	0.392	0.0144	$1.917 \times 10^{-4}$	$8.222 \times 10^{-6}$	1.77	1.00	$0.412 \times 10^{-3}$
212	14.698	59.82	0.0373	970	1.007	0.488	0.392	0.0145	$1.894 \times 10^{-4}$	$8.250 \times 10^{-6}$	1.75	1.00	$0.417 \times 10^{-3}$
220	17.19	59.62	0.0432	965	1.009	0.492	0.393	0.0148	$1808 \times 10^{-4}$	$8.333 \times 10^{-6}$	1.67	1.00	$0.429 \times 10^{-3}$
230	20.78	59.36	0.0516	959	1.011	0.497	0.394	0.0152	$1.711 \times 10^{-4}$	$8.472 \times 10^{-6}$	1.58	1.00	$0.443 \times 10^{-3}$
240	24.97	59.09	0.0612	952	1.013	0.503	0.394	0.0156	$1.625 \times 10^{-4}$	$8.611 \times 10^{-6}$	1.50	1.00	$0.462 \times 10^{-3}$
250	29.82	58.82	0.0723	946	1.015	0.509	0.395	0.0160	$1.544 \times 10^{-4}$	$8.611 \times 10^{-6}$	1.43	1.00	$0.480 \times 10^{-3}$
260	35.42	58.53	0.0850	939	1.018	0.516	0.395	0.0164	$1.472 \times 10^{-4}$	$8.861 \times 10^{-6}$	1.37	1.00	$0.497 \times 10^{-3}$
270	41.85	58.24	0.0993	932	1.020	0.523	0.395	0.0168	$1.406 \times 10^{-4}$	$9.000 \times 10^{-6}$	1.31	1.01	$0.514 \times 10^{-3}$
280	49.18	57.94	0.1156	926	1.023	0.530	0.395	0.0172	$1.344 \times 10^{-4}$	$9.111 \times 10^{-6}$	1.25	1.01	$0.532 \times 10^{-3}$
290	57-53	57.63	0.3390	918	1.026	0.538	0.395	0.0177	$1.289 \times 10^{-4}$	$9.250 \times 10^{-6}$	1.21	1.01	$0.549 \times 10^{-3}$
300	66.98	57.31	0.1545	910	1.029	0.547	0.394	0.0182	$1.236 \times 10^{-4}$	$9.389 \times 10^{-6}$	1.16	1.02	$0.566 \times 10^{-3}$
320	89.60	56.65	0.2033	895	1.036	0.567	0.393	0.0191	$1.144 \times 10^{-4}$	$9.639 \times 10^{-6}$	1.09	1.03	$0.636 \times 10^{-3}$
340	117.93	55.95	0.2637	880	1.044	0.590	0.391	0.0202	$1.063 \times 10^{-4}$	$9.889 \times 10^{-6}$	1.02	1.04	$0.656 \times 10^{-3}$
360	152.92	56.22	0.3377	863	1.054	0.617	0.389	0.0213	$9.972 \times 10^{-5}$	$1.013 \times 10^{-5}$	0.973	1.06	$0.681 \times 10^{-3}$
380	195.60	54.46	0.4275	845	1.065	0.647	0.385	0.0224	$9.361 \times 10^{-5}$	$1.041 \times 10^{-5}$	0.932	1.08	$0.720 \times 10^{-3}$
400	241.1	53.65	0.5359	827	1.078	0.683	0.382	0.0237	$8.833 \times 10^{-5}$	$1.066 \times 10^{-5}$	0.893	1.11	$0.771 \times 10^{-3}$
450	422.1	51.46	0.9082	775	1.121	0.799	0.370	0.0271	$7.722 \times 10^{-5}$	$1.130 \times 10^{-5}$	0.842	1.20	$0.912 \times 10^{-3}$
500	680.0	48.95	1.479	715	1.188	0.972	0.352	0.0312	$6.833 \times 10^{-5}$	$1.200 \times 10^{-5}$	0.830	1.35	$1.111 \times 10^{-3}$
550	1046.7	45.96	4.268	641	1.298	1.247	0.329	0.0368	$6.083 \times 10^{-5}$	$1.280 \times 10^{-5}$	0.864	1.56	$1.445 \times 10^{-3}$
600	1541	42.32	3.736	550	1.509	1.759	0.299	0.0461	$5.389 \times 10^{-5}$	$1.380 \times 10^{-5}$	0.979	1.90	$1.883 \times 10^{-3}$
650	2210	37.31	6.152	422	2.086	3.103	0.267	0.0677	$4.639 \times 10^{-5}$	$1.542 \times 10^{-5}$	1.30	2.54	
700	3090	27.28	13.44	168	13.80	25.90	0.254	0.1964	$3.417 \times 10^{-5}$	$2.044 \times 10^{-5}$	6.68	9.71	
705.44	3204	19.79	19.79	0	$\infty$	$\infty$	$\infty$	$\infty$	$2.897 \times 10^{-5}$	$2.897 \times 10^{-5}$			

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/\text{Pr}$ . The temperatures 32.02°F, 212°F, and 705.44°F are the triple-, boiling-, and critical-point temperatures of water, respectively. All properties listed above (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit Btu/lbm-°F for specific heat is equivalent to Btu/lbm-R, and the unit Btu/h-ft-°F for thermal conductivity is equivalent to Btu/h-ft-R.

Source: Viscosity and thermal conductivity data are from J. V. Sengers and J. T. T. Watson, *Journal of Physical and Chemical Reference Data* 15 (1986), pp. 1291–1322. Other data are obtained from various sources or calculated.

TABLE A-10E

Properties of saturated refrigerant-134a

Temp. <i>T</i> , F°	Saturation Pressure <i>P</i> <sub>sat</sub> , psia	Density $\rho$ , lbm/ft <sup>3</sup>		Enthalpy of Vaporization <i>h</i> <sub>fg</sub> , Btu/lbm	Specific Heat <i>c</i> <sub>p</sub> , Btu/lbm·R		Thermal Conductivity <i>k</i> , Btu/h·ft·R		Dynamic Viscosity $\mu$ , lbm/ft·s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/R	Surface Tension lbf/ft
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-40	7.4	88.51	0.1731	97.1	0.2996	0.1788	0.0636	0.00466	3.278 × 10 <sup>-4</sup>	1.714 × 10 <sup>-6</sup>	5.558	0.237	0.00114	0.001206
-30	9.9	87.5	0.2258	95.6	0.3021	0.1829	0.0626	0.00497	3.004 × 10 <sup>-4</sup>	2.053 × 10 <sup>-6</sup>	5.226	0.272	0.00117	0.001146
-20	12.9	86.48	0.2905	94.1	0.3046	0.1872	0.0613	0.00529	2.762 × 10 <sup>-4</sup>	2.433 × 10 <sup>-6</sup>	4.937	0.310	0.00120	0.001087
-10	16.6	85.44	0.3691	92.5	0.3074	0.1918	0.0602	0.00559	2.546 × 10 <sup>-4</sup>	2.856 × 10 <sup>-6</sup>	4.684	0.352	0.00124	0.001029
0	21.2	84.38	0.4635	90.9	0.3103	0.1966	0.0589	0.00589	2.345 × 10 <sup>-4</sup>	3.314 × 10 <sup>-6</sup>	4.463	0.398	0.00128	0.000972
10	26.6	83.31	0.5761	89.3	0.3134	0.2017	0.0576	0.00619	2.181 × 10 <sup>-4</sup>	3.811 × 10 <sup>-6</sup>	4.269	0.447	0.00132	0.000915
20	33.1	82.2	0.7094	87.5	0.3167	0.2070	0.0563	0.00648	2.024 × 10 <sup>-4</sup>	4.342 × 10 <sup>-6</sup>	4.098	0.500	0.00132	0.000859
30	40.8	81.08	0.866	85.8	0.3203	0.2127	0.0550	0.00676	1.883 × 10 <sup>-4</sup>	4.906 × 10 <sup>-6</sup>	3.947	0.555	0.00142	0.000803
40	49.8	79.92	1.049	83.9	0.3240	0.2188	0.0536	0.00704	1.752 × 10 <sup>-4</sup>	5.494 × 10 <sup>-6</sup>	3.814	0.614	0.00149	0.000749
50	60.2	78.73	1.262	82.0	0.3281	0.2253	0.0522	0.00732	1.633 × 10 <sup>-4</sup>	6.103 × 10 <sup>-6</sup>	3.697	0.677	0.00156	0.000695
60	72.2	77.51	1.509	80.0	0.3325	0.2323	0.0507	0.00758	1.522 × 10 <sup>-4</sup>	6.725 × 10 <sup>-6</sup>	3.594	0.742	0.00163	0.000642
70	85.9	76.25	1.794	78.0	0.3372	0.2398	0.0492	0.00785	1.420 × 10 <sup>-4</sup>	7.356 × 10 <sup>-6</sup>	3.504	0.810	0.00173	0.000590
80	101.4	74.94	2.122	75.8	0.3424	0.2481	0.0476	0.00810	1.324 × 10 <sup>-4</sup>	7.986 × 10 <sup>-6</sup>	3.425	0.880	0.00183	0.000538
90	119.1	73.59	2.5	73.5	0.3481	0.2572	0.0460	0.00835	1.234 × 10 <sup>-4</sup>	8.611 × 10 <sup>-6</sup>	3.357	0.955	0.00195	0.000488
100	138.9	72.17	2.935	71.1	0.3548	0.2674	0.0444	0.00860	1.149 × 10 <sup>-4</sup>	9.222 × 10 <sup>-6</sup>	3.303	1.032	0.00210	0.000439
110	161.2	70.69	3.435	68.5	0.3627	0.2790	0.0427	0.00884	1.068 × 10 <sup>-4</sup>	9.814 × 10 <sup>-6</sup>	3.262	1.115	0.00227	0.000391
120	186.0	69.13	4.012	65.8	0.3719	0.2925	0.0410	0.00908	9.911 × 10 <sup>-5</sup>	1.038 × 10 <sup>-5</sup>	3.235	1.204	0.00248	0.000344
130	213.5	67.48	4.679	62.9	0.3829	0.3083	0.0392	0.00931	9.175 × 10 <sup>-5</sup>	1.092 × 10 <sup>-5</sup>	3.223	1.303	0.00275	0.000299
140	244.1	65.72	5.455	59.8	0.3963	0.3276	0.0374	0.00954	8.464 × 10 <sup>-5</sup>	1.144 × 10 <sup>-5</sup>	3.229	1.416	0.00308	0.000255
150	277.8	63.83	6.367	56.4	0.4131	0.3520	0.0355	0.00976	7.778 × 10 <sup>-5</sup>	1.195 × 10 <sup>-5</sup>	3.259	1.551	0.00351	0.000212
160	314.9	61.76	7.45	52.7	0.4352	0.3839	0.0335	0.00998	7.108 × 10 <sup>-5</sup>	1.245 × 10 <sup>-5</sup>	3.324	1.725	0.00411	0.000171
170	355.8	59.47	8.762	48.5	0.4659	0.4286	0.0314	0.01020	6.450 × 10 <sup>-5</sup>	1.298 × 10 <sup>-5</sup>	3.443	1.963	0.00498	0.000132
180	400.7	56.85	10.4	43.7	0.5123	0.4960	0.0292	0.01041	5.792 × 10 <sup>-5</sup>	1.366 × 10 <sup>-5</sup>	3.661	2.327	0.00637	0.000095
190	449.9	53.75	12.53	38.0	0.5929	0.6112	0.0267	0.01063	5.119 × 10 <sup>-5</sup>	1.431 × 10 <sup>-5</sup>	4.090	2.964	0.00891	0.000061
200	504.0	49.75	15.57	30.7	0.7717	0.8544	0.0239	0.01085	4.397 × 10 <sup>-5</sup>	1.544 × 10 <sup>-5</sup>	5.119	4.376	0.01490	0.000031
210	563.8	43.19	21.18	18.9	1.4786	1.6683	0.0199	0.01110	3.483 × 10 <sup>-5</sup>	1.787 × 10 <sup>-5</sup>	9.311	9.669	0.04021	0.000006

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/Pr$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit Btu/lbm·°F for specific heat is equivalent to Btu/lbm·R, and the unit Btu/h·ft·°F for thermal conductivity is equivalent to Btu/h·ft·R.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: R. Tilner-Roth and H. D. Baehr, "An International Standard Formulation for the Thermodynamic Properties of 1,1,1,2-Tetrafluoroethane (HFC-134a) for Temperatures from 170 K to 455 K and Pressures up to 70 Mpa," *J. Phys. Chem. Ref. Data*, Vol. 23, No.5, 1994; M. J. Assael, N. K. Dalaouti, A. A. Griva, and J. H. Dymond, "Viscosity and Thermal Conductivity of Halogenated Methane and Ethane Refrigerants," *IJR*, Vol. 22, pp. 525-535, 1999; NIST REPROP 6 program (M. O. McLinden, S. A. Klein, E. W. Lemmon, and A. P. Peskin, Physical and Chemical Properties Division, National Institute of Standards and Technology, Boulder, CO 80303, 1995).

**TABLE A-11E**

Properties of saturated ammonia

Temp. <i>T</i> , F°	Saturation Pressure <i>P</i> <sub>sat</sub> , psia	Density $\rho$ , lbm/ft <sup>3</sup>		Enthalpy of Vaporization <i>h</i> <sub>fg</sub> , Btu/lbm	Specific Heat <i>c</i> <sub>p</sub> , Btu/lbm-R		Thermal Conductivity <i>k</i> , Btu/h-ft-R		Dynamic Viscosity $\mu$ , lbm/ft-s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/R	Surface Tension lbf/ft
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-40	10.4	43.08	0.0402	597.0	1.0542	0.5354	-	0.01026	1.966 × 10 <sup>-4</sup>	5.342 × 10 <sup>-6</sup>	-	1.003	0.00098	0.002443
-30	13.9	42.66	0.0527	590.2	1.0610	0.5457	-	0.01057	1.853 × 10 <sup>-4</sup>	5.472 × 10 <sup>-6</sup>	-	1.017	0.00101	0.002357
-20	18.3	42.33	0.0681	583.2	1.0677	0.5571	0.3501	0.01089	1.746 × 10 <sup>-4</sup>	5.600 × 10 <sup>-6</sup>	1.917	1.031	0.00103	0.002272
-10	23.7	41.79	0.0869	575.9	1.0742	0.5698	0.3426	0.01121	1.645 × 10 <sup>-4</sup>	5.731 × 10 <sup>-6</sup>	1.856	1.048	0.00106	0.002187
0	30-4	41.34	0.1097	568.4	1.0807	0.5838	0.3352	0.01154	1.549 × 10 <sup>-4</sup>	5.861 × 10 <sup>-6</sup>	1.797	1.068	0.00109	0.002103
10	38.5	40.89	0.1370	560.7	1.0873	0.5992	0.3278	0.01187	1.458 × 10 <sup>-4</sup>	5.994 × 10 <sup>-6</sup>	1.740	1.089	0.00112	0.002018
20	48.2	40.43	0.1694	552.6	1.0941	0.6160	0.3203	0.01220	1.371 × 10 <sup>-4</sup>	6.125 × 10 <sup>-6</sup>	1.686	1.113	0.00116	0.001934
30	59.8	39.96	0.2075	544.4	1.1012	0.6344	0.3129	0.01254	1.290 × 10 <sup>-4</sup>	6.256 × 10 <sup>-6</sup>	1.634	1.140	0.00119	0.001850
40	73.4	39.48	0.2521	535.8	1.1087	0.6544	0.3055	0.01288	1.213 × 10 <sup>-4</sup>	6.389 × 10 <sup>-6</sup>	1.585	1.168	0.00123	0.001767
50	89.2	38.99	0.3040	526.9	1.1168	0.6762	0.2980	0.01323	1.140 × 10 <sup>-4</sup>	6.522 × 10 <sup>-6</sup>	1.539	1.200	0.00128	0.001684
60	107.7	38.50	0.3641	517.7	1.1256	0.6999	0.2906	0.01358	1.072 × 10 <sup>-4</sup>	6.656 × 10 <sup>-6</sup>	1.495	1.234	0.00132	0.001601
70	128.9	37.99	0.4332	508.1	1.1353	0.7257	0.2832	0.01394	1.008 × 10 <sup>-4</sup>	6.786 × 10 <sup>-6</sup>	1.456	1.272	0.00137	0.001518
80	153.2	37.47	0.5124	498.2	1.1461	0.7539	0.2757	0.01431	9.486 × 10 <sup>-5</sup>	6.922 × 10 <sup>-6</sup>	1.419	1.313	0.00143	0.001436
90	180.8	36.94	0.6029	487.8	1.1582	0.7846	0.2683	0.01468	8.922 × 10 <sup>-5</sup>	7.056 × 10 <sup>-6</sup>	1.387	1.358	0.00149	0.001354
100	212.0	36.40	0.7060	477.0	1.1719	0.8183	0.2609	0.01505	8.397 × 10 <sup>-5</sup>	7.189 × 10 <sup>-6</sup>	1.358	1.407	0.00156	0.001273
110	247.2	35.83	0.8233	465.8	1.1875	0.8554	0.2535	0.01543	7.903 × 10 <sup>-5</sup>	7.325 × 10 <sup>-6</sup>	1.333	1.461	0.00164	0.001192
120	286.5	35.26	0.9564	454.1	1.2054	0.8965	0.2460	0.01582	7.444 × 10 <sup>-5</sup>	7.458 × 10 <sup>-6</sup>	1.313	1.522	0.00174	0.001111
130	330.4	34.66	1.1074	441.7	1.2261	0.9425	0.2386	0.01621	7.017 × 10 <sup>-5</sup>	7.594 × 10 <sup>-6</sup>	1.298	1.589	0.00184	0.001031
140	379.4	34.04	1.2786	428.8	1.2502	0.9943	0.2312	0.01661	6.617 × 10 <sup>-5</sup>	7.731 × 10 <sup>-6</sup>	1.288	1.666	0.00196	0.000951
150	433.2	33.39	1.4730	415.2	1.2785	1.0533	0.2237	0.01702	6.244 × 10 <sup>-5</sup>	7.867 × 10 <sup>-6</sup>	1.285	1.753	0.00211	0.000872
160	492.7	32.72	1.6940	400.8	1.3120	1.1214	0.2163	0.01744	5.900 × 10 <sup>-5</sup>	8.006 × 10 <sup>-6</sup>	1.288	1.853	0.00228	0.000794
170	558.2	32.01	1.9460	385.4	1.3523	1.2012	0.2089	0.01786	5.578 × 10 <sup>-5</sup>	8.142 × 10 <sup>-6</sup>	1.300	1.971	0.00249	0.000716
180	630.1	31.26	2.2346	369.1	1.4015	1.2965	0.2014	0.01829	5.278 × 10 <sup>-5</sup>	8.281 × 10 <sup>-6</sup>	1.322	2.113	0.00274	0.000638
190	708.5	30.47	2.5670	351.6	1.4624	1.4128	0.1940	0.01874	5.000 × 10 <sup>-5</sup>	8.419 × 10 <sup>-6</sup>	1.357	2.286	0.00306	0.000562
200	794.4	29.62	2.9527	332.7	1.5397	1.5586	0.1866	0.01919	4.742 × 10 <sup>-5</sup>	8.561 × 10 <sup>-6</sup>	1.409	2.503	0.00348	0.000486
210	887.9	28.70	3.4053	312.0	1.6411	1.7473	0.1791	0.01966	4.500 × 10 <sup>-5</sup>	8.703 × 10 <sup>-6</sup>	1.484	2.784	0.00403	0.000411
220	989.5	27.69	3.9440	289.2	1.7798	2.0022	0.1717	0.02015	4.275 × 10 <sup>-5</sup>	8.844 × 10 <sup>-6</sup>	1.595	3.164	0.00480	0.000338
230	1099.0	25.57	4.5987	263.5	1.9824	2.3659	0.1643	0.02065	4.064 × 10 <sup>-5</sup>	8.989 × 10 <sup>-6</sup>	1.765	3.707	0.00594	0.000265
240	1219.4	25.28	5.4197	234.0	2.3100	2.9264	0.1568	0.02119	3.864 × 10 <sup>-5</sup>	9.136 × 10 <sup>-6</sup>	2.049	4.542	0.00784	0.000194

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/Pr$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error except at temperatures near the critical-point value.

Note 2: The unit Btu/lbm-°F for specific heat is equivalent to Btu/lbm-R, and the unit Btu/lbm-F, for thermal conductivity is equivalent to Btu/h-ft-R.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Tillner-Roth, Harms-Watzenterg, and Baehr, "Eine neue Fundamentalgleichung für Ammoniak," *DKV-Tagungsbericht* 20: 167-181, 1993; Liley and Desai, "Thermophysical Properties of Refrigerants," *ASHRAE*, 1993, ISBN 1-1883413-10-9.

TABLE A-12E

## Properties of saturated propane

Temp. <i>T</i> , F°	Saturation Pressure <i>P</i> <sub>sat</sub> , psia	Density $\rho$ , lbm/ft <sup>3</sup>		Enthalpy of Vaporization <i>h</i> <sub>fg</sub> , Btu/lbm	Specific Heat <i>c</i> <sub>p</sub> , Btu/lbm·R		Thermal Conductivity <i>k</i> , Btu/h·ft·R		Dynamic Viscosity $\mu$ , lbm/ft·s		Prandtl Number Pr		Volume Expansion Coefficient $\beta$ , 1/R	Surface Tension lbf/ft
		Liquid	Vapor		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor		
-200	0.0201	42.06	0.0003	217.7	0.4750	0.2595	0.1073	0.00313	$5.012 \times 10^{-4}$	$2.789 \times 10^{-6}$	7.991	0.833	0.00083	0.001890
-180	0.0752	41.36	0.0011	213.4	0.4793	0.2680	0.1033	0.00347	$3.941 \times 10^{-4}$	$2.975 \times 10^{-6}$	6.582	0.826	0.00086	0.001780
-160	0.2307	40.65	0.0032	209.1	0.4845	0.2769	0.0992	0.00384	$3.199 \times 10^{-4}$	$3.164 \times 10^{-6}$	5.626	0.821	0.00088	0.001671
-140	0.6037	39.93	0.0078	204.8	0.4907	0.2866	0.0949	0.00423	$2.660 \times 10^{-4}$	$3.358 \times 10^{-6}$	4.951	0.818	0.00091	0.001563
-120	1.389	39.20	0.0170	200.5	0.4982	0.2971	0.0906	0.00465	$2.252 \times 10^{-4}$	$3.556 \times 10^{-6}$	4.457	0.817	0.00094	0.001455
-100	2.878	38.46	0.0334	196.1	0.5069	0.3087	0.0863	0.00511	$1.934 \times 10^{-4}$	$3.756 \times 10^{-6}$	4.087	0.817	0.00097	0.001349
-90	4.006	38.08	0.0453	193.9	0.5117	0.3150	0.0842	0.00534	$1.799 \times 10^{-4}$	$3.858 \times 10^{-6}$	3.936	0.819	0.00099	0.001297
-80	5.467	37.70	0.0605	191.6	0.5169	0.3215	0.0821	0.00559	$1.678 \times 10^{-4}$	$3.961 \times 10^{-6}$	3.803	0.820	0.00101	0.001244
-70	7.327	37.32	0.0793	189.3	0.5224	0.3284	0.0800	0.00585	$1.569 \times 10^{-4}$	$4.067 \times 10^{-6}$	3.686	0.822	0.00104	0.001192
-60	9.657	36.93	0.1024	186.9	0.5283	0.3357	0.0780	0.00611	$1.469 \times 10^{-4}$	$4.172 \times 10^{-6}$	3.582	0.825	0.00106	0.001140
-50	12.54	36.54	0.1305	184.4	0.5345	0.3433	0.0760	0.00639	$1.378 \times 10^{-4}$	$4.278 \times 10^{-6}$	3.490	0.828	0.00109	0.001089
-40	16.05	36.13	0.1641	181.9	0.5392	0.3513	0.0740	0.00568	$1.294 \times 10^{-4}$	$4.386 \times 10^{-6}$	3.395	0.831	0.00112	0.001038
-30	20.29	35.73	0.2041	179.3	0.5460	0.3596	0.0721	0.00697	$1.217 \times 10^{-4}$	$4.497 \times 10^{-6}$	3.320	0.835	0.00115	0.000987
-20	25.34	35.31	0.2512	176.6	0.5531	0.3684	0.0702	0.00728	$1.146 \times 10^{-4}$	$4.611 \times 10^{-6}$	3.253	0.840	0.00119	0.000937
-10	31.3	34.89	0.3063	173.8	0.5607	0.3776	0.0683	0.00761	$1.079 \times 10^{-4}$	$4.725 \times 10^{-6}$	3.192	0.845	0.00123	0.000887
0	38.28	34.46	0.3703	170.9	0.5689	0.3874	0.0665	0.00794	$1.018 \times 10^{-4}$	$4.842 \times 10^{-6}$	3.137	0.850	0.00127	0.000838
10	46.38	34.02	0.4441	167.9	0.5775	0.3976	0.0647	0.00829	$9.606 \times 10^{-5}$	$4.961 \times 10^{-6}$	3.088	0.857	0.00132	0.000789
20	55.7	33.56	0.5289	164.8	0.5867	0.4084	0.0629	0.00865	$9.067 \times 10^{-5}$	$5.086 \times 10^{-6}$	3.043	0.864	0.00138	0.000740
30	66.35	33.10	0.6259	161.6	0.5966	0.4199	0.0512	0.00903	$8.561 \times 10^{-5}$	$5.211 \times 10^{-6}$	3.003	0.873	0.00144	0.000692
40	78.45	32.62	0.7365	158.1	0.6072	0.4321	0.0595	0.00942	$8.081 \times 10^{-5}$	$5.342 \times 10^{-6}$	2.967	0.882	0.00151	0.000644
50	92.12	32.13	0.8621	154.6	0.6187	0.4452	0.0579	0.00983	$7.631 \times 10^{-5}$	$5.478 \times 10^{-6}$	2.935	0.893	0.00159	0.000597
60	107.5	31.63	1.0046	150.8	0.6311	0.4593	0.0563	0.01025	$7.200 \times 10^{-5}$	$5.617 \times 10^{-6}$	2.906	0.906	0.00168	0.000551
70	124.6	31.11	1.1659	146.8	0.6447	0.4746	0.0547	0.01070	$6.794 \times 10^{-5}$	$5.764 \times 10^{-6}$	2.881	0.921	0.00179	0.000505
80	143.7	30.56	1.3484	142.7	0.6596	0.4915	0.0532	0.01116	$6.406 \times 10^{-5}$	$5.919 \times 10^{-6}$	2.860	0.938	0.00191	0.000460
90	164.8	30.00	1.5549	138.2	0.6762	0.5103	0.0517	0.01165	$6.033 \times 10^{-5}$	$6.081 \times 10^{-6}$	2.843	0.959	0.00205	0.000416
100	188.1	29.41	1.7887	133.6	0.6947	0.5315	0.0501	0.01217	$5.675 \times 10^{-5}$	$6.256 \times 10^{-6}$	2.831	0.984	0.00222	0.000372
120	241.8	28.13	2.3562	123.2	0.7403	0.5844	0.0472	0.01328	$5.000 \times 10^{-5}$	$6.644 \times 10^{-6}$	2.825	1.052	0.00267	0.000288
140	306.1	26.69	3.1003	111.1	0.7841	0.6613	0.0442	0.01454	$4.358 \times 10^{-5}$	$7.111 \times 10^{-6}$	2.784	1.164	0.00338	0.000208
160	382.4	24.98	4.1145	96.4	0.8696	0.7911	0.0411	0.01603	$3.733 \times 10^{-5}$	$7.719 \times 10^{-6}$	2.845	1.371	0.00459	0.000133
180	472.9	22.79	5.6265	77.1	1.1436	1.0813	0.0376	0.01793	$3.083 \times 10^{-5}$	$8.617 \times 10^{-6}$	3.380	1.870	0.00791	0.000065

Note 1: Kinematic viscosity  $\nu$  and thermal diffusivity  $\alpha$  can be calculated from their definitions,  $\nu = \mu/\rho$  and  $\alpha = k/\rho c_p = \nu/Pr$ . The properties listed here (except the vapor density) can be used at any pressures with negligible error at temperatures near the critical-point value.

Note 2: The unit Btu/lbm·°F for specific heat is equivalent to Btu/lbm·°R, and the unit Btu/h·ft·°F for thermal conductivity is equivalent to Btu/h·ft·R.

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Reiner Tillner-Roth, "Fundamental Equations of State," Shaker, Verlag, Aachen, 1998; B. A. Younglove and J. F. Ely, "Thermophysical Properties of Fluids. II Methane, Ethane, Propane, Isobutane, and Normal Butane," *J. Phys. Chem. Ref. Data*, Vol. 16, No. 4, 1987; G. R. Somayajulu, "A Generalized Equation for Surface Tension from the Triple-Point to the Critical-Point," *International Journal of Thermophysics*, Vol. 9, No. 4, 1988.

TABLE A-13E

## Properties of liquids

Temp. <i>T</i> , F°	Density $\rho$ , lbm/ft <sup>3</sup>	Specific Heat $c_p$ , Btu/lbm·R	Thermal Conductivity $k$ , Btu/h·ft·R	Thermal Diffusivity $\alpha$ , ft <sup>2</sup> /s	Dynamic Viscosity $\mu$ , lbm/ft·s	Kinematic Viscosity $\nu$ , ft <sup>2</sup> /s	Prandtl Number Pr	Volume Expansion Coeff. $\beta$ , 1/R
<i>Methane (CH<sub>4</sub>)</i>								
-280	27.41	0.8152	0.1205	$1.497 \times 10^{-6}$	$1.057 \times 10^{-4}$	$3.857 \times 10^{-6}$	2.575	0.00175
-260	26.43	0.8301	0.1097	$1.389 \times 10^{-6}$	$8.014 \times 10^{-5}$	$3.032 \times 10^{-6}$	2.183	0.00192
-240	25.39	0.8523	0.0994	$1.276 \times 10^{-6}$	$6.303 \times 10^{-5}$	$2.482 \times 10^{-6}$	1.945	0.00215
-220	24.27	0.8838	0.0896	$1.159 \times 10^{-6}$	$5.075 \times 10^{-5}$	$2.091 \times 10^{-6}$	1.803	0.00247
-200	23.04	0.9314	0.0801	$1.036 \times 10^{-6}$	$4.142 \times 10^{-5}$	$1.798 \times 10^{-6}$	1.734	0.00295
-180	21.64	1.010	0.0709	$9.008 \times 10^{-7}$	$3.394 \times 10^{-5}$	$1.568 \times 10^{-6}$	1.741	0.00374
-160	19.99	1.158	0.0616	$7.397 \times 10^{-7}$	$2.758 \times 10^{-5}$	$1.379 \times 10^{-6}$	1.865	0.00526
-140	17.84	1.542	0.0518	$5.234 \times 10^{-7}$	$2.168 \times 10^{-5}$	$1.215 \times 10^{-6}$	2.322	0.00943
<i>Methanol [CH<sub>3</sub>(OH)]</i>								
70	49.15	0.6024	0.1148	$1.076 \times 10^{-6}$	$3.872 \times 10^{-4}$	$7.879 \times 10^{-3}$	7.317	0.000656
90	48.50	0.6189	0.1143	$1.057 \times 10^{-6}$	$3.317 \times 10^{-4}$	$6.840 \times 10^{-6}$	6.468	0.000671
110	47.85	0.6373	0.1138	$1.036 \times 10^{-6}$	$2.872 \times 10^{-4}$	$6.005 \times 10^{-6}$	5.793	0.000691
130	47.18	0.6576	0.1133	$1.014 \times 10^{-6}$	$2.513 \times 10^{-4}$	$5.326 \times 10^{-6}$	5.250	0.000716
150	46.50	0.6796	0.1128	$9.918 \times 10^{-7}$	$2.218 \times 10^{-4}$	$4.769 \times 10^{-6}$	4.808	0.000749
170	45.80	0.7035	0.1124	$9.687 \times 10^{-7}$	$1.973 \times 10^{-4}$	$4.308 \times 10^{-6}$	4.447	0.000789
<i>Isobutane (R600a)</i>								
-150	42.75	0.4483	0.0799	$1.157 \times 10^{-6}$	$6.417 \times 10^{-4}$	$1.500 \times 10^{-5}$	12.96	0.000785
-100	41.06	0.4721	0.0782	$1.120 \times 10^{-3}$	$3.669 \times 10^{-4}$	$8.939 \times 10^{-6}$	7.977	0.000836
-50	39.31	0.4986	0.0731	$1.036 \times 10^{-6}$	$2.376 \times 10^{-4}$	$6.043 \times 10^{-6}$	5.830	0.000908
0	37.48	0.5289	0.0664	$9.299 \times 10^{-7}$	$1.651 \times 10^{-4}$	$4.406 \times 10^{-6}$	4.738	0.001012
50	35.52	0.5643	0.0591	$8.187 \times 10^{-7}$	$1.196 \times 10^{-4}$	$3.368 \times 10^{-6}$	4.114	0.001169
100	33.35	0.6075	0.0521	$7.139 \times 10^{-7}$	$8.847 \times 10^{-5}$	$2.653 \times 10^{-3}$	3.716	0.001421
150	30.84	0.6656	0.0457	$6.188 \times 10^{-7}$	$6.558 \times 10^{-5}$	$2.127 \times 10^{-6}$	3.437	0.001883
200	27.73	0.7635	0.0400	$5.249 \times 10^{-7}$	$4.750 \times 10^{-5}$	$1.713 \times 10^{-6}$	3.264	0.002970
<i>Glycerin</i>								
32	79.65	0.5402	0.163	$1.052 \times 10^{-6}$	7.047	0.08847	84101	
40	79.49	0.5458	0.1637	$1.048 \times 10^{-3}$	4.803	0.06042	57655	
50	79.28	0.5541	0.1645	$1.040 \times 10^{-6}$	2.850	0.03594	34561	
60	79.07	0.5632	0.1651	$1.029 \times 10^{-6}$	1.547	0.01956	18995	
70	78.86	0.5715	0.1652	$1.018 \times 10^{-6}$	0.9422	0.01195	11730	
80	78.66	0.5794	0.1652	$1.007 \times 10^{-6}$	0.5497	0.00699	6941	
90	78.45	0.5878	0.1652	$9.955 \times 10^{-7}$	0.3756	0.004787	4809	
100	78.24	0.5964	0.1653	$9.841 \times 10^{-7}$	0.2277	0.00291	2957	
<i>Engine Oil (unused)</i>								
32	56.12	0.4291	0.0849	$9.792 \times 10^{-7}$	2.563	$4.566 \times 10^{-2}$	46636	0.000389
50	55.79	0.4395	0.08338	$9.448 \times 10^{-7}$	1.210	$2.169 \times 10^{-2}$	22963	0.000389
75	55.3	0.4531	0.08378	$9.288 \times 10^{-7}$	0.4286	$7.751 \times 10^{-3}$	8345	0.000389
100	54.77	0.4669	0.08367	$9.089 \times 10^{-7}$	0.1630	$2.977 \times 10^{-3}$	3275	0.000389
125	54.24	0.4809	0.08207	$8.740 \times 10^{-7}$	$7.617 \times 10^{-2}$	$1.404 \times 10^{-3}$	1607	0.000389
150	53.73	0.4946	0.08046	$8.411 \times 10^{-7}$	$3.833 \times 10^{-2}$	$7.135 \times 10^{-4}$	848.3	0.000389
200	52.68	0.5231	0.07936	$7.999 \times 10^{-7}$	$1.405 \times 10^{-2}$	$2.668 \times 10^{-4}$	333.6	0.000389
250	51.71	0.5523	0.07776	$7.563 \times 10^{-7}$	$6.744 \times 10^{-3}$	$1.304 \times 10^{-4}$	172.5	0.000389
300	50.63	0.5818	0.07673	$7.236 \times 10^{-7}$	$3.661 \times 10^{-3}$	$7.232 \times 10^{-5}$	99.94	0.000389

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-14E

## Properties of liquid metals

Temp. $T, F^{\circ}$	Density $\rho, \text{lbm/ft}^3$	Specific Heat $c_p, \text{Btu/lbm}\cdot\text{R}$	Thermal Conductivity $k, \text{Btu/h}\cdot\text{ft}\cdot\text{R}$	Thermal Diffusivity $\alpha, \text{ft}^2/\text{s}$	Dynamic Viscosity $\mu, \text{lbm/ft}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{ft}^2/\text{s}$	Prandtl Number Pr	Volume Expansion Coeff. $\beta,$ 1/R
<i>Mercury (Hg) Melting Point: <math>-38^{\circ}\text{F}</math></i>								
32	848.7	0.03353	4.727	$4.614 \times 10^{-5}$	$1.133 \times 10^{-3}$	$1.335 \times 10^{-6}$	0.02895	$1.005 \times 10^{-4}$
50	847.2	0.03344	4.805	$4.712 \times 10^{-5}$	$1.092 \times 10^{-3}$	$1.289 \times 10^{-6}$	0.02737	$1.005 \times 10^{-4}$
100	842.9	0.03319	5.015	$4.980 \times 10^{-5}$	$9.919 \times 10^{-4}$	$1.176 \times 10^{-6}$	0.02363	$1.005 \times 10^{-4}$
150	838.7	0.03298	5.221	$5.244 \times 10^{-5}$	$9.122 \times 10^{-4}$	$1.087 \times 10^{-6}$	0.02074	$1.005 \times 10^{-4}$
200	834.5	0.03279	5.422	$5.504 \times 10^{-5}$	$8.492 \times 10^{-4}$	$1.017 \times 10^{-6}$	0.01849	$1.005 \times 10^{-4}$
300	826.2	0.03252	5.815	$6.013 \times 10^{-5}$	$7.583 \times 10^{-4}$	$9.180 \times 10^{-7}$	0.01527	$1.005 \times 10^{-4}$
400	817.9	0.03236	6.184	$6.491 \times 10^{-5}$	$6.972 \times 10^{-4}$	$8.524 \times 10^{-7}$	0.01313	$1.008 \times 10^{-4}$
500	809.6	0.03230	6.518	$6.924 \times 10^{-5}$	$6.525 \times 10^{-4}$	$8.061 \times 10^{-7}$	0.01164	$1.018 \times 10^{-4}$
600	801.3	0.03235	6.839	$7.329 \times 10^{-5}$	$6.186 \times 10^{-4}$	$7.719 \times 10^{-7}$	0.01053	$1.035 \times 10^{-4}$
<i>Bismuth (Bi) Melting Point: <math>520^{\circ}\text{F}</math></i>								
700	620.7	0.03509	9.361	$1.193 \times 10^{-4}$	$1.001 \times 10^{-3}$	$1.614 \times 10^{-6}$	0.01352	
800	616.5	0.03569	9.245	$1.167 \times 10^{-4}$	$9.142 \times 10^{-4}$	$1.482 \times 10^{-6}$	0.01271	
900	612.2	0.0363	9.129	$1.141 \times 10^{-4}$	$8.267 \times 10^{-4}$	$1.350 \times 10^{-6}$	0.01183	
1000	608.0	0.0369	9.014	$1.116 \times 10^{-4}$	$7.392 \times 10^{-4}$	$1.215 \times 10^{-6}$	0.0109	
1100	603.7	0.0375	9.014	$1.105 \times 10^{-4}$	$6.872 \times 10^{-4}$	$1.138 \times 10^{-6}$	0.01029	
<i>Lead (Pb) Melting Point: <math>621^{\circ}\text{F}</math></i>								
700	658	0.03797	9.302	$1.034 \times 10^{-4}$	$1.612 \times 10^{-3}$	$2.450 \times 10^{-6}$	0.02369	
800	654	0.03750	9.157	$1.037 \times 10^{-4}$	$1.453 \times 10^{-3}$	$2.223 \times 10^{-6}$	0.02143	
900	650	0.03702	9.013	$1.040 \times 10^{-4}$	$1.296 \times 10^{-3}$	$1.994 \times 10^{-6}$	0.01917	
1000	645.7	0.03702	8.912	$1.035 \times 10^{-4}$	$1.202 \times 10^{-3}$	$1.862 \times 10^{-6}$	0.01798	
1100	641.5	0.03702	8.810	$1.030 \times 10^{-4}$	$1.108 \times 10^{-3}$	$1.727 \times 10^{-6}$	0.01676	
1200	637.2	0.03702	8.709	$1.025 \times 10^{-4}$	$1.013 \times 10^{-3}$	$1.590 \times 10^{-6}$	0.01551	
<i>Sodium (Na) Melting Point: <math>280^{\circ}\text{F}</math></i>								
300	57.13	0.3258	48.19	$7.192 \times 10^{-4}$	$4.136 \times 10^{-4}$	$7.239 \times 10^{-6}$	0.01007	
400	56.28	0.3219	46.58	$7.142 \times 10^{-4}$	$3.572 \times 10^{-4}$	$6.350 \times 10^{-6}$	0.008891	
500	55.42	0.3181	44.98	$7.087 \times 10^{-4}$	$3.011 \times 10^{-4}$	$5.433 \times 10^{-6}$	0.007667	
600	54.56	0.3143	43.37	$7.026 \times 10^{-4}$	$2.448 \times 10^{-4}$	$4.488 \times 10^{-6}$	0.006387	
800	52.85	0.3089	40.55	$6.901 \times 10^{-4}$	$1.772 \times 10^{-4}$	$3.354 \times 10^{-6}$	0.004860	
1000	51.14	0.3057	38.12	$6.773 \times 10^{-4}$	$1.541 \times 10^{-4}$	$3.014 \times 10^{-6}$	0.004449	
<i>Potassium (K) Melting Point: <math>147^{\circ}\text{F}</math></i>								
300	50.40	0.1911	26.00	$7.500 \times 10^{-4}$	$2.486 \times 10^{-4}$	$4.933 \times 10^{-6}$	0.006577	
400	49.58	0.1887	25.37	$7.532 \times 10^{-4}$	$2.231 \times 10^{-4}$	$4.500 \times 10^{-6}$	0.005975	
500	48.76	0.1863	24.73	$7.562 \times 10^{-4}$	$1.976 \times 10^{-4}$	$4.052 \times 10^{-6}$	0.005359	
600	47.94	0.1839	24.09	$7.591 \times 10^{-4}$	$1.721 \times 10^{-4}$	$3.589 \times 10^{-6}$	0.004728	
800	46.31	0.1791	22.82	$7.643 \times 10^{-4}$	$1.210 \times 10^{-4}$	$2.614 \times 10^{-6}$	0.003420	
1000	44.62	0.1791	21.34	$7.417 \times 10^{-4}$	$1.075 \times 10^{-4}$	$2.409 \times 10^{-6}$	0.003248	
<i>Sodium-Potassium (%22Na-%78K) Melting Point: <math>12^{\circ}\text{F}</math></i>								
200	52.99	0.2259	14.79	$3.432 \times 10^{-4}$	$3.886 \times 10^{-4}$	$7.331 \times 10^{-6}$	0.02136	
300	52.16	0.2230	14.99	$3.580 \times 10^{-4}$	$3.467 \times 10^{-4}$	$6.647 \times 10^{-6}$	0.01857	
400	51.32	0.2201	15.19	$3.735 \times 10^{-4}$	$3.050 \times 10^{-4}$	$5.940 \times 10^{-6}$	0.0159	
600	49.65	0.2143	15.59	$4.070 \times 10^{-4}$	$2.213 \times 10^{-4}$	$4.456 \times 10^{-6}$	0.01095	
800	47.99	0.2100	15.95	$4.396 \times 10^{-4}$	$1.539 \times 10^{-4}$	$3.207 \times 10^{-6}$	0.007296	
1000	46.36	0.2103	16.20	$4.615 \times 10^{-4}$	$1.353 \times 10^{-4}$	$2.919 \times 10^{-6}$	0.006324	

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-15E

Properties of air at 1 atm pressure

Temp. $T, \text{F}^\circ$	Density $\rho, \text{lbm/ft}^3$	Specific Heat $c_p, \text{Btu/lbm}\cdot\text{R}$	Thermal Conductivity $k, \text{Btu/h}\cdot\text{ft}\cdot\text{R}$	Thermal Diffusivity $\alpha, \text{ft}^2/\text{s}$	Dynamic Viscosity $\mu, \text{lbm/ft}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{ft}^2/\text{s}$	Prandtl Number Pr
-300	0.24844	0.5072	0.00508	$1.119 \times 10^{-5}$	$4.039 \times 10^{-6}$	$1.625 \times 10^{-5}$	1.4501
-200	0.15276	0.2247	0.00778	$6.294 \times 10^{-5}$	$6.772 \times 10^{-6}$	$4.433 \times 10^{-5}$	0.7042
-100	0.11029	0.2360	0.01037	$1.106 \times 10^{-4}$	$9.042 \times 10^{-6}$	$8.197 \times 10^{-5}$	0.7404
-50	0.09683	0.2389	0.01164	$1.397 \times 10^{-4}$	$1.006 \times 10^{-5}$	$1.039 \times 10^{-4}$	0.7439
0	0.08630	0.2401	0.01288	$1.726 \times 10^{-4}$	$1.102 \times 10^{-5}$	$1.278 \times 10^{-4}$	0.7403
10	0.08446	0.2402	0.01312	$1.797 \times 10^{-4}$	$1.121 \times 10^{-5}$	$1.328 \times 10^{-4}$	0.7391
20	0.08270	0.2403	0.01336	$1.868 \times 10^{-4}$	$1.140 \times 10^{-5}$	$1.379 \times 10^{-4}$	0.7378
30	0.08101	0.2403	0.01361	$1.942 \times 10^{-4}$	$1.158 \times 10^{-5}$	$1.430 \times 10^{-4}$	0.7365
40	0.07939	0.2404	0.01385	$2.016 \times 10^{-4}$	$1.176 \times 10^{-5}$	$1.482 \times 10^{-4}$	0.7350
50	0.07783	0.2404	0.01409	$2.092 \times 10^{-4}$	$1.194 \times 10^{-5}$	$1.535 \times 10^{-4}$	0.7336
60	0.07633	0.2404	0.01433	$2.169 \times 10^{-4}$	$1.212 \times 10^{-5}$	$1.588 \times 10^{-4}$	0.7321
70	0.07489	0.2404	0.01457	$2.248 \times 10^{-4}$	$1.230 \times 10^{-5}$	$1.643 \times 10^{-4}$	0.7306
80	0.07350	0.2404	0.01481	$2.328 \times 10^{-4}$	$1.247 \times 10^{-5}$	$1.697 \times 10^{-4}$	0.7290
90	0.07217	0.2404	0.01505	$2.409 \times 10^{-4}$	$1.265 \times 10^{-5}$	$1.753 \times 10^{-4}$	0.7275
100	0.07088	0.2405	0.01529	$2.491 \times 10^{-4}$	$1.281 \times 10^{-5}$	$1.809 \times 10^{-4}$	0.7260
110	0.06963	0.2405	0.01552	$2.575 \times 10^{-4}$	$1.299 \times 10^{-5}$	$1.866 \times 10^{-4}$	0.7245
120	0.06843	0.2405	0.01576	$2.660 \times 10^{-4}$	$1.316 \times 10^{-5}$	$1.923 \times 10^{-4}$	0.7230
130	0.06727	0.2405	0.01599	$2.746 \times 10^{-4}$	$1.332 \times 10^{-5}$	$1.981 \times 10^{-4}$	0.7216
140	0.06615	0.2406	0.01623	$2.833 \times 10^{-4}$	$1.349 \times 10^{-5}$	$2.040 \times 10^{-4}$	0.7202
150	0.06507	0.2406	0.01646	$2.921 \times 10^{-4}$	$1.365 \times 10^{-5}$	$2.099 \times 10^{-4}$	0.7188
160	0.06402	0.2406	0.01669	$3.010 \times 10^{-4}$	$1.382 \times 10^{-5}$	$2.159 \times 10^{-4}$	0.7174
170	0.06300	0.2407	0.01692	$3.100 \times 10^{-4}$	$1.398 \times 10^{-5}$	$2.220 \times 10^{-4}$	0.7161
180	0.06201	0.2408	0.01715	$3.191 \times 10^{-4}$	$1.414 \times 10^{-5}$	$2.281 \times 10^{-4}$	0.7148
190	0.06106	0.2408	0.01738	$3.284 \times 10^{-4}$	$1.430 \times 10^{-5}$	$2.343 \times 10^{-4}$	0.7136
200	0.06013	0.2409	0.01761	$3.377 \times 10^{-4}$	$1.446 \times 10^{-5}$	$2.406 \times 10^{-4}$	0.7124
250	0.05590	0.2415	0.01874	$3.857 \times 10^{-4}$	$1.524 \times 10^{-5}$	$2.727 \times 10^{-4}$	0.7071
300	0.05222	0.2423	0.01985	$4.358 \times 10^{-4}$	$1.599 \times 10^{-5}$	$3.063 \times 10^{-4}$	0.7028
350	0.04899	0.2433	0.02094	$4.879 \times 10^{-4}$	$1.672 \times 10^{-5}$	$3.413 \times 10^{-4}$	0.6995
400	0.04614	0.2445	0.02200	$5.419 \times 10^{-4}$	$1.743 \times 10^{-5}$	$3.777 \times 10^{-4}$	0.6971
450	0.04361	0.2458	0.02305	$5.974 \times 10^{-4}$	$1.812 \times 10^{-5}$	$4.154 \times 10^{-4}$	0.6953
500	0.04134	0.2472	0.02408	$6.546 \times 10^{-4}$	$1.878 \times 10^{-5}$	$4.544 \times 10^{-4}$	0.6942
600	0.03743	0.2503	0.02608	$7.732 \times 10^{-4}$	$2.007 \times 10^{-5}$	$5.361 \times 10^{-4}$	0.6934
700	0.03421	0.2535	0.02800	$8.970 \times 10^{-4}$	$2.129 \times 10^{-5}$	$6.225 \times 10^{-4}$	0.6940
800	0.03149	0.2568	0.02986	$1.025 \times 10^{-3}$	$2.247 \times 10^{-5}$	$7.134 \times 10^{-4}$	0.6956
900	0.02917	0.2599	0.03164	$1.158 \times 10^{-3}$	$2.359 \times 10^{-5}$	$8.087 \times 10^{-4}$	0.6978
1000	0.02718	0.2630	0.03336	$1.296 \times 10^{-3}$	$2.467 \times 10^{-5}$	$9.080 \times 10^{-4}$	0.7004
1500	0.02024	0.2761	0.04106	$2.041 \times 10^{-3}$	$2.957 \times 10^{-5}$	$1.460 \times 10^{-3}$	0.7158
2000	0.01613	0.2855	0.04752	$2.867 \times 10^{-3}$	$3.379 \times 10^{-5}$	$2.095 \times 10^{-3}$	0.7308
2500	0.01340	0.2922	0.05309	$3.765 \times 10^{-3}$	$3.750 \times 10^{-5}$	$2.798 \times 10^{-3}$	0.7432
3000	0.01147	0.2972	0.05811	$4.737 \times 10^{-3}$	$4.082 \times 10^{-5}$	$3.560 \times 10^{-3}$	0.7516
3500	0.01002	0.3010	0.06293	$5.797 \times 10^{-3}$	$4.381 \times 10^{-5}$	$4.373 \times 10^{-3}$	0.7543
4000	0.00889	0.3040	0.06789	$6.975 \times 10^{-3}$	$4.651 \times 10^{-5}$	$5.229 \times 10^{-3}$	0.7497

Note: For ideal gases, the properties  $c_p, k, \mu,$  and Pr are independent of pressure. The properties  $\rho, \nu,$  and  $\alpha$  at a pressure  $P$  (in atm) other than 1 atm are determined by multiplying the values of  $\rho$  at the given temperature by  $P$  and by dividing  $\nu$  and  $\alpha$  by  $P$ .

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Original sources: Keenan, Chao, Keyes, Gas Tables, Wiley, 1984; and *Thermophysical Properties of Matter*, Vol. 3: *Thermal Conductivity*, Y. S. Touloukian, P. E. Liley, S. C. Saxena, Vol. 11: *Viscosity*, Y. S. Touloukian, S. C. Saxena, and P. Hestermans, IFI/Plenum, NY, 1970, ISBN 0-306067020-8.

TABLE A-16E

Properties of gases at 1 atm pressure

Temp. <i>T</i> , F°	Density $\rho$ , lbm/ft <sup>3</sup>	Specific Heat $c_p$ , Btu/lbm·R	Thermal Conductivity $k$ , Btu/h·ft·R	Thermal Diffusivity $\alpha$ , ft <sup>2</sup> /s	Dynamic Viscosity $\mu$ , lbm/ft·s	Kinematic Viscosity $\nu$ , ft <sup>2</sup> /s	Prandtl Number Pr
<i>Carbon Dioxide, CO<sub>2</sub></i>							
-50	0.14712	0.1797	0.00628	$6.600 \times 10^{-5}$	$7.739 \times 10^{-6}$	$5.261 \times 10^{-5}$	0.7970
0	0.13111	0.1885	0.00758	$8.522 \times 10^{-5}$	$8.661 \times 10^{-6}$	$6.606 \times 10^{-5}$	0.7751
50	0.11825	0.1965	0.00888	$1.061 \times 10^{-4}$	$9.564 \times 10^{-6}$	$8.086 \times 10^{-5}$	0.7621
100	0.10769	0.2039	0.01017	$1.286 \times 10^{-4}$	$1.045 \times 10^{-5}$	$9.703 \times 10^{-5}$	0.7543
200	0.09136	0.2171	0.01273	$1.784 \times 10^{-4}$	$1.217 \times 10^{-5}$	$1.332 \times 10^{-4}$	0.7469
300	0.07934	0.2284	0.01528	$2.341 \times 10^{-4}$	$1.382 \times 10^{-5}$	$1.743 \times 10^{-4}$	0.7445
500	0.06280	0.2473	0.02027	$3.626 \times 10^{-4}$	$1.696 \times 10^{-5}$	$2.700 \times 10^{-4}$	0.7446
1000	0.04129	0.2796	0.03213	$7.733 \times 10^{-4}$	$2.381 \times 10^{-5}$	$5.767 \times 10^{-4}$	0.7458
1500	0.03075	0.2995	0.04281	$1.290 \times 10^{-3}$	$2.956 \times 10^{-5}$	$9.610 \times 10^{-4}$	0.7445
2000	0.02450	0.3124	0.05193	$1.885 \times 10^{-3}$	$3.451 \times 10^{-5}$	$1.408 \times 10^{-3}$	0.7474
<i>Carbon Monoxide, CO</i>							
-50	0.09363	0.2571	0.01118	$1.290 \times 10^{-4}$	$9.419 \times 10^{-6}$	$1.005 \times 10^{-4}$	0.7798
0	0.08345	0.2523	0.01240	$1.636 \times 10^{-4}$	$1.036 \times 10^{-5}$	$1.242 \times 10^{-4}$	0.7593
50	0.07526	0.2496	0.01359	$2.009 \times 10^{-4}$	$1.127 \times 10^{-5}$	$1.498 \times 10^{-4}$	0.7454
100	0.06854	0.2484	0.01476	$2.408 \times 10^{-4}$	$1.214 \times 10^{-5}$	$1.772 \times 10^{-4}$	0.7359
200	0.05815	0.2485	0.01702	$3.273 \times 10^{-4}$	$1.379 \times 10^{-5}$	$2.372 \times 10^{-4}$	0.7247
300	0.05049	0.2505	0.01920	$4.217 \times 10^{-4}$	$1.531 \times 10^{-5}$	$3.032 \times 10^{-4}$	0.7191
500	0.03997	0.2567	0.02331	$6.311 \times 10^{-4}$	$1.802 \times 10^{-5}$	$4.508 \times 10^{-4}$	0.7143
1000	0.02628	0.2732	0.03243	$1.254 \times 10^{-3}$	$2.334 \times 10^{-5}$	$8.881 \times 10^{-4}$	0.7078
1500	0.01957	0.2862	0.04049	$2.008 \times 10^{-3}$	$2.766 \times 10^{-5}$	$1.413 \times 10^{-3}$	0.7038
2000	0.01559	0.2958	0.04822	$2.903 \times 10^{-3}$	$3.231 \times 10^{-5}$	$2.072 \times 10^{-3}$	0.7136
<i>Methane, CH<sub>4</sub></i>							
-50	0.05363	0.5335	0.01401	$1.360 \times 10^{-4}$	$5.861 \times 10^{-6}$	$1.092 \times 10^{-4}$	0.8033
0	0.04779	0.5277	0.01616	$1.780 \times 10^{-4}$	$6.506 \times 10^{-6}$	$1.361 \times 10^{-4}$	0.7649
50	0.04311	0.5320	0.01839	$2.228 \times 10^{-4}$	$7.133 \times 10^{-6}$	$1.655 \times 10^{-4}$	0.7428
100	0.03925	0.5433	0.02071	$2.698 \times 10^{-4}$	$7.742 \times 10^{-6}$	$1.972 \times 10^{-4}$	0.7311
200	0.03330	0.5784	0.02559	$3.690 \times 10^{-4}$	$8.906 \times 10^{-6}$	$2.674 \times 10^{-4}$	0.7245
300	0.02892	0.6226	0.03077	$4.748 \times 10^{-4}$	$1.000 \times 10^{-5}$	$3.457 \times 10^{-4}$	0.7283
500	0.02289	0.7194	0.04195	$7.075 \times 10^{-4}$	$1.200 \times 10^{-5}$	$5.244 \times 10^{-4}$	0.7412
1000	0.01505	0.9438	0.07346	$1.436 \times 10^{-3}$	$1.620 \times 10^{-5}$	$1.076 \times 10^{-3}$	0.7491
1500	0.01121	1.1162	0.10766	$2.390 \times 10^{-3}$	$1.974 \times 10^{-5}$	$1.760 \times 10^{-3}$	0.7366
2000	0.00893	1.2419	0.14151	$3.544 \times 10^{-3}$	$2.327 \times 10^{-5}$	$2.605 \times 10^{-3}$	0.7353
<i>Hydrogen, H<sub>2</sub></i>							
-50	0.00674	3.0603	0.08246	$1.110 \times 10^{-3}$	$4.969 \times 10^{-6}$	$7.373 \times 10^{-4}$	0.6638
0	0.00601	3.2508	0.09049	$1.287 \times 10^{-3}$	$5.381 \times 10^{-6}$	$8.960 \times 10^{-4}$	0.6960
50	0.00542	3.3553	0.09818	$1.500 \times 10^{-3}$	$5.781 \times 10^{-6}$	$1.067 \times 10^{-3}$	0.7112
100	0.00493	3.4118	0.10555	$1.742 \times 10^{-3}$	$6.167 \times 10^{-6}$	$1.250 \times 10^{-3}$	0.7177
200	0.00419	3.4549	0.11946	$2.295 \times 10^{-3}$	$6.911 \times 10^{-6}$	$1.652 \times 10^{-3}$	0.7197
300	0.00363	3.4613	0.13241	$2.924 \times 10^{-3}$	$7.622 \times 10^{-6}$	$2.098 \times 10^{-3}$	0.7174
500	0.00288	3.4572	0.15620	$4.363 \times 10^{-3}$	$8.967 \times 10^{-6}$	$3.117 \times 10^{-3}$	0.7146
1000	0.00189	3.5127	0.20989	$8.776 \times 10^{-3}$	$1.201 \times 10^{-5}$	$6.354 \times 10^{-3}$	0.7241
1500	0.00141	3.6317	0.26381	$1.432 \times 10^{-2}$	$1.477 \times 10^{-5}$	$1.048 \times 10^{-2}$	0.7323
2000	0.00112	3.7656	0.31923	$2.098 \times 10^{-2}$	$1.734 \times 10^{-5}$	$1.544 \times 10^{-2}$	0.7362
<i>Nitrogen, N<sub>2</sub></i>							
-50	0.09364	0.2320	0.01176	$1.504 \times 10^{-4}$	$9.500 \times 10^{-6}$	$1.014 \times 10^{-4}$	0.6746
0	0.08346	0.2441	0.01300	$1.773 \times 10^{-4}$	$1.043 \times 10^{-5}$	$1.251 \times 10^{-4}$	0.7056
50	0.07527	0.2480	0.01420	$2.113 \times 10^{-4}$	$1.134 \times 10^{-5}$	$1.507 \times 10^{-4}$	0.7133



TABLE A-16E

Properties of gases at 1 atm pressure (Concluded)

Temp. $T, \text{F}^\circ$	Density $\rho, \text{lbm/ft}^3$	Specific Heat $c_p, \text{Btu/lbm}\cdot\text{R}$	Thermal Conductivity $k, \text{Btu/h}\cdot\text{ft}\cdot\text{R}$	Thermal Diffusivity $\alpha, \text{ft}^2/\text{s}$	Dynamic Viscosity $\mu, \text{lbm/ft}\cdot\text{s}$	Kinematic Viscosity $\nu, \text{ft}^2/\text{s}$	Prandtl Number Pr
100	0.06854	0.2489	0.01537	$2.502 \times 10^{-4}$	$1.221 \times 10^{-5}$	$1.783 \times 10^{-4}$	0.7126
200	0.05815	0.2487	0.01760	$3.379 \times 10^{-4}$	$1.388 \times 10^{-5}$	$2.387 \times 10^{-4}$	0.7062
300	0.05050	0.2492	0.01970	$4.349 \times 10^{-4}$	$1.543 \times 10^{-5}$	$3.055 \times 10^{-4}$	0.7025
500	0.03997	0.2535	0.02359	$6.466 \times 10^{-4}$	$1.823 \times 10^{-5}$	$4.559 \times 10^{-4}$	0.7051
1000	0.02628	0.2697	0.03204	$1.255 \times 10^{-3}$	$2.387 \times 10^{-5}$	$9.083 \times 10^{-4}$	0.7232
1500	0.01958	0.2831	0.04002	$2.006 \times 10^{-3}$	$2.829 \times 10^{-5}$	$1.445 \times 10^{-3}$	0.7202
2000	0.01560	0.2927	0.04918	$2.992 \times 10^{-3}$	$3.212 \times 10^{-5}$	$2.059 \times 10^{-3}$	0.6882
<i>Oxygen, O<sub>2</sub></i>							
-50	0.10697	0.2331	0.01216	$1.355 \times 10^{-4}$	$1.104 \times 10^{-5}$	$1.032 \times 10^{-4}$	0.7622
0	0.09533	0.2245	0.01346	$1.747 \times 10^{-4}$	$1.218 \times 10^{-5}$	$1.277 \times 10^{-4}$	0.7312
50	0.08598	0.2209	0.01475	$2.157 \times 10^{-4}$	$1.326 \times 10^{-5}$	$1.543 \times 10^{-4}$	0.7152
100	0.07830	0.2200	0.01601	$2.582 \times 10^{-4}$	$1.429 \times 10^{-5}$	$1.826 \times 10^{-4}$	0.7072
200	0.06643	0.2221	0.01851	$3.484 \times 10^{-4}$	$1.625 \times 10^{-5}$	$2.446 \times 10^{-4}$	0.7020
300	0.05768	0.2262	0.02096	$4.463 \times 10^{-4}$	$1.806 \times 10^{-5}$	$3.132 \times 10^{-4}$	0.7018
500	0.04566	0.2352	0.02577	$6.665 \times 10^{-4}$	$2.139 \times 10^{-5}$	$4.685 \times 10^{-4}$	0.7029
1000	0.03002	0.2520	0.03698	$1.357 \times 10^{-3}$	$2.855 \times 10^{-5}$	$9.509 \times 10^{-4}$	0.7005
1500	0.02236	0.2626	0.04701	$2.224 \times 10^{-3}$	$3.474 \times 10^{-5}$	$1.553 \times 10^{-3}$	0.6985
2000	0.01782	0.2701	0.05614	$3.241 \times 10^{-3}$	$4.035 \times 10^{-5}$	$2.265 \times 10^{-3}$	0.6988
<i>Water Vapor, H<sub>2</sub>O</i>							
-50	0.06022	0.4512	0.00797	$8.153 \times 10^{-5}$	$4.933 \times 10^{-6}$	$8.192 \times 10^{-5}$	1.0050
0	0.05367	0.4484	0.00898	$1.036 \times 10^{-4}$	$5.592 \times 10^{-6}$	$1.041 \times 10^{-4}$	1.0049
50	0.04841	0.4472	0.01006	$1.291 \times 10^{-4}$	$6.261 \times 10^{-6}$	$1.293 \times 10^{-4}$	1.0018
100	0.04408	0.4473	0.01121	$1.579 \times 10^{-4}$	$6.942 \times 10^{-6}$	$1.574 \times 10^{-4}$	0.9969
200	0.03740	0.4503	0.01372	$2.263 \times 10^{-4}$	$8.333 \times 10^{-6}$	$2.228 \times 10^{-4}$	0.9845
300	0.03248	0.4557	0.01648	$3.093 \times 10^{-4}$	$9.756 \times 10^{-6}$	$3.004 \times 10^{-4}$	0.9713
500	0.02571	0.4707	0.02267	$5.204 \times 10^{-4}$	$1.267 \times 10^{-5}$	$4.931 \times 10^{-4}$	0.9475
1000	0.01690	0.5167	0.04134	$1.314 \times 10^{-3}$	$2.014 \times 10^{-5}$	$1.191 \times 10^{-3}$	0.9063
1500	0.01259	0.5625	0.06315	$2.477 \times 10^{-3}$	$2.742 \times 10^{-5}$	$2.178 \times 10^{-3}$	0.8793
2000	0.01003	0.6034	0.08681	$3.984 \times 10^{-3}$	$3.422 \times 10^{-5}$	$3.411 \times 10^{-3}$	0.8563

Note: For ideal gases, the properties  $c_p, k, \mu$ , and Pr are independent of pressure. The properties  $\rho, \nu$ , and  $\alpha$  at a pressure  $P$  (in atm) other than 1 atm are determined by multiplying the values of  $\rho$  at the given temperature by  $P$  and by dividing  $\nu$  and  $\alpha$  by  $P$ .

Source: Data generated from the EES software developed by S. A. Klein and F. L. Alvarado. Originally based on various sources.

TABLE A-17E

Properties of the atmosphere at high altitude

Altitude, <i>z</i> , ft	Temperature <i>T</i> , °F	Pressure, $\rho$ , psia	Gravity <i>g</i> , ft/s <sup>2</sup>	Speed of Sound <i>c</i> , ft/s	Density $\rho$ , lbm/ft <sup>3</sup>	Viscosity $\mu$ , lbm/ft-s	Thermal Conductivity, <i>k</i> , Btu/h-ft-R
0	59.00	14.7	32.174	1116	0.07647	$1.202 \times 10^{-5}$	0.0146
500	57.22	14.4	32.173	1115	0.07536	$1.199 \times 10^{-5}$	0.0146
1000	55.43	14.2	32.171	1113	0.07426	$1.196 \times 10^{-5}$	0.0146
1500	53.65	13.9	32.169	1111	0.07317	$1.193 \times 10^{-5}$	0.0145
2000	51.87	13.7	32.168	1109	0.07210	$1.190 \times 10^{-5}$	0.0145
2500	50.09	13.4	32.166	1107	0.07104	$1.186 \times 10^{-5}$	0.0144
3000	48.30	13.2	32.165	1105	0.06998	$1.183 \times 10^{-5}$	0.0144
3500	46.52	12.9	32.163	1103	0.06985	$1.180 \times 10^{-5}$	0.0143
4000	44.74	12.7	32.162	1101	0.06792	$1.177 \times 10^{-5}$	0.0143
4500	42.96	12.5	32.160	1099	0.06690	$1.173 \times 10^{-5}$	0.0142
5000	41.17	12.2	32.159	1097	0.06590	$1.170 \times 10^{-5}$	0.0142
5500	39.39	12.0	32.157	1095	0.06491	$1.167 \times 10^{-5}$	0.0141
6000	37.61	11.8	32.156	1093	0.06393	$1.164 \times 10^{-5}$	0.0141
6500	35.83	11.6	32.154	1091	0.06296	$1.160 \times 10^{-5}$	0.0141
7000	34.05	11.3	32.152	1089	0.06200	$1.157 \times 10^{-5}$	0.0140
7500	32.26	11.1	32.151	1087	0.06105	$1.154 \times 10^{-5}$	0.0140
8000	30.48	10.9	32.149	1085	0.06012	$1.150 \times 10^{-5}$	0.0139
8500	28.70	10.7	32.148	1083	0.05919	$1.147 \times 10^{-5}$	0.0139
9000	26.92	10.5	32.146	1081	0.05828	$1.144 \times 10^{-5}$	0.0138
9500	25.14	10.3	32.145	1079	0.05738	$1.140 \times 10^{-5}$	0.0138
10,000	23.36	10.1	32.145	1077	0.05648	$1.137 \times 10^{-5}$	0.0137
11,000	19.79	9.72	32.140	1073	0.05473	$1.130 \times 10^{-5}$	0.0136
12,000	16.23	9.34	32.137	1069	0.05302	$1.124 \times 10^{-5}$	0.0136
13,000	12.67	8.99	32.134	1065	0.05135	$1.117 \times 10^{-5}$	0.0135
14,000	9.12	8.63	32.131	1061	0.04973	$1.110 \times 10^{-5}$	0.0134
15,000	5.55	8.29	32.128	1057	0.04814	$1.104 \times 10^{-5}$	0.0133
16,000	+1.99	7.97	32.125	1053	0.04659	$1.097 \times 10^{-5}$	0.0132
17,000	-1.58	7.65	32.122	1049	0.04508	$1.090 \times 10^{-5}$	0.0132
18,000	-5.14	7.34	32.119	1045	0.04361	$1.083 \times 10^{-5}$	0.0130
19,000	-8.70	7.05	32.115	1041	0.04217	$1.076 \times 10^{-5}$	0.0129
20,000	-12.2	6.76	32.112	1037	0.04077	$1.070 \times 10^{-5}$	0.0128
22,000	-19.4	6.21	32.106	1029	0.03808	$1.056 \times 10^{-5}$	0.0126
24,000	-26.5	5.70	32.100	1020	0.03553	$1.042 \times 10^{-5}$	0.0124
26,000	-33.6	5.22	32.094	1012	0.03311	$1.028 \times 10^{-5}$	0.0122
28,000	-40.7	4.78	32.088	1003	0.03082	$1.014 \times 10^{-5}$	0.0121
30,000	-47.8	4.37	32.082	995	0.02866	$1.000 \times 10^{-5}$	0.0119
32,000	-54.9	3.99	32.08	987	0.02661	$0.986 \times 10^{-5}$	0.0117
34,000	-62.0	3.63	32.07	978	0.02468	$0.971 \times 10^{-5}$	0.0115
36,000	-69.2	3.30	32.06	969	0.02285	$0.956 \times 10^{-5}$	0.0113
38,000	-69.7	3.05	32.06	968	0.02079	$0.955 \times 10^{-5}$	0.0113
40,000	-69.7	2.73	32.05	968	0.01890	$0.955 \times 10^{-5}$	0.0113
45,000	-69.7	2.148	32.04	968	0.01487	$0.955 \times 10^{-5}$	0.0113
50,000	-69.7	1.691	32.02	968	0.01171	$0.955 \times 10^{-5}$	0.0113
55,000	-69.7	1.332	32.00	968	0.00922	$0.955 \times 10^{-5}$	0.0113
60,000	-69.7	1.048	31.99	968	0.00726	$0.955 \times 10^{-5}$	0.0113

Source: U.S. Standard Atmosphere Supplements, U.S. Government Printing Office, 1966.